



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Optimizing Conventional Water Treatment Plants

Presentation to the AWWOA Annual Seminar
Banff, Alberta, March 15th, 2006

Simon Breese, Technical Practice Leader, Drinking Water
Earth Tech, Inc.



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006

Workshop Outline

- Approaches to Plant Optimization
- What defines “good” design/performance ?
- Common Causes of Sub-Par Performance
- Evaluation & Optimization of:
 - Coagulation & Flocculation
 - Clarification (Sedimentation or DAF)
 - Granular Media Filtration
- Discussion & Question Period





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



What is “Optimization” ?

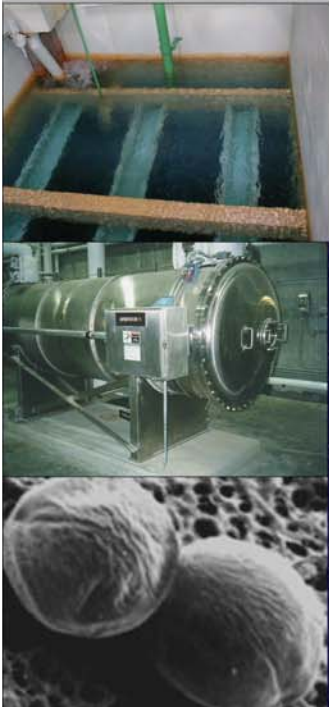
- “To attain the most efficient or effective use of” your water treatment plant
- Achievement of consistently high quality finished water on a continuous basis
- Important not to focus too much on individual processes
- Focus on OVERALL plant performance





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Approaches to Plant Optimization

- Mostly common sense...not a “black art”
- Be organized, get the facts first !!
- Systematic gathering of information about plant performance:
 - Data trending & analysis
 - Check plant design criteria against “actual”
 - Track chemical dosing vs performance
 - Field measurements
 - Visual Observations





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Data Trending and Analysis

- The “GIGO” (Garbage In-Garbage Out) Principle Applies !!!
- Collect and collate plant data in a form which facilitates analysis....i.e. spreadsheet
- Correlate plant operating parameters against each other to look for valuable trends



AWWOA Annual
Seminar

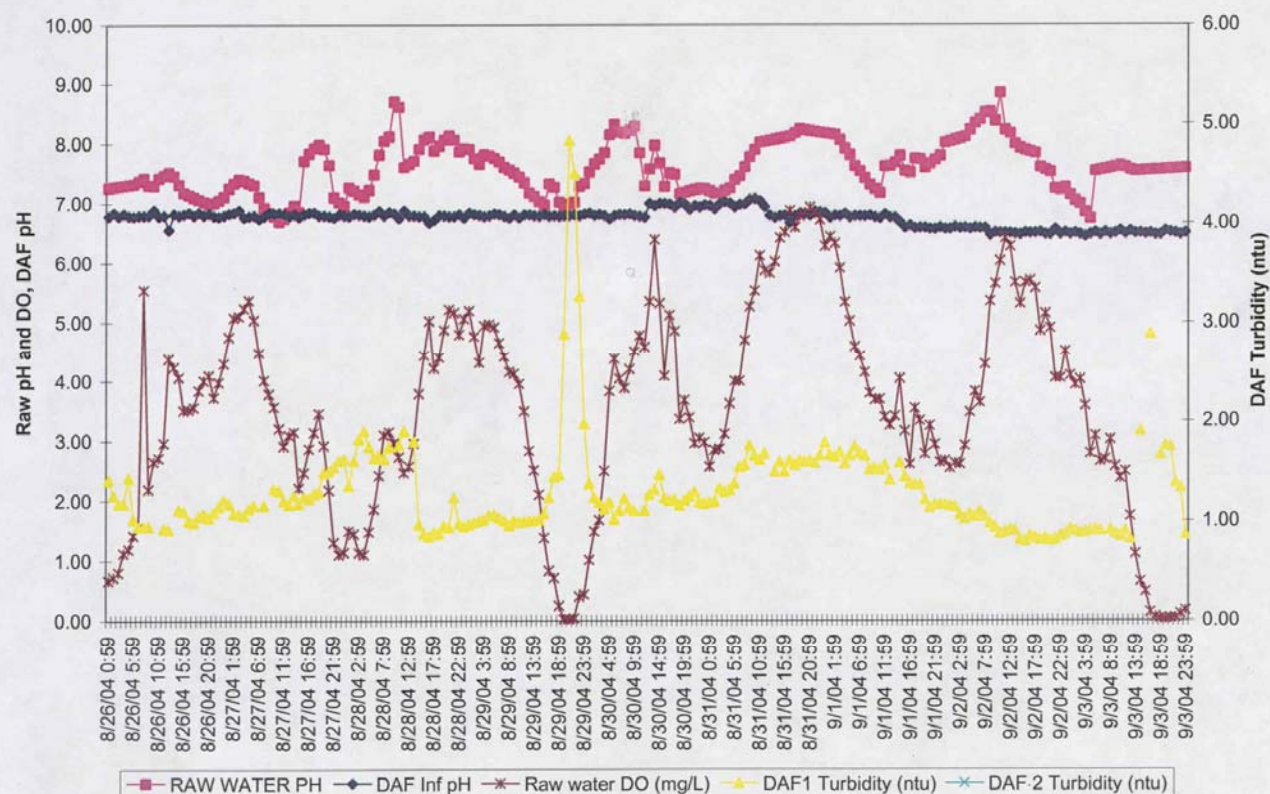
Banff, Alberta
March 15, 2006



Analyzing trends can quickly solve problems

8_26_9_3

8/26 - 9/3 LDF DAF Performance





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Chemical Dosing Trends

- Understand how chemical dosing impacts plant performance
- Look for over- or under-dosing, track
 - Raw water turbidity vs Coagulant Dose
 - Raw and coagulated water pH and alkalinity vs coagulant dose
 - Clarified water turbidity vs coagulant dosage



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Coagulation & Flash Mixing



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Coagulation & Flash Mixing

- Getting the Chemistry Right
 - Coagulation Objectives
 - Selecting the Right Coagulant
 - Appropriate Coagulant Dosage
 - Matching Alkalinity with Coagulant Dosage
- Getting the Dosing & Mixing Right
 - Coagulation Mechanisms
 - Coagulant Mixing Methods
 - Coagulant Pumping



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



What the heck is coagulation anyway ?

- The use of chemicals (coagulants) to destabilize colloidal material, and entrap them within a floc particle
- Once in particulate form, floc is easily removed



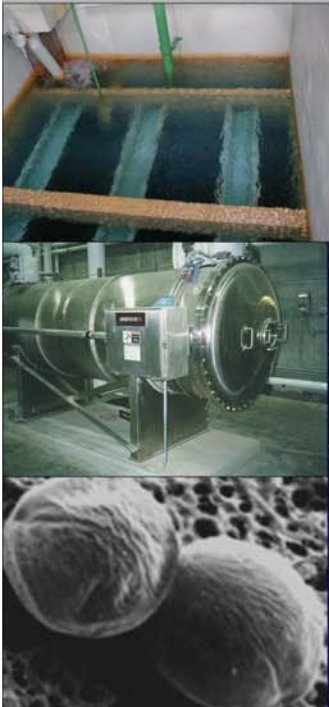


AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006

Colloid Stability

- Colloids ($<10\mu\text{m}$) are stable and remain in suspension by virtue of their electrostatic charge (predominantly negative)
- May take anywhere from 200⁺ days up to 50⁺ years to settle
- Without effective coagulation, solids removal would be impractical





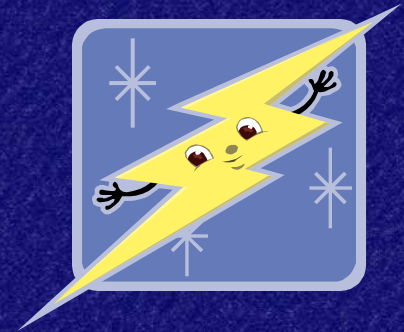
AWWQA Annual
Seminar

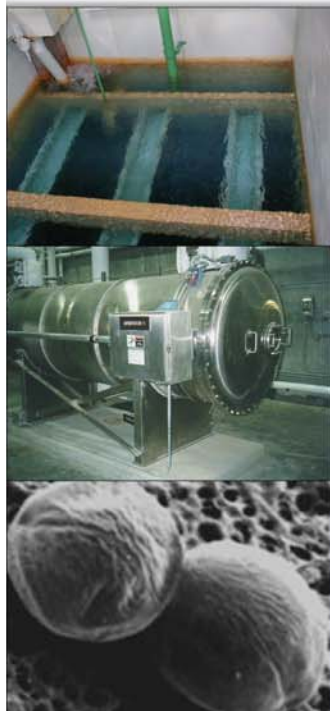
Banff, Alberta
March 15, 2006



Theory of Coagulation

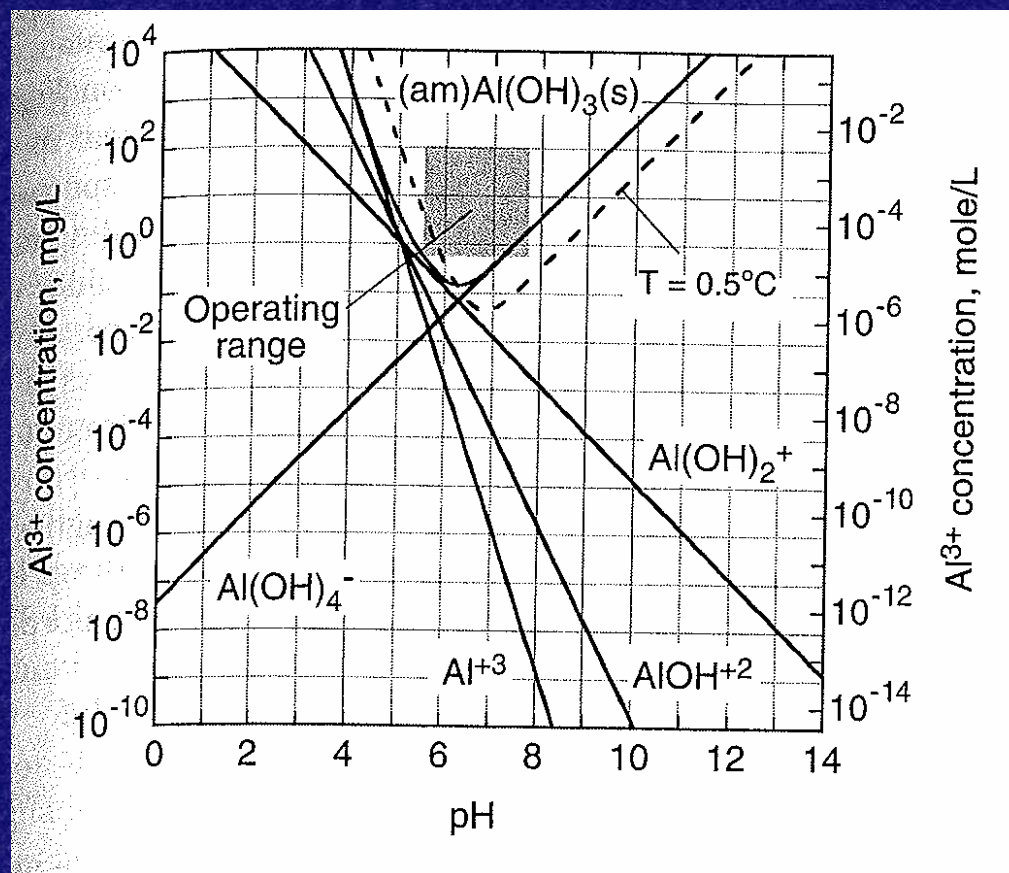
- Coagulation is achieved mainly through the reduction of the electrical double layer on the surface of a charged particle resulting in its destabilization or **removal of charge**
- Generally takes place in a matter of seconds after coagulant addition
- Once charge is removed, particles can stick together & **form a floc**

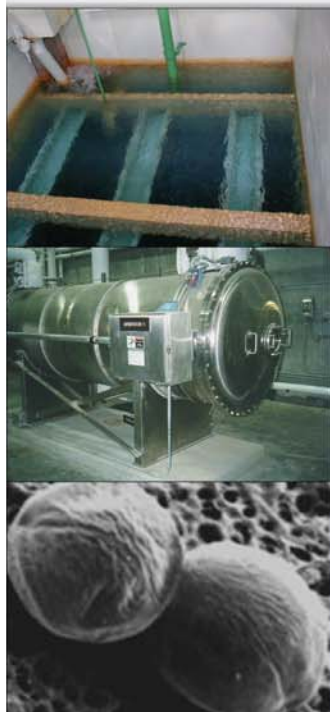




Alum Coagulation

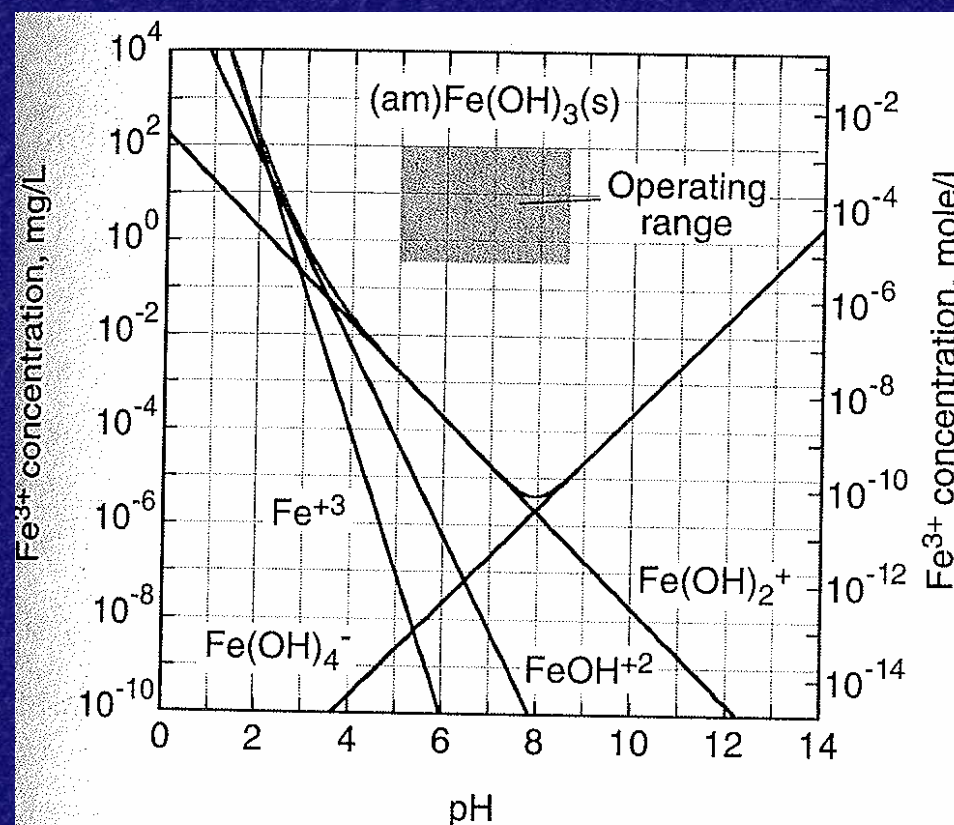
- Fairly tight “optimal” pH range 5.5 – 7.5





Ferric Coagulation

- Broader Effective pH range 5 – 8.5





Selecting & Evaluating Coagulants

- Jar test, jar test, jar test !!!
 - Different coagulants against each other
 - Coagulant and Flocculant Aid polymers
 - Chemical addition in varying order (coagulant, coagulant aid, alkalinity enhancing)
- **2 factors** most often overlooked:
 - Alumina (Al_2O_3) Content
 - Degree of Basicity



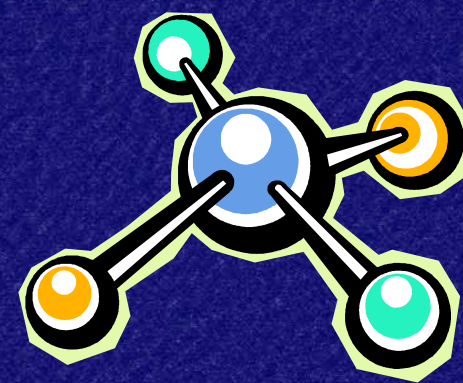


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Understanding Alumina Content



Coagulant Chemistry



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Not all coagulants are created equal

Coagulant	Percent as Alumina
Alum	8.20% as Alumina
IsoPAC 70	11% as Alumina
Polyaminium Chloride (PACl)	18% as Alumina
Aluminium Chlorhydrate (ACH)	23.50% as Alumina



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Standardization Based on Alumina

Therefore 10 PPM of Alum (at 8.2% Al_2O_3) can result in comparative coagulants “dose standardized” by active **Alumina** composition being fed at:

- Isopac 70 (11% Al_2O_3) = 7.45 PPM (25% less)
- PACI (18 % Al_2O_3) = 4.56 PPM (55% less)
- ACH (23.5 % Al_2O_3) = 3.49 PPM (65% less)

Al_2O_3 content can be found on MSDS sheet



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



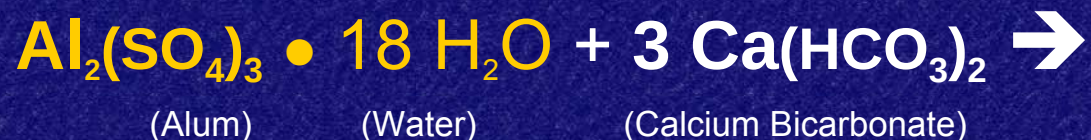
Understanding Coagulant Basicity



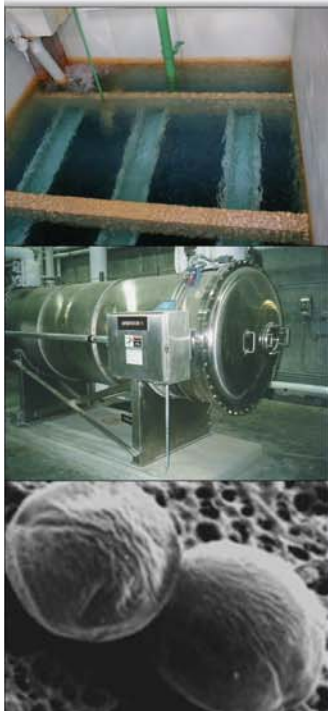
AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006

Coagulation Chemistry

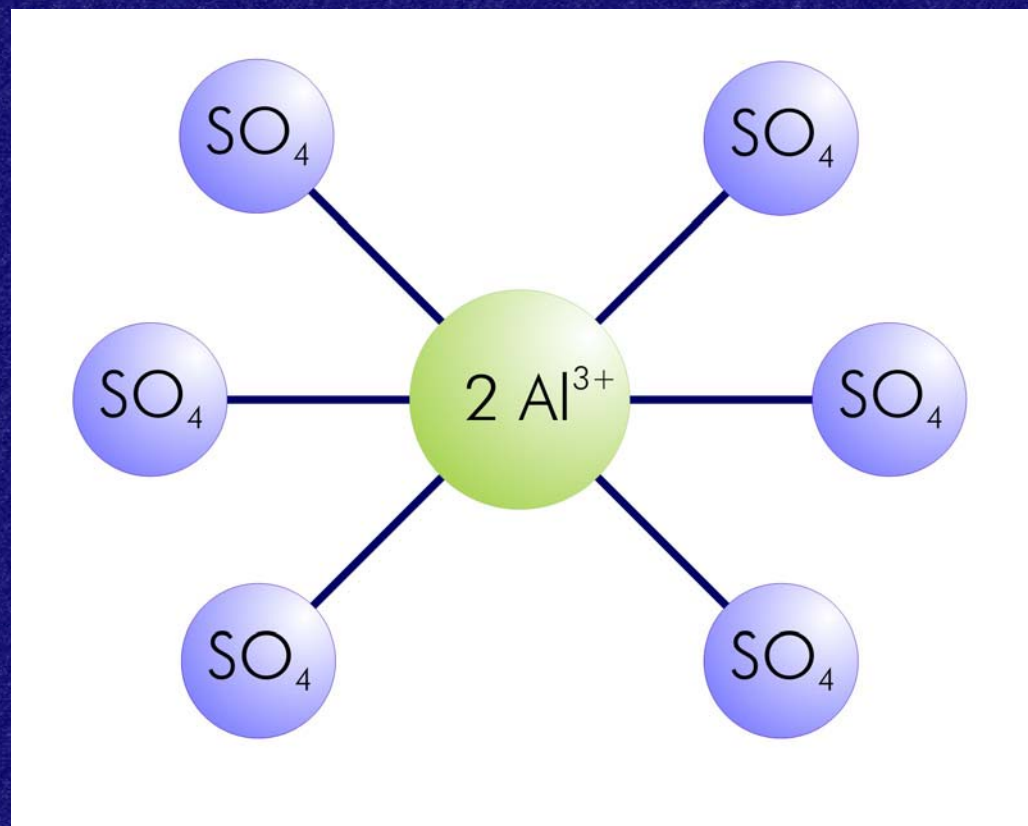


Important: Every 1 mg/l of Alum added to water requires 0.45 mg/l of Alkalinity (as CaCO_3)



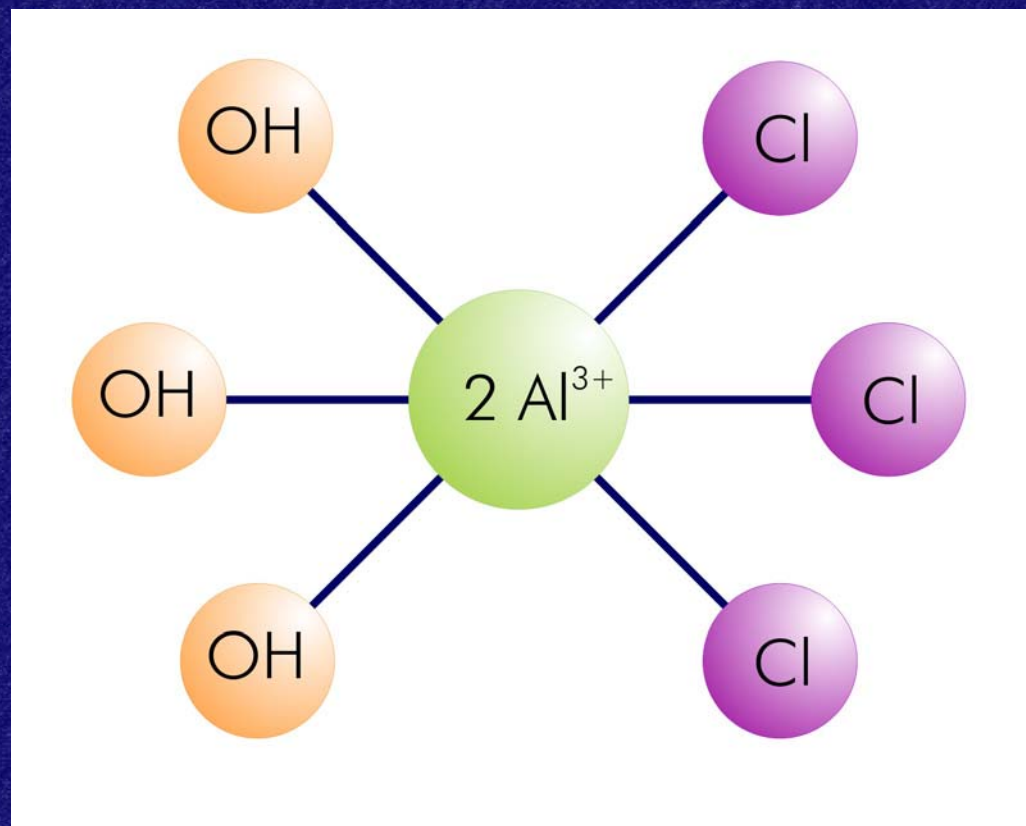


Coagulation Reactions - Alum





Polyhydroxy Aluminum Chloride



Therefore can be considered 50% **pre-hydrolysed** (3/6 sites)

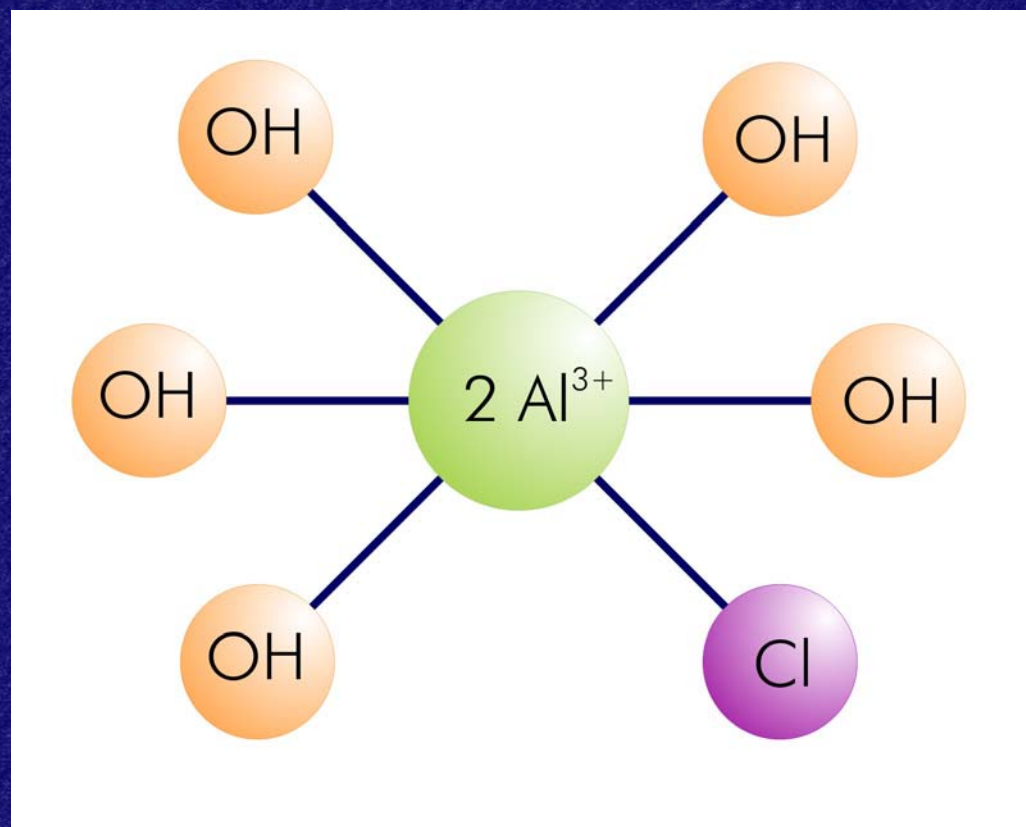


AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Aluminum Chlorohydrate (ACH)



Therefore considered 80% **pre-hydrolysed** ($5/6 = 0.83333$)



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Degree of “Basicity”

(Or Pre-Hydrolization)

Coagulant	Extent of Pre-Hydrolization
Alum	0%
PACI (ISOPAC)	45%
ISOPAC 70	70%
ACH	80%

- Alum consumes more alkalinity than other aluminium based coagulants
- Higher consumption of alkalinity means greater impact on pH
- Optimal coagulation may not occur without sufficient “residual” alkalinity, at least 10 mg/L as CaCO_3



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

Alkalinity Limitations

Product	Alkalinity Available mg/L	Al ₂ O ₃ Strength	Basicity	MAX DOSE (Based on Basicity)	Alum Eqv (Based on Al ₂ O ₃)
Alum	10	8.2	0%	20	20
Isopac 70	10	11	70%	67	89
PACI	10	18	45%	36	80
ACH	10	23.5	83%	118	337





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Operational & Design factors affecting coagulation

- Uniformity of Coagulant Flow
 - Ideally dose in a steady stream
 - Many utilities moving to gear pumps, to avoid pulsation inherent with metering pumps
- Vigour of coagulant mixing
 - Coagulation reactions take a fraction of a second – Instantaneous mixing is critical
 - Static mixers can lose effectiveness at lower flows
- pH and Alkalinity
 - Consider the need to add alkalinity if coagulant demands are higher. Soda ash generally the most effective additive
 - Generally try to ensure 10 – 20 mg/L as CaCO_3 residual alkalinity after coagulation



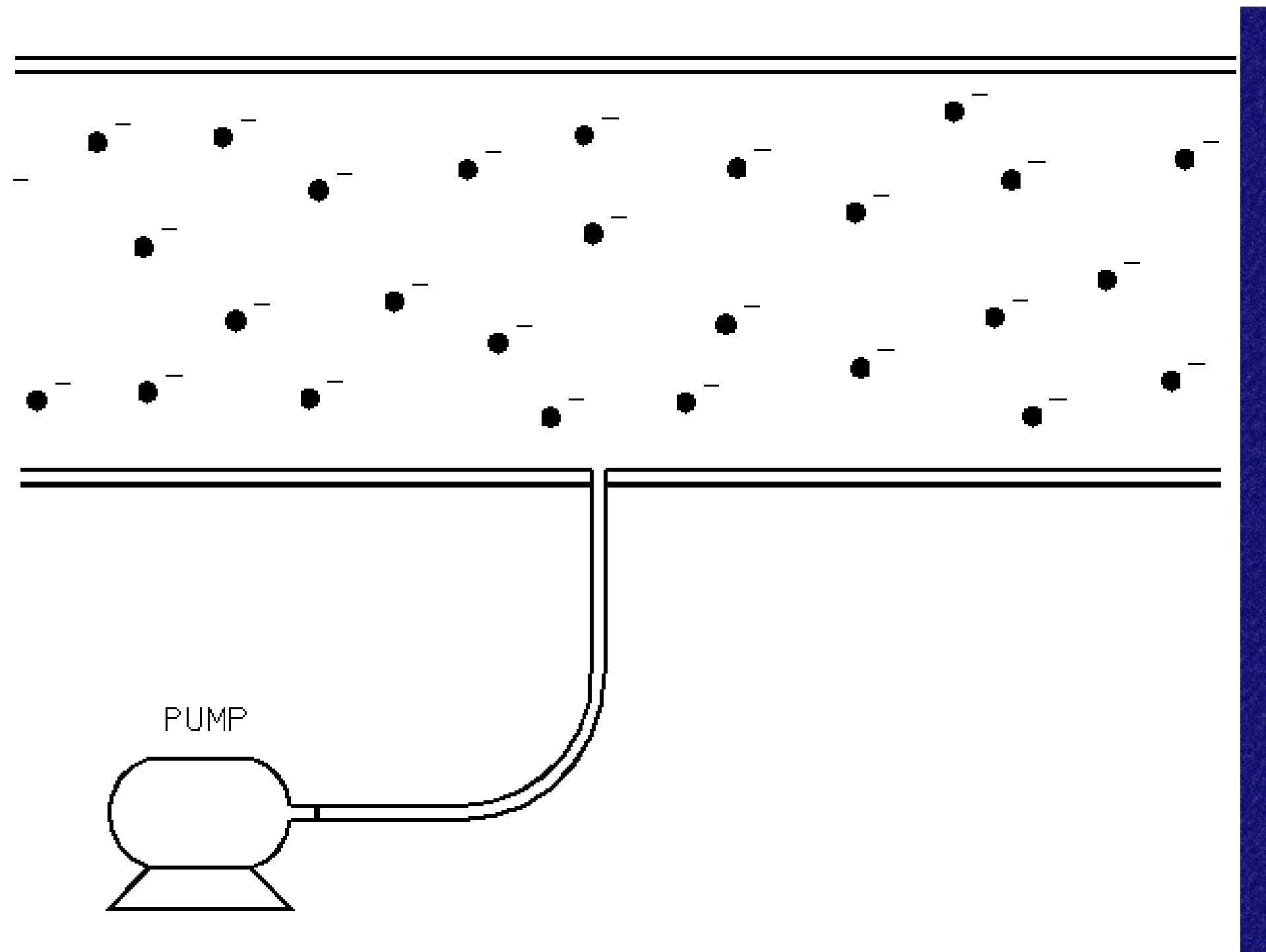
AWWQA Annual
Seminar

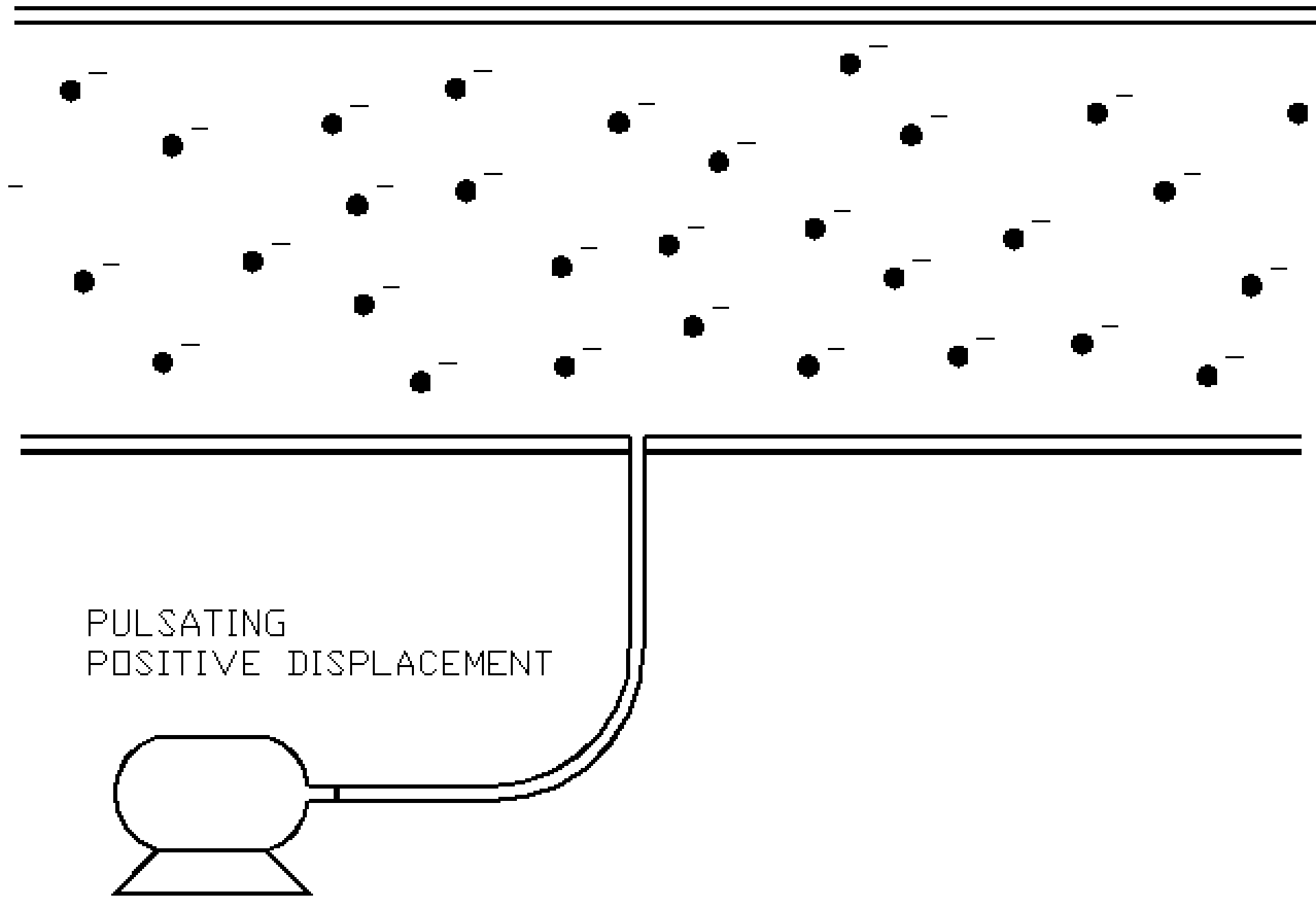
Banff, Alberta
March 15, 2006

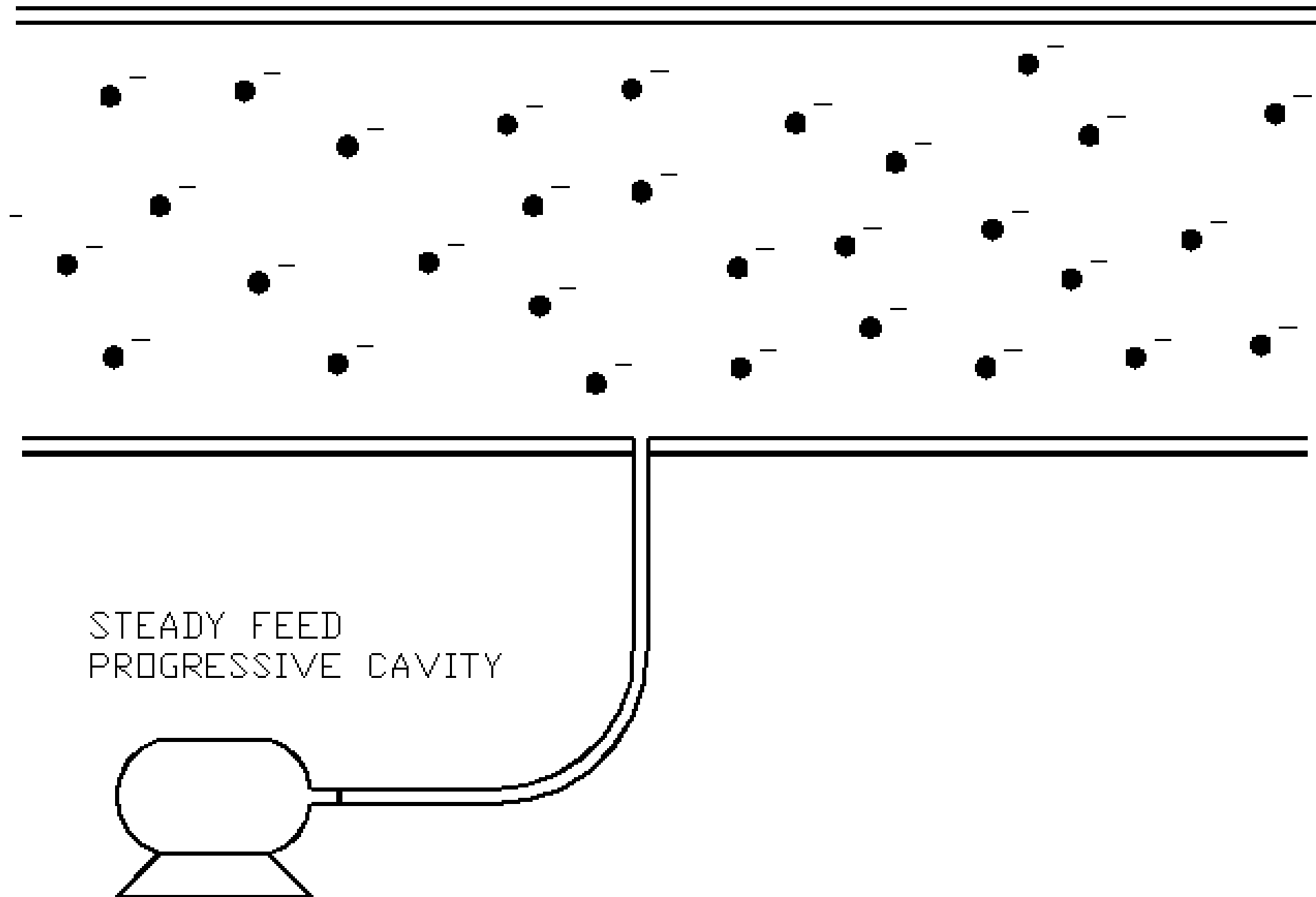


Common problems with coagulation

- Under or over-dosing – Use Jar Testing !!
- Mixing of insufficient energy – Undesirable coagulation reactions occur
- Fouling or clogging of injectors or diffusers – Usually caused either by pre-dilution of coagulant, or poor mixing at the point of injection
 - Causes high, very localized coagulant concentrations
 - Significant precipitation around the injector
- Trying to mix too many chemicals at once, causing side reactions







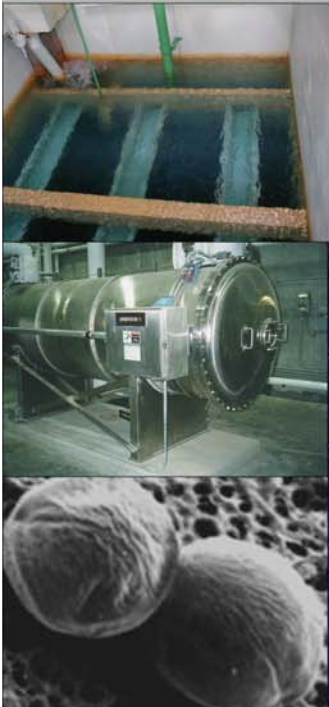


AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006

Coagulant Mixing

- Rapid Mixing is Critical – True “Flash” Mixing is desired
- Speed of coagulation reactions are very quick – From a fraction of a second to 7 seconds
- Excessive mixing time is wasted
- **NEVER** pre-dilute coagulant to improve mixing turbulence



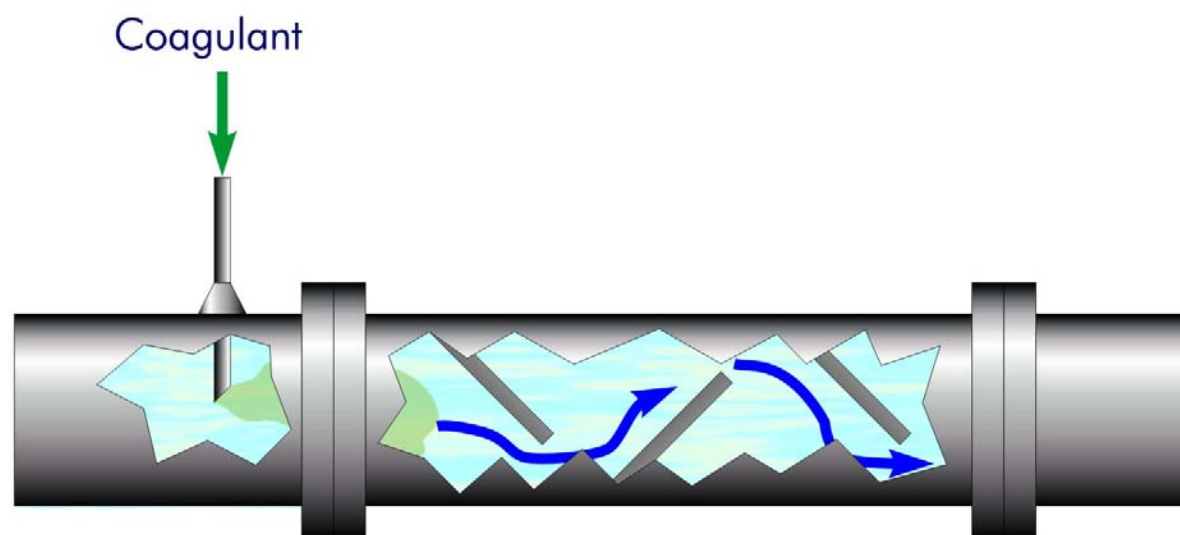


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

Static Mixing

- Very common in small plants
- Mixing energy is linked to flow
- Low flow = Low Mixing Energy = Poor Flash Mixing



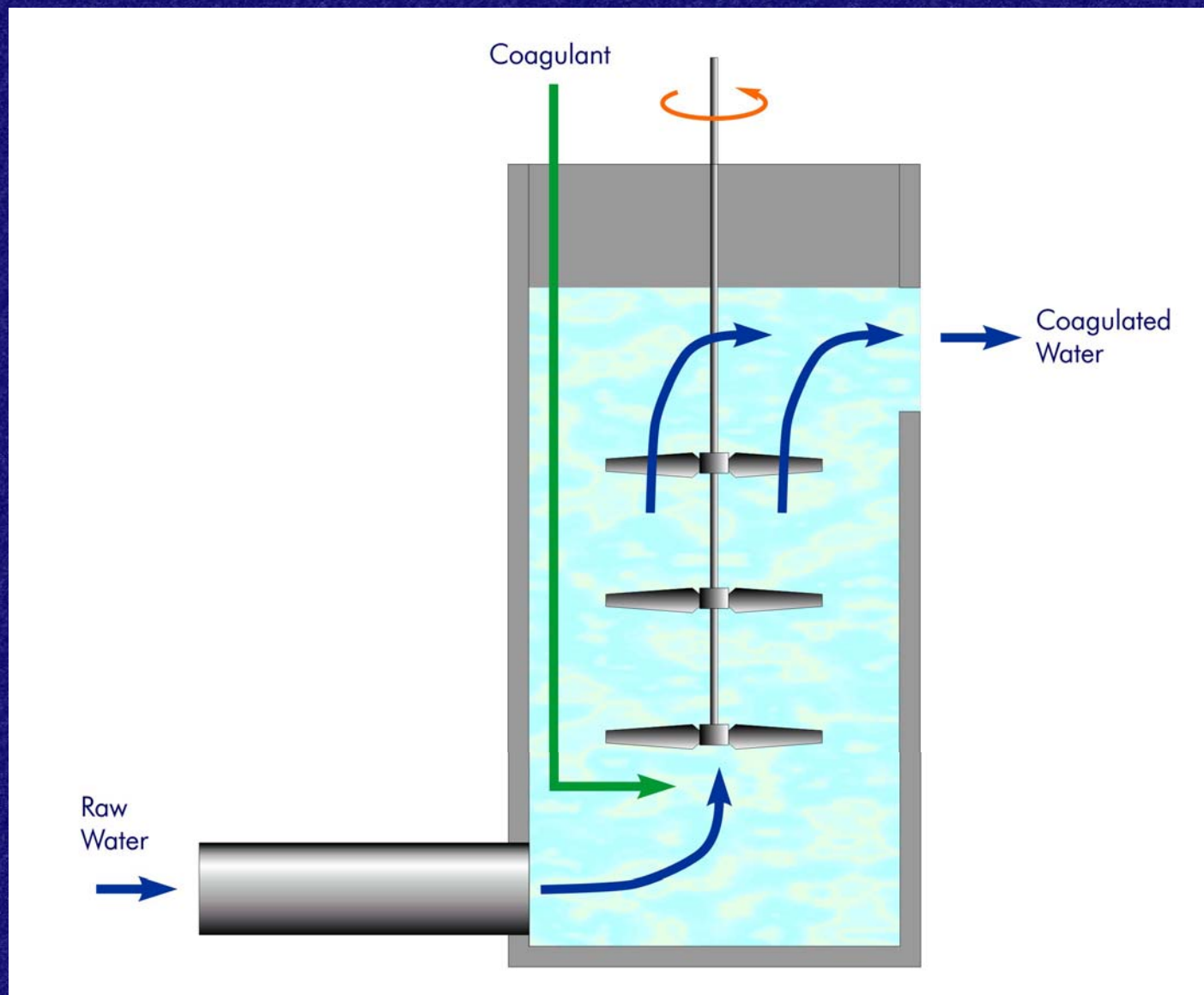


AWWOA Annual
Seminar

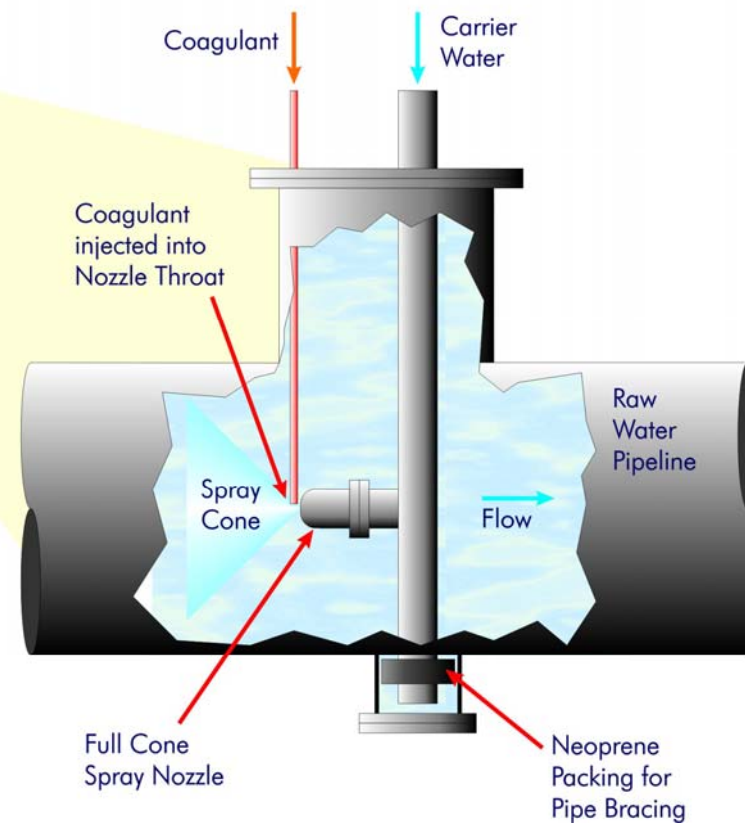
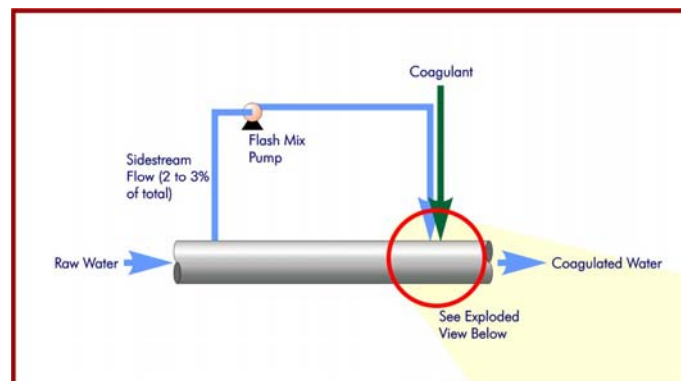
Banff, Alberta
March 15, 2006



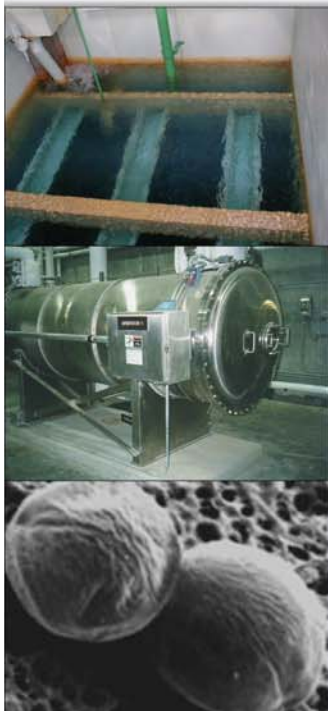
Mechanical Flash Mixing



"Jet" Flash Mixing



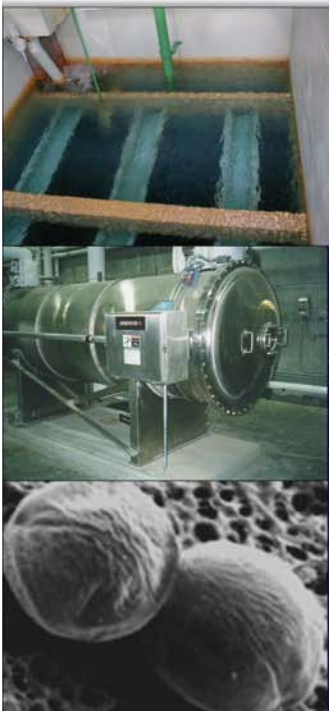
- ★ Most energy efficient
- ★ Flash mix achieved within 1 pipe diameter





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Flocculation Good Practice

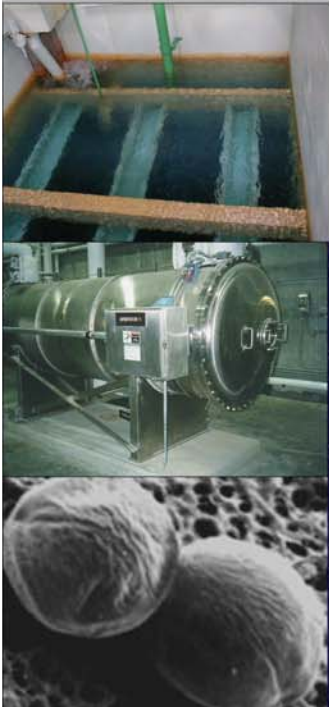
- Tapered flocculation ($G = 20 - 70 \text{ s}^{-1}$) for sedimentation – 20 – 30 min total
- Perforated intra-cell baffle walls to minimize short circuiting
- Higher energy ($G = 100 \text{ s}^{-1}$) non-tapered flocculation for DAF – 15 min total
- Maximum blade tip speed 2 – 3 m/s for vertical turbine flocculators to avoid floc damage
- Include variable speed drives to adjust flocculation energy for optimal performance



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

Clarification





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



What constitutes “good” clarifier performance ?

- Consistently less than 2 NTU is excellent
- Stable when faced with rapidly changing water quality conditions
- Produces a sludge of consistent quality:
 - Sedimentation: 0.5 – 1 %TS
 - DAF (Hydraulically desludged): 0.5 – 1 %TS
 - DAF (Mechanically scraped): 2 – 3 %TS
 - ActiFlo: Generally 0.1 – 0.3 %TS
- Poor performance can be difficult to rectify – Often design related



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



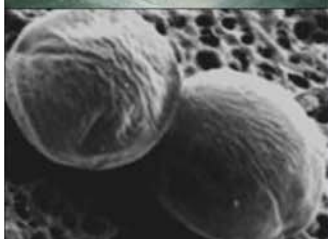
Common Causes for Poor Clarifier Performance

- Density currents due to temperature variation within basins
- Excessive operating loading rates
- Entrained air – Incidental flotation
- Poor hydraulics due to uneven inlet flow splitting or flocculation circulatory patterns
- Sudden changes in raw water conditions
- Chemical under- or over-dosing
- Inappropriate sludge removal rates
- Insufficient air loading (DAF) or sand concentrations (ActiFlo)



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Is your clarifier suited to your raw water quality ?

Clarification Process	High Algae Load	Highly Coloured Sources	Low Turbidity, Impounded Sources	Moderate Turbidity, Impounded Sources	Elevated Turbidity, River Sources	Lime Softening
Conventional or High Rate Sedimentation	☆☆	☆☆	☆☆	☆☆☆	☆☆☆☆	☆☆☆
Sludge Blanket Clarification	☆☆	☆☆	☆☆	☆☆☆	☆☆☆	☆☆☆☆☆
DAF (Conventional Or High Rate)	☆☆☆☆☆	☆☆☆☆☆	☆☆☆☆☆	☆☆☆	No-Go	No-Go
ActiFlo	☆☆☆	☆☆☆☆	☆☆☆☆	☆☆☆☆☆	☆☆☆☆☆	No-Go



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006

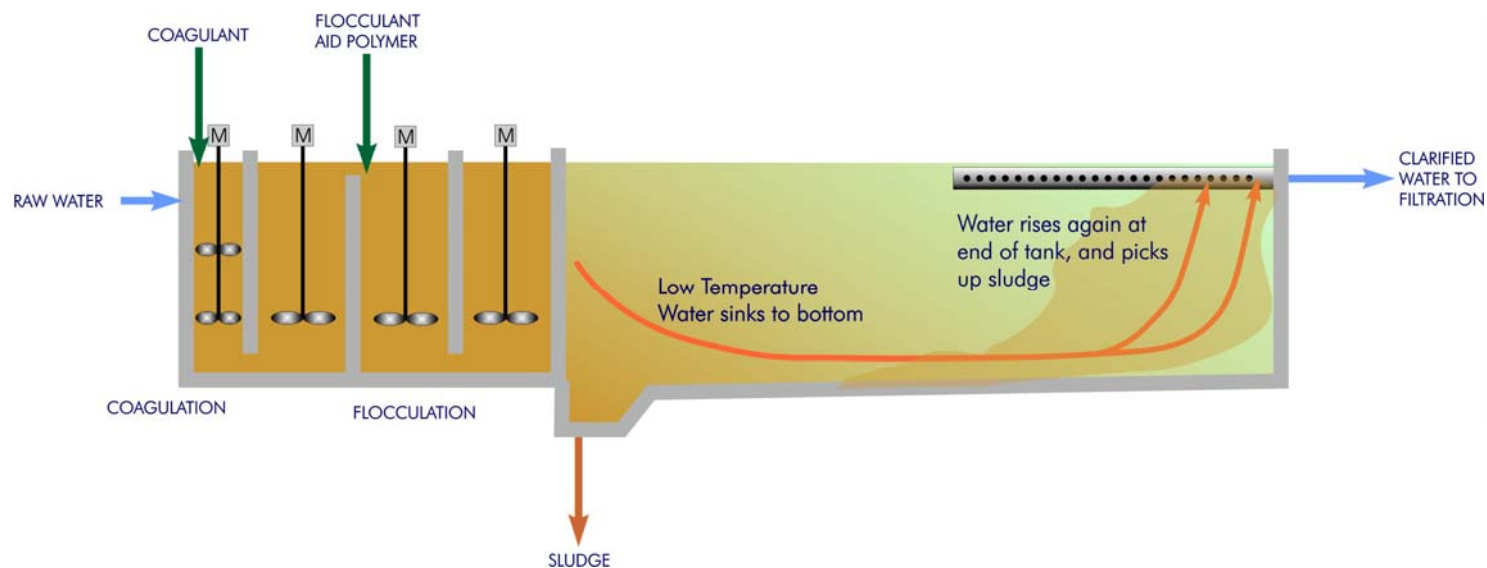


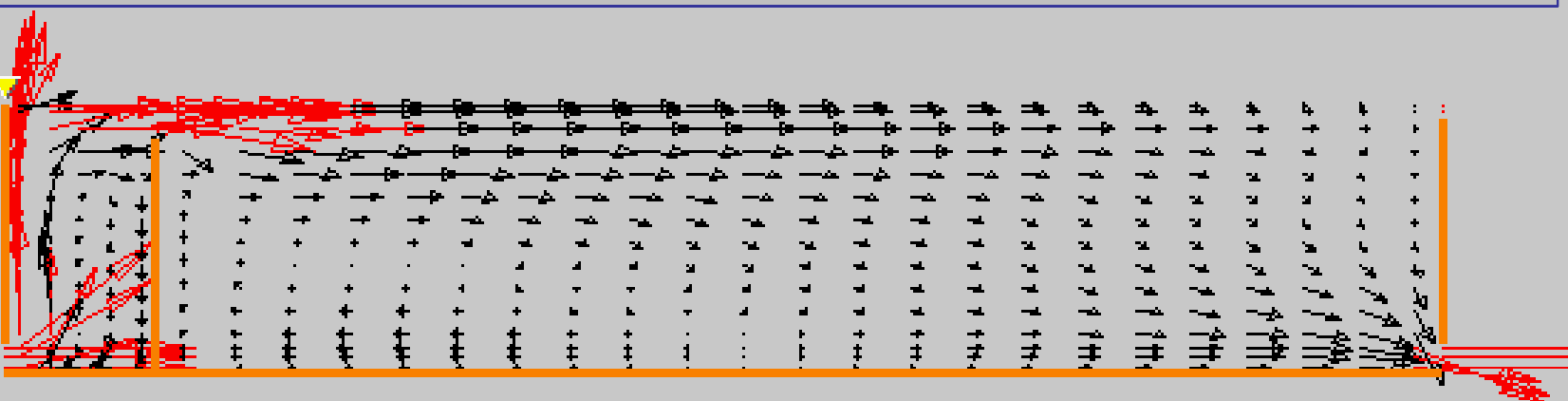
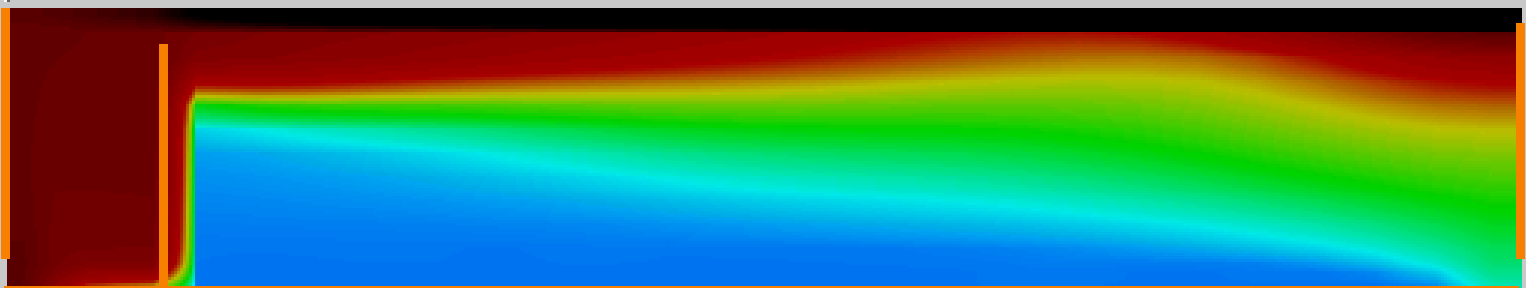
Is your clarifier operating at or below design capacity ?

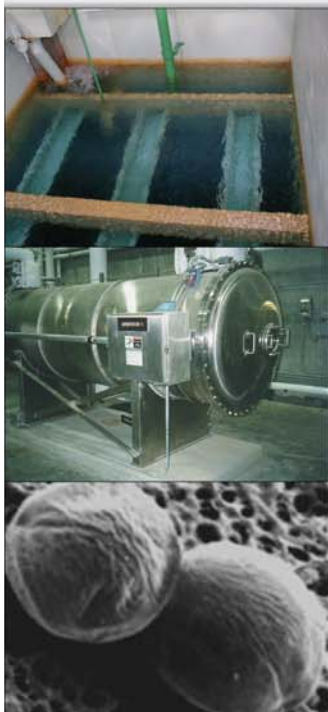
- Loading Rate – Flow per Unit Area, $\text{m}^3/\text{m}^2/\text{hr}$, or m/hr
- Typical Loading Rates
 - Traditional Sedimentation: Up to 4 m/hr
 - Conventional DAF: Up to 20 m/hr
 - High Rate DAF: 30 - 45 m/hr
 - ActiFlo: 40 - 60 m/hr
- Loading rate is an AVERAGE over the entire basin area
- Localized high velocities can cause major problems

Density Currents

- Generally worst in large sedimentation basins due to surface warming
- Can cause significant floc carryover

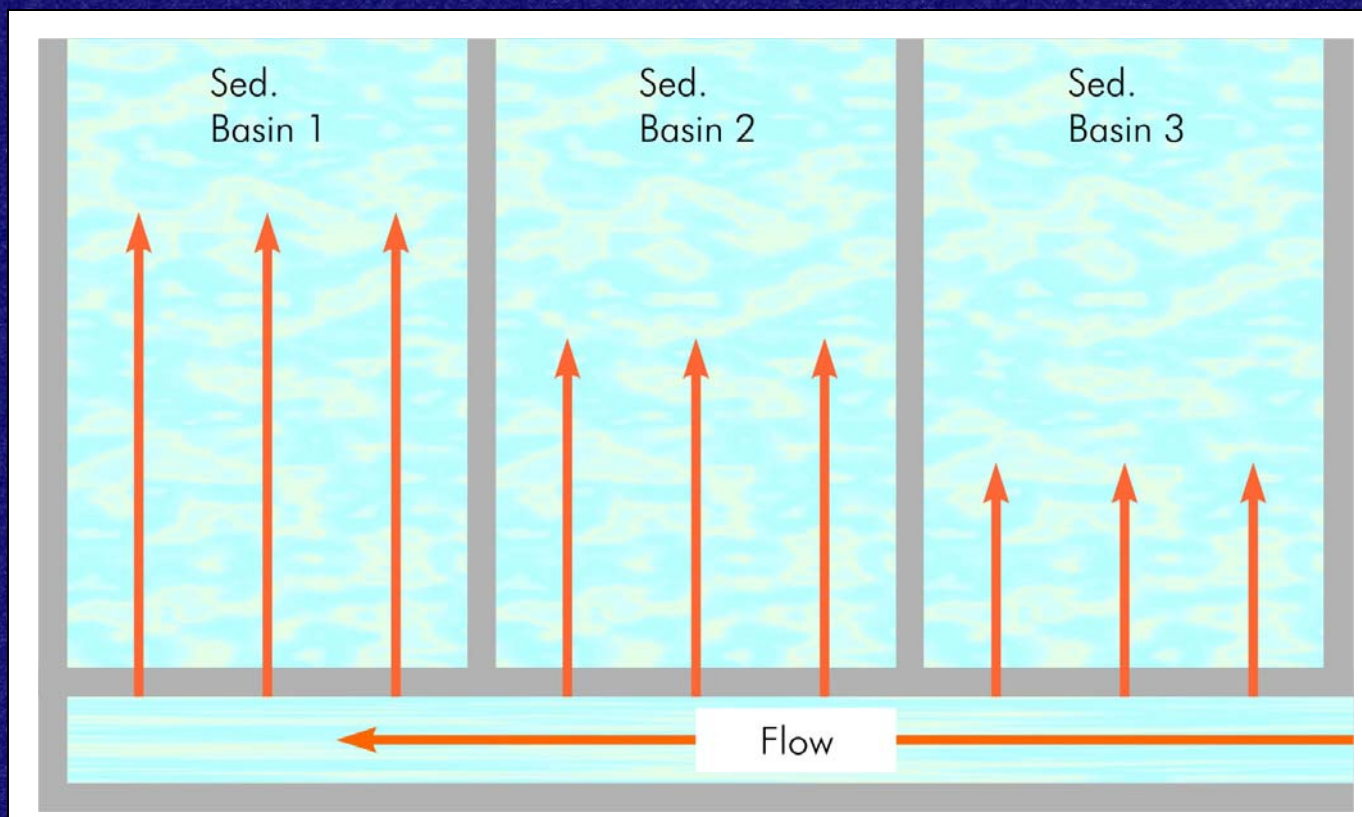






Inlet Flow Distribution

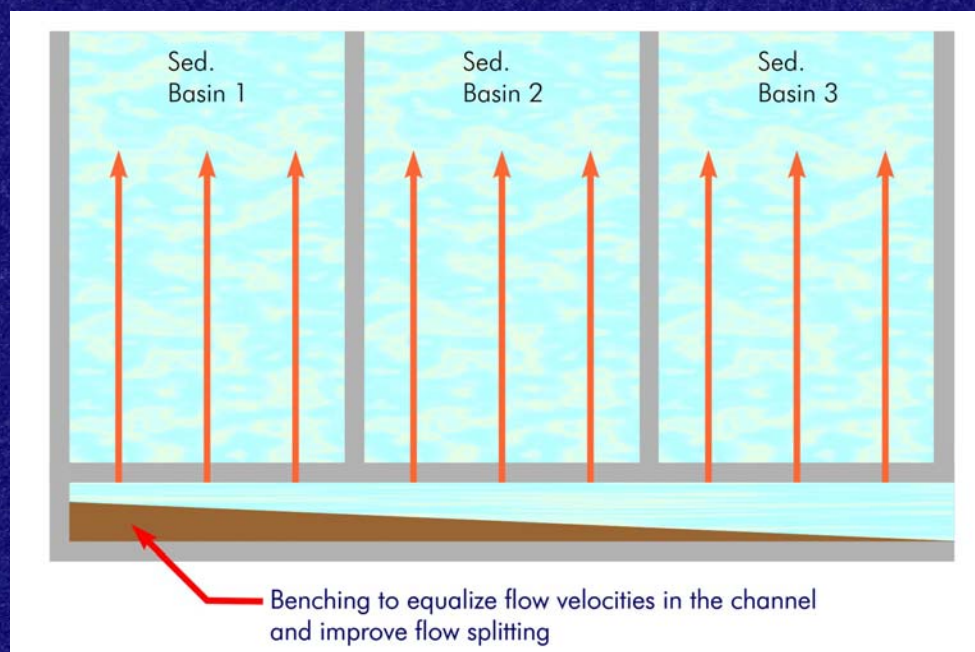
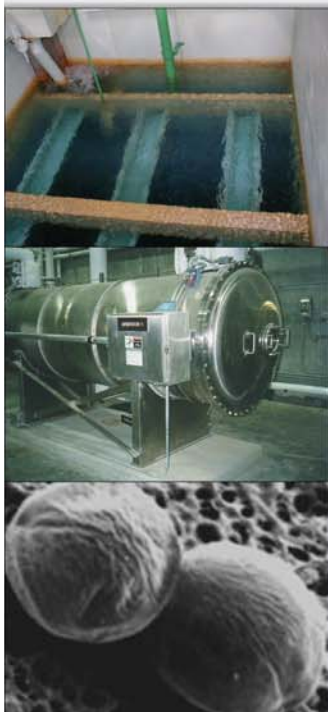
- Generally caused by poor inlet channel design
- Sometimes caused by uneven inlet weirs





Rectifying Mal-Distribution

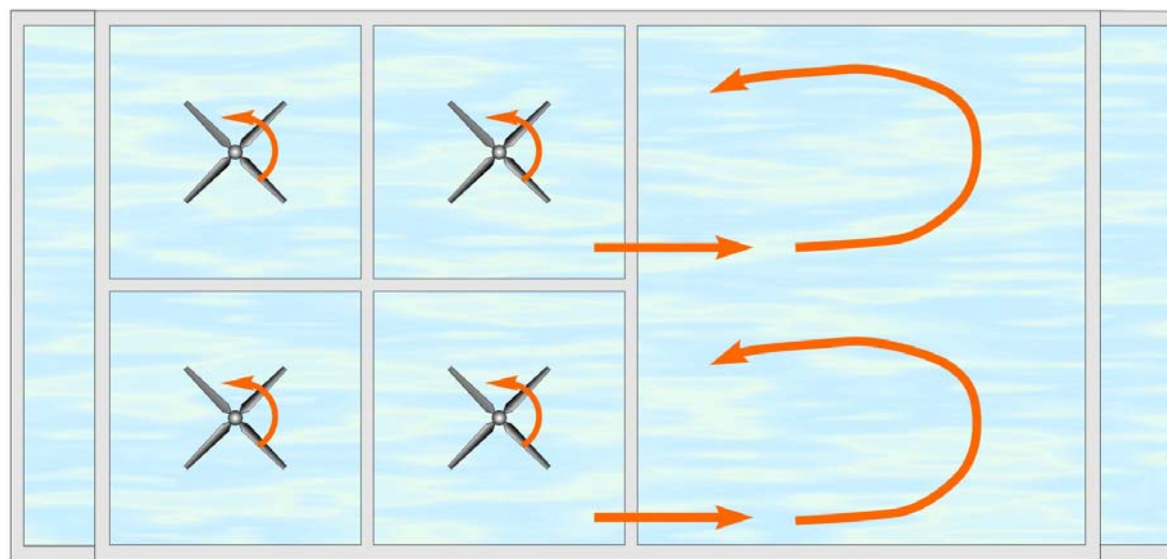
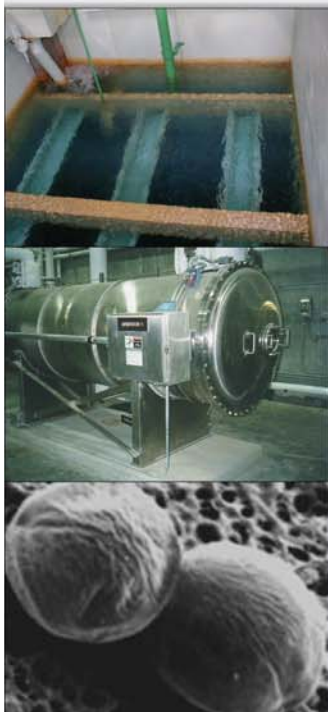
- Switch to flow meters and valves, but often there is insufficient head
- Modify the inlet channel to provide tapering and equalize velocities

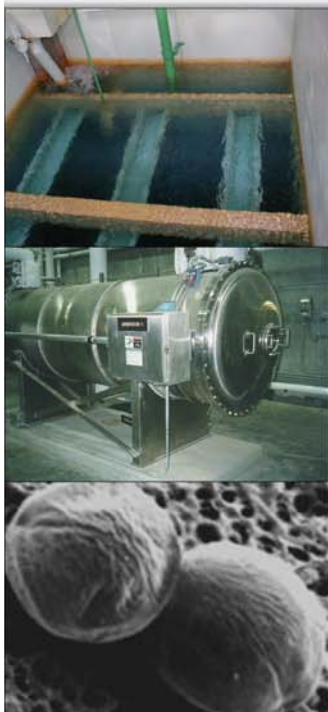




Clarifier Inlet Mal-Distribution

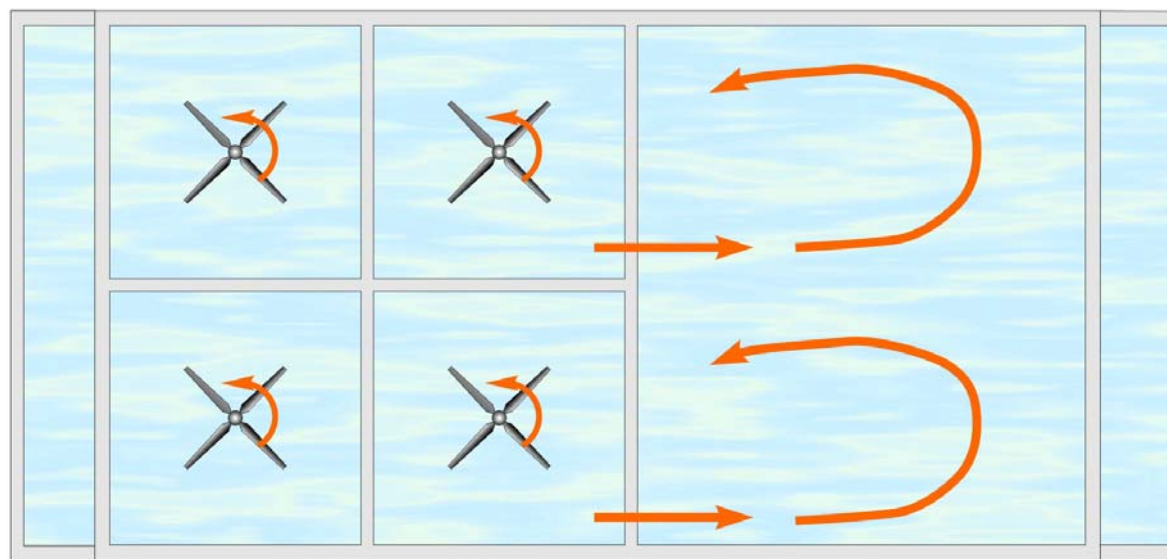
- Poorly designed flocculation basins can result in bulk circulation, resulting in high localized entry velocities





Clarifier Inlet Mal-Distribution

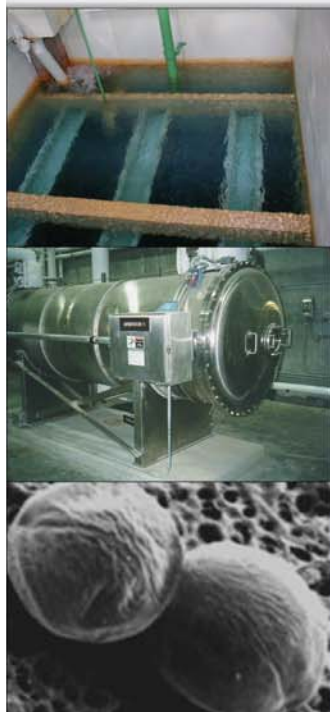
- Better flow distribution usually requires head loss to be introduced
- Mitigation can be difficult, without causing floc damage





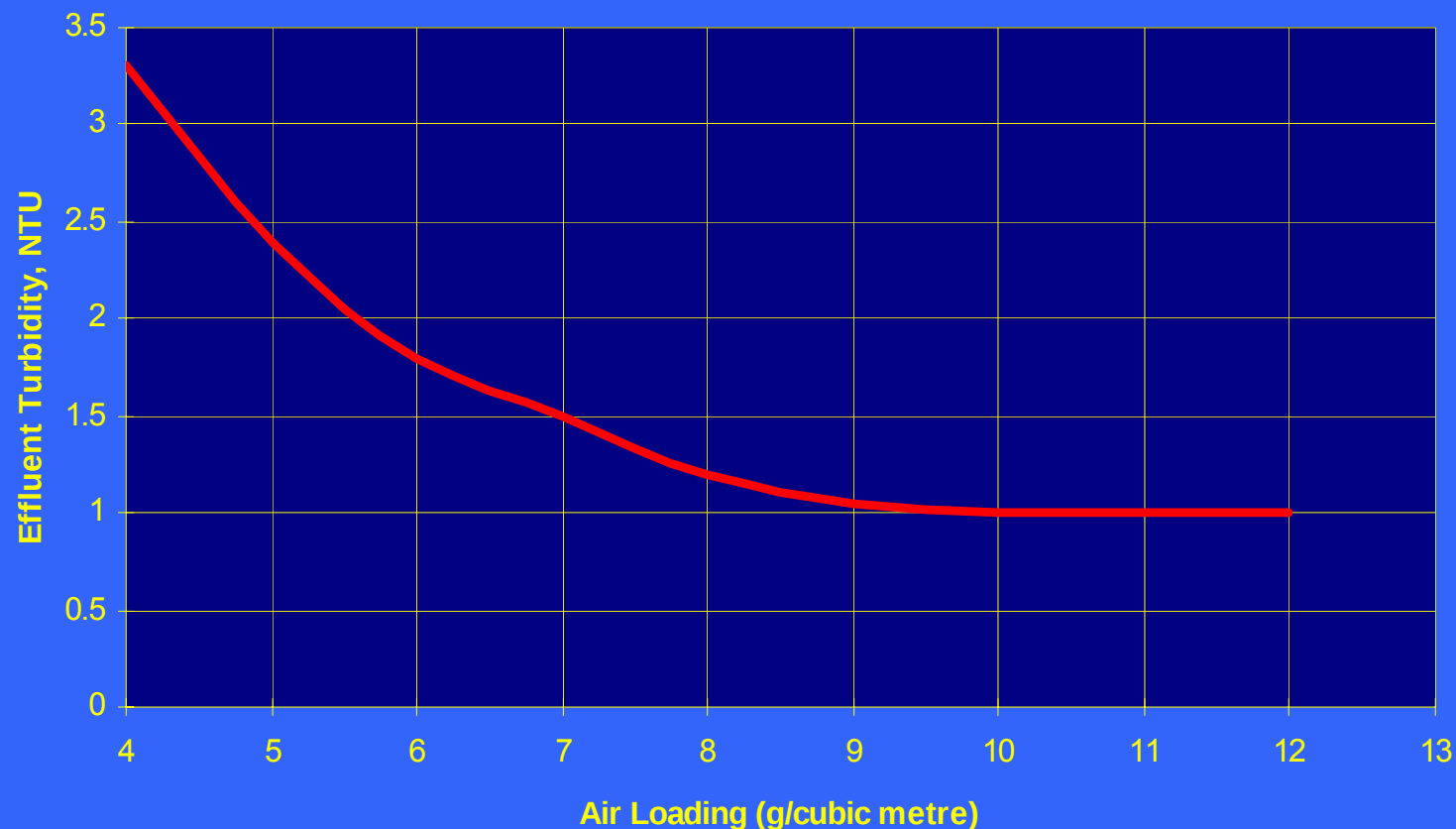
AWWOA Annual
Seminar

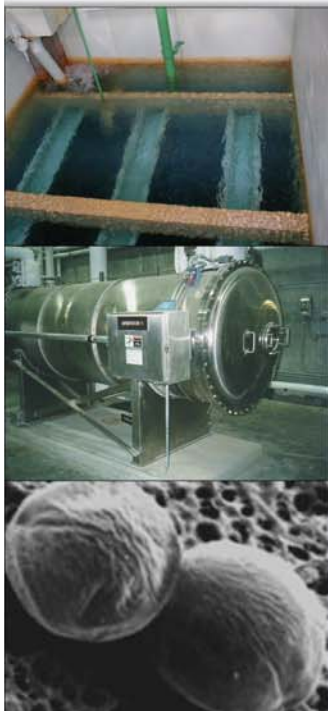
Banff, Alberta
March 15, 2006



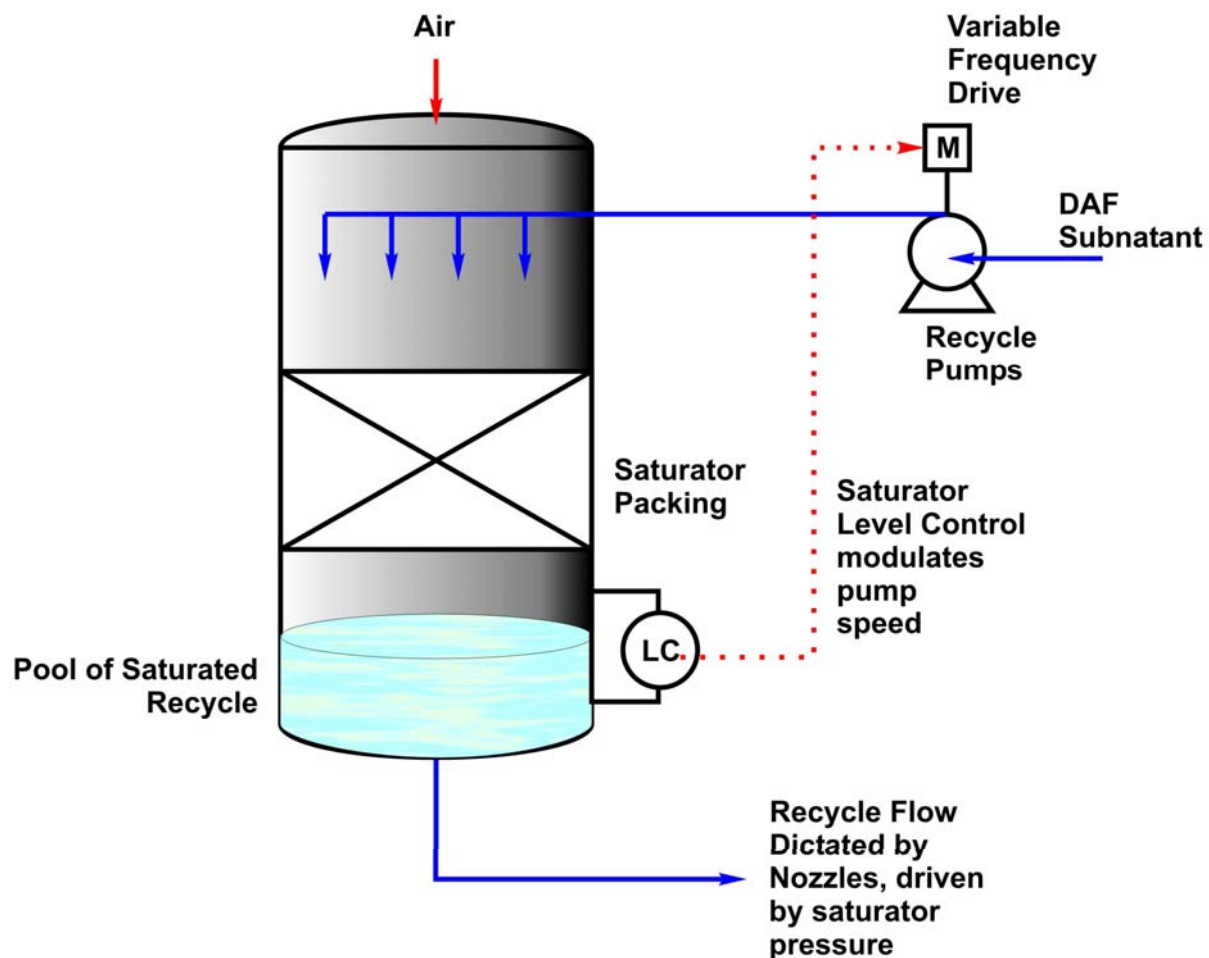
DAF Clarifiers: How Much Air is Enough ?

Effluent turbidity vs Air Loading
(Data of Zabel, 1978)





DAF Saturator Control





AWWOA Annual
Seminar

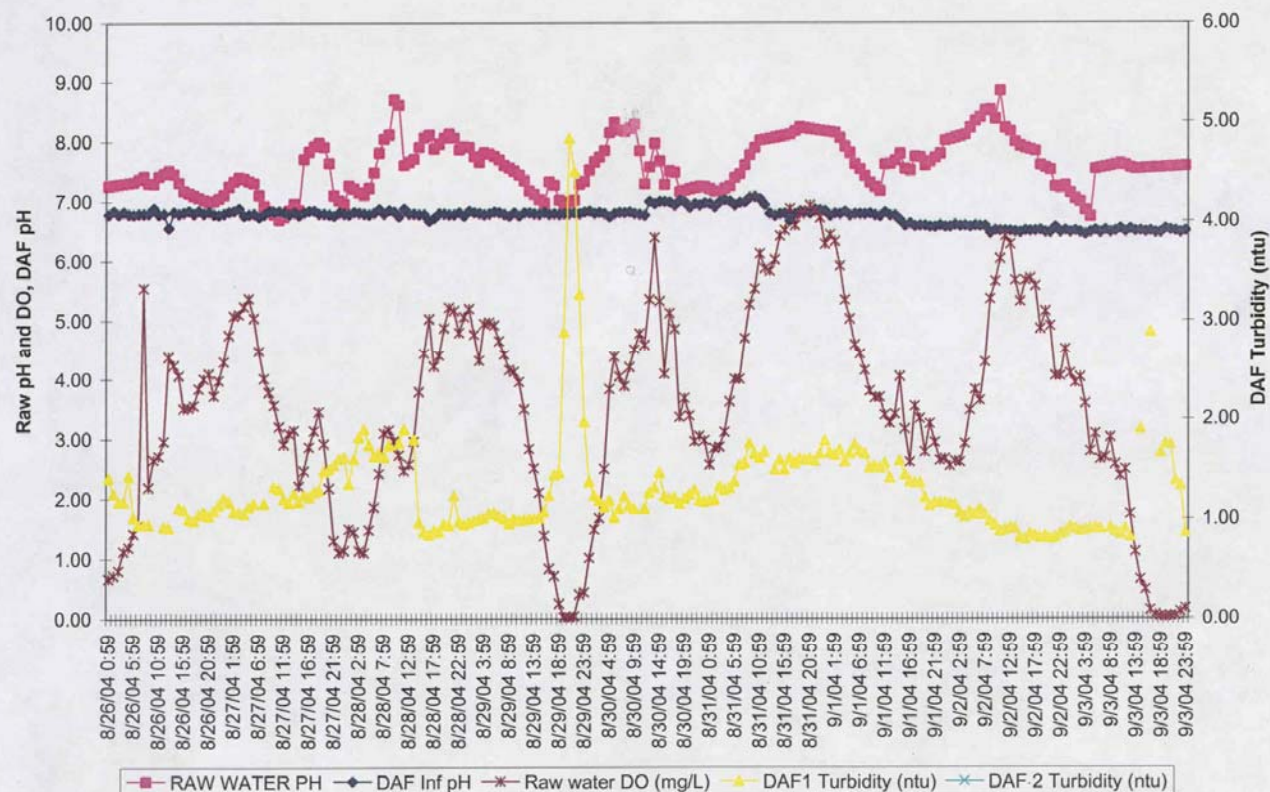
Banff, Alberta
March 15, 2006



Not enough air is a bad thing !!

8_26_9_3

8/26 - 9/3 LDF DAF Performance





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Entrained Air Problems



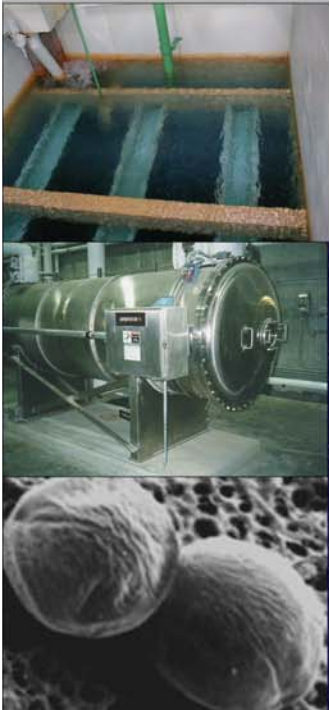
Clarifier performing
well in early morning

Launders and
Inclined Plates
readily visible



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



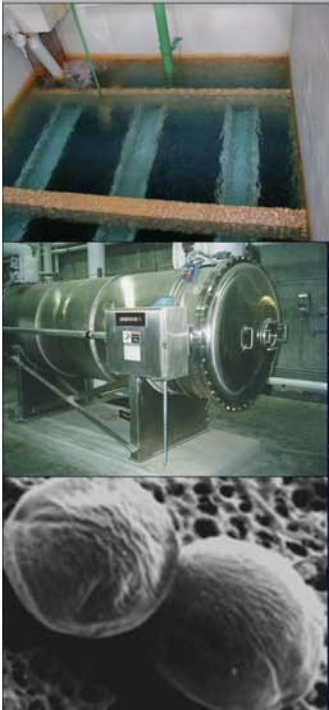
.....starting to deteriorate !!!





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



...and getting worse !!!





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



This is a sedimentation basin ??





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Extended downtime for cleaning !!!





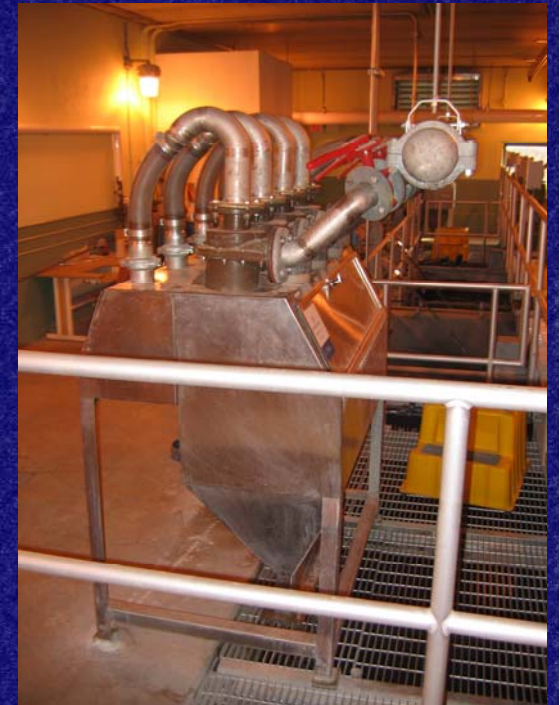
AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



ActiFlo Operational Issues

- Control of hydrocyclones to adjust waste flows
- Control of polymer dosing crucial:
 - Under-dosing = floc carryover
 - Over-dosing = polymer carryover
- Sand Concentration
 - Generally aim for 3 – 5 g sand/L
 - John Meunier trying to develop an on-line sand concentration analyzer ?





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Granular Media Filtration



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



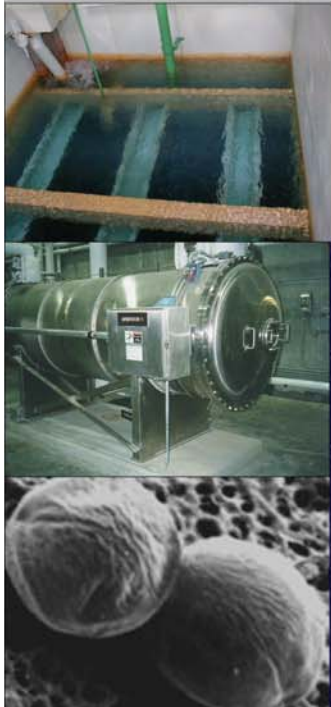
What constitutes “good” filter performance ?

- Consistently less than 0.3 NTU
- Particle counts < 50 particles/mL
- > 2-log removal of *Giardia* and *Cryptosporidium* sized particles
- Long and predictable filter runs (24+ hours)
 - Same for each filter
- Minimal premature particle breakthrough
- Poor performance can be difficult to rectify, but many issues can be resolved with simple fixes



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



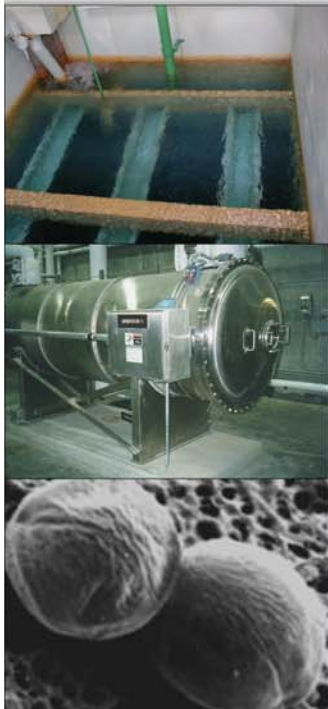
What constitutes “good” filter design ?

- Most efficient media design has largest media at the top, and the finest at the bottom
- However, backwashing immediately re-classifies bed to place the finest grains at the surface
- Therefore use multi-media to mimic this effect, with coarse grains in the top layer to trap solids, and finer layer below for polishing



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



What constitutes “good” filter design ?

- “Conventional” Filter Design
 - Typical Loading Rates 6 – 9 m/hr. Higher possible with pilot testing
 - Total Media Depth ≤ 1 m
 - Anthracite: ES 0.8 – 1.2 mm, UC 1.4 – 1.65
 - Sand: ES 0.45 – 0.55 mm, UC 1.4 – 1.65
- “Deep Bed” Filter Designs
 - Typical Loading Rates much higher, relying on chemical dosing to a greater extent
 - Total Media Depth 2 – 3 m
 - Anthracite: ES 0.8 – 1.2 mm, UC 1.4 – 1.65
 - Sand: ES 0.45 – 0.55 mm, UC 1.4 – 1.65



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

Filter Auxiliary Cleaning

- Air Scour
 - Air flow: $0.9 - 1.5 \text{ m}^3/\text{min}/\text{m}^2$
 - Air scour provides a vigorous cleaning action, due to “collapse pulse” action
- Surface Wash
 - Generally falling out of favour, but common in older filters
 - Typical Flows:
 - Fixed nozzles: $5 \text{ m}^3/\text{m}^2/\text{hr}$
 - Rotating Arms: $1.2 \text{ m}^3/\text{m}^2/\text{hr}$





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Good Filter Design Practice

- If dual-media is used, media should be hydraulically compatible to reduce intermixing:

$$\frac{d_1}{d_2} = \left[\frac{(\rho_2 - \rho_{water})}{(\rho_1 - \rho_{water})} \right]^{\left(\frac{2}{3}\right)}$$

$\rho_1, \rho_2, \rho_{water}$ = Density of Media 1, Media 2, and water

d_1, d_2 = Diameter of Media 1, Media 2



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



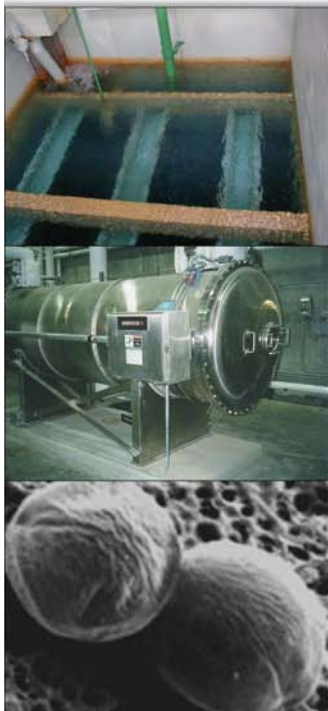
Good Filter Design Practice

- The important thing to remember is that all media should be selected to share a common fluidization velocity
- This minimizes intermixing of media layers
- Severe intermixing causes short filter runs by reducing void volume in upper layer of filter
- Note: Media characteristics can change over time:
 - Encrustations
 - Deposition
 - Physical degradation of media grains (wear)

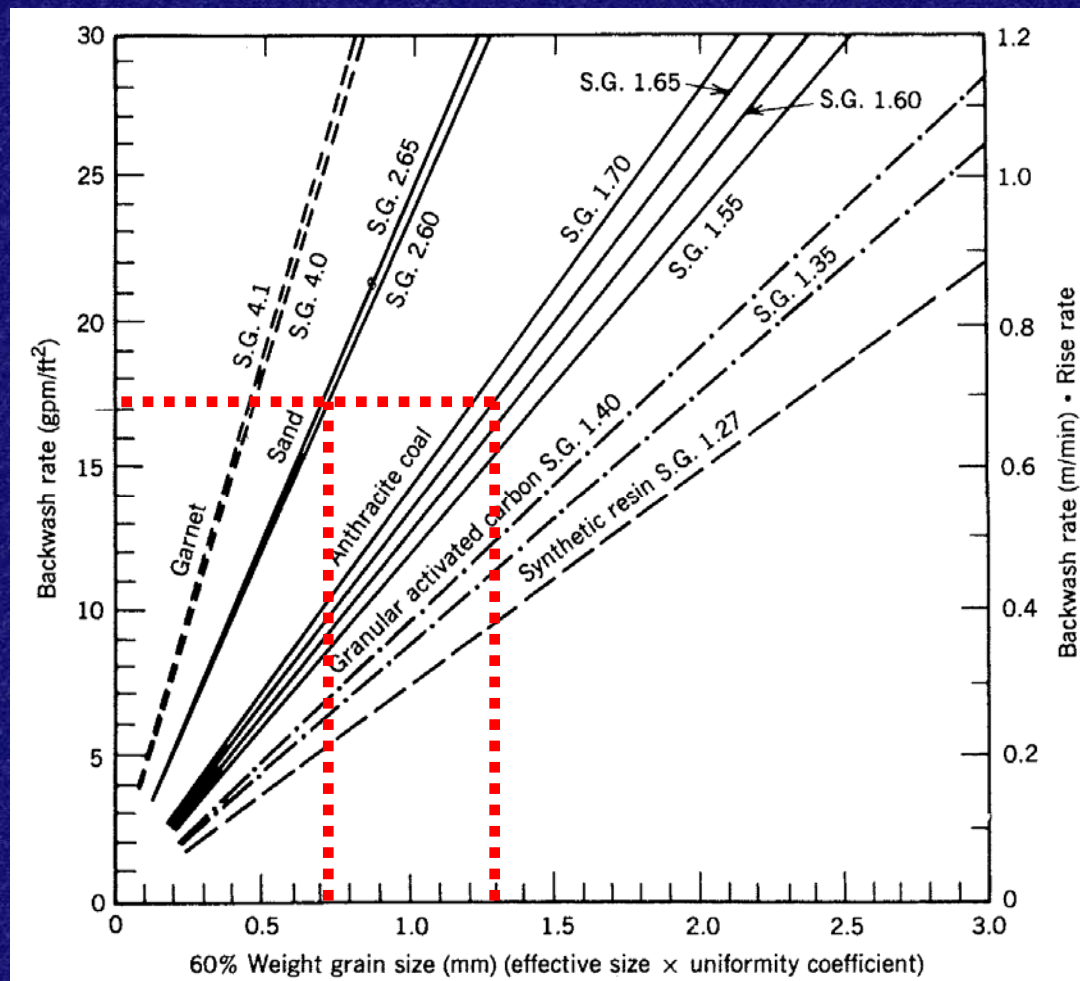


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Appropriate Backwashing Rates

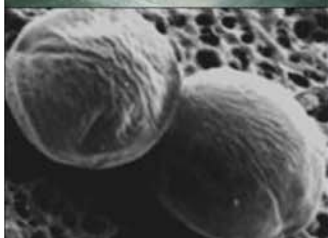


Note: Rates are at 20C, and must be adjusted for other temperatures

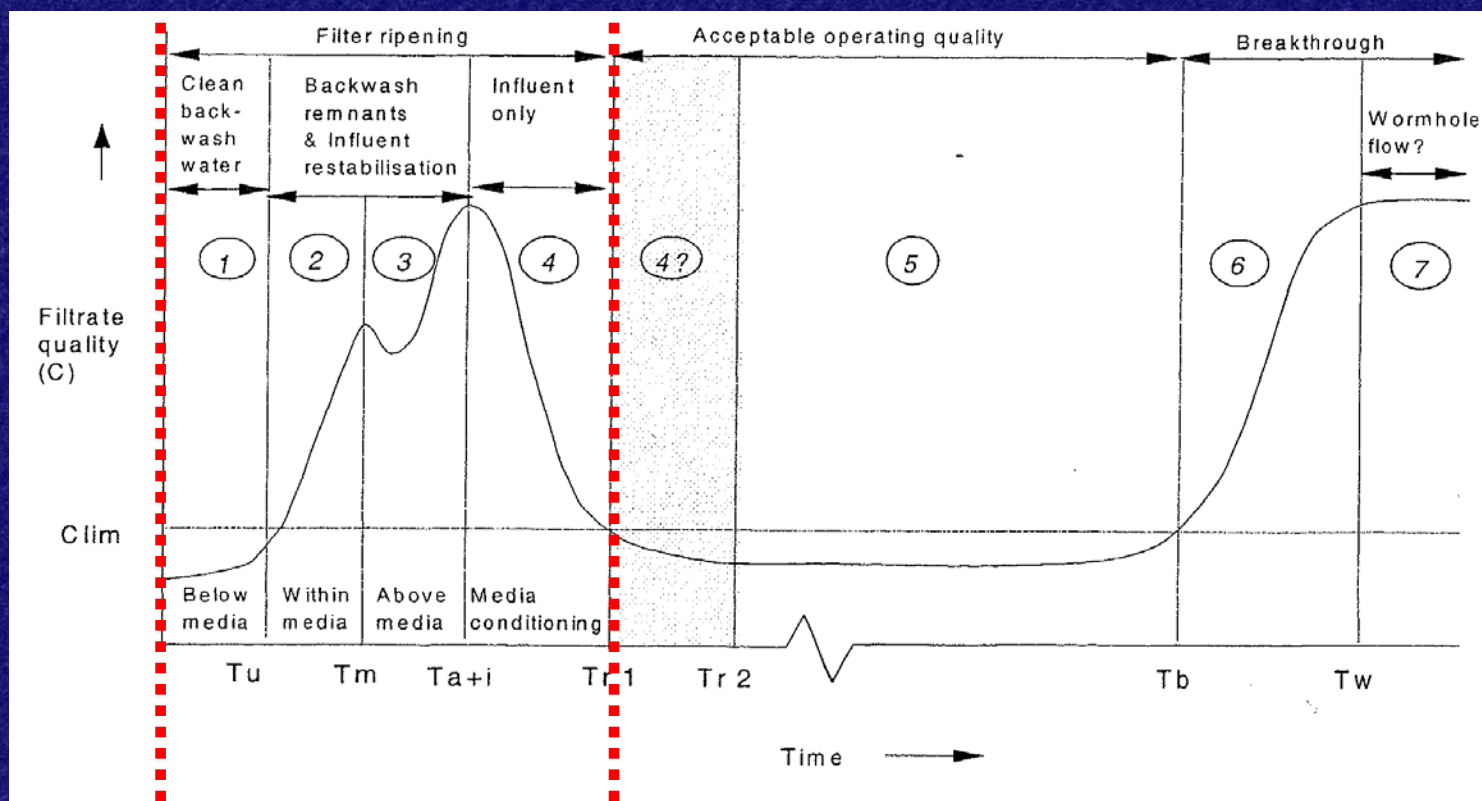


AWWOA Annual Seminar

Banff, Alberta
March 15, 2006



A Typical Filter Run



Filter-to-Waste will
improve overall
filtered water
quality



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Granular Media Filtration

Common Problems

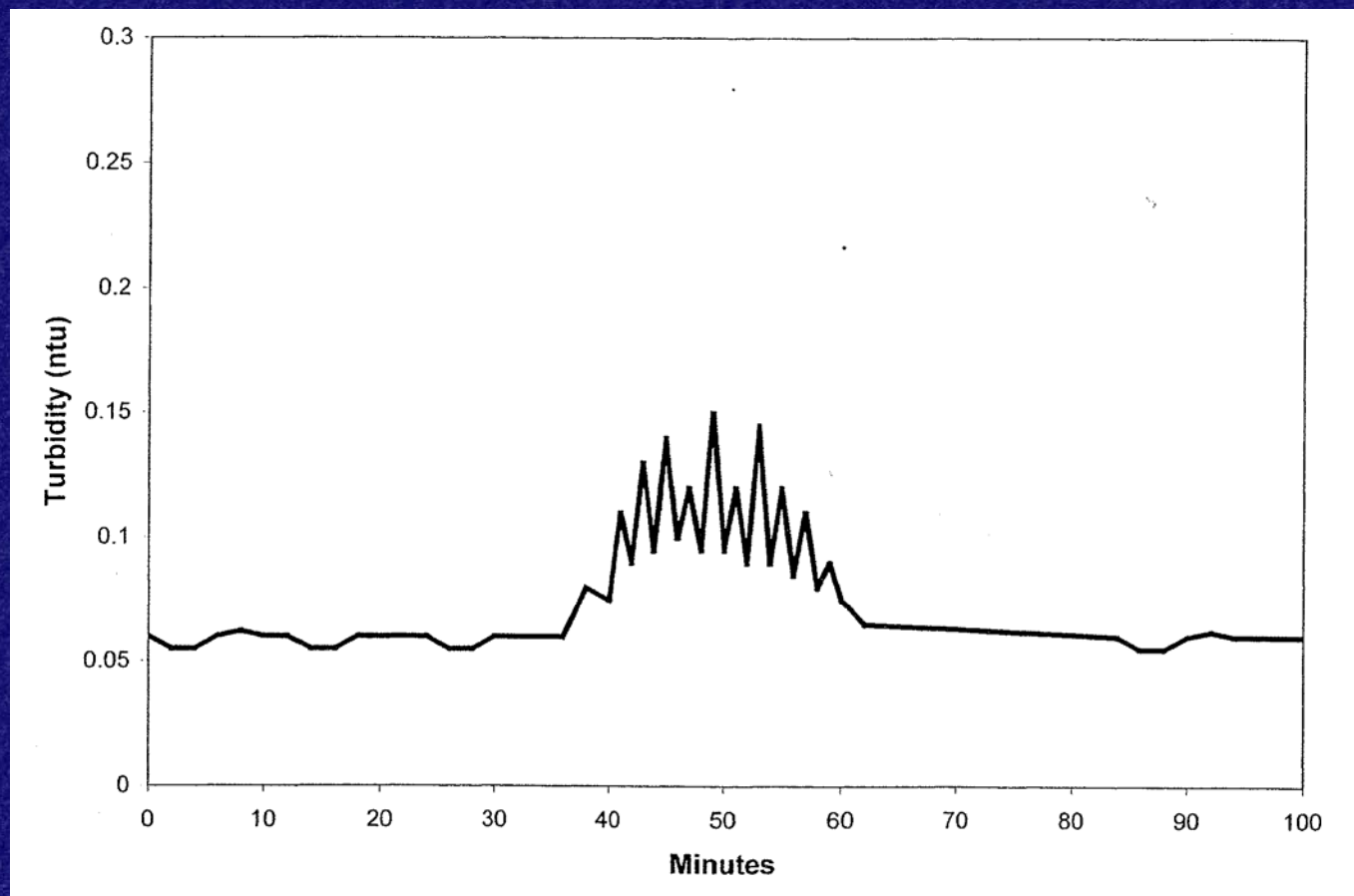


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Filter Issues – Valve Hunting



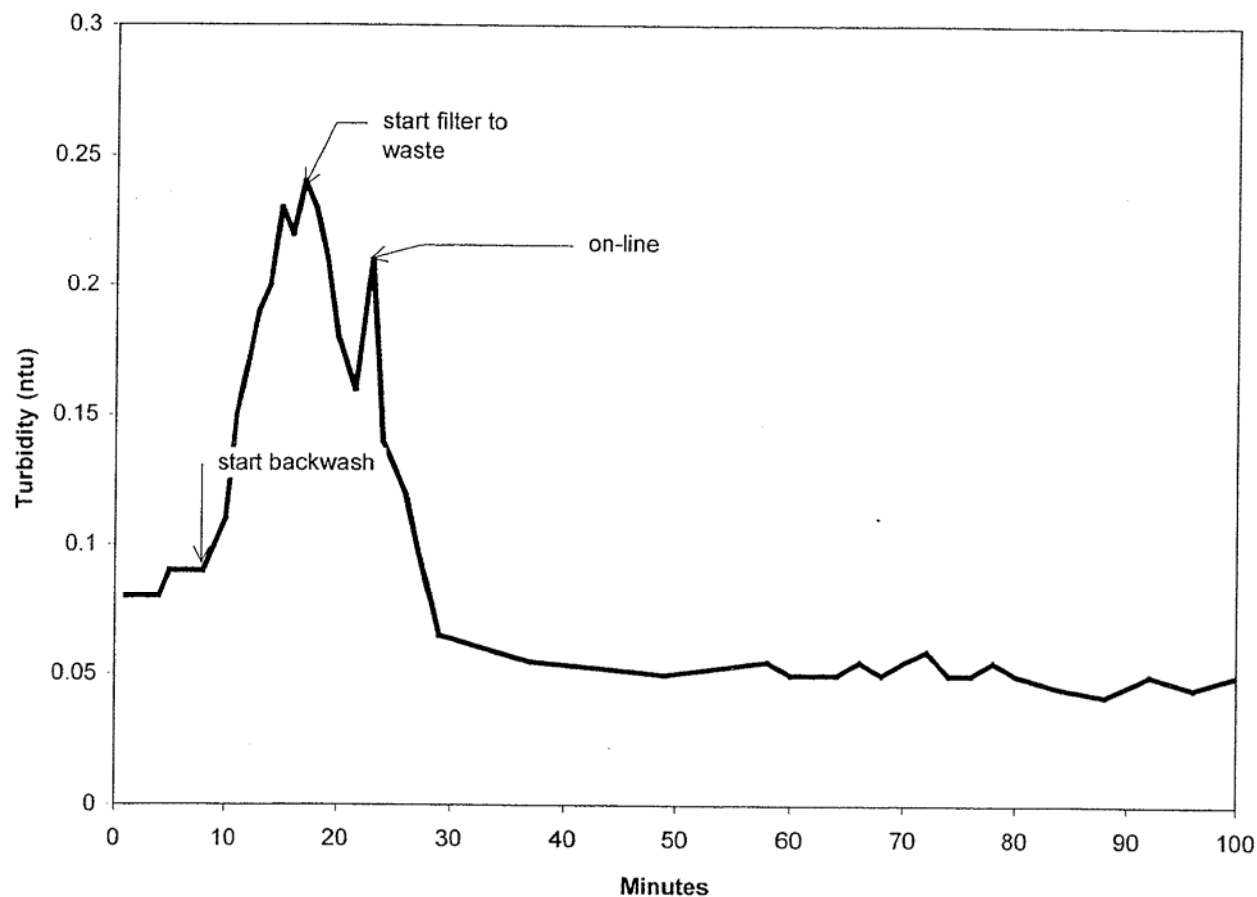


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Filter Issues – Initial Turbidity Spike



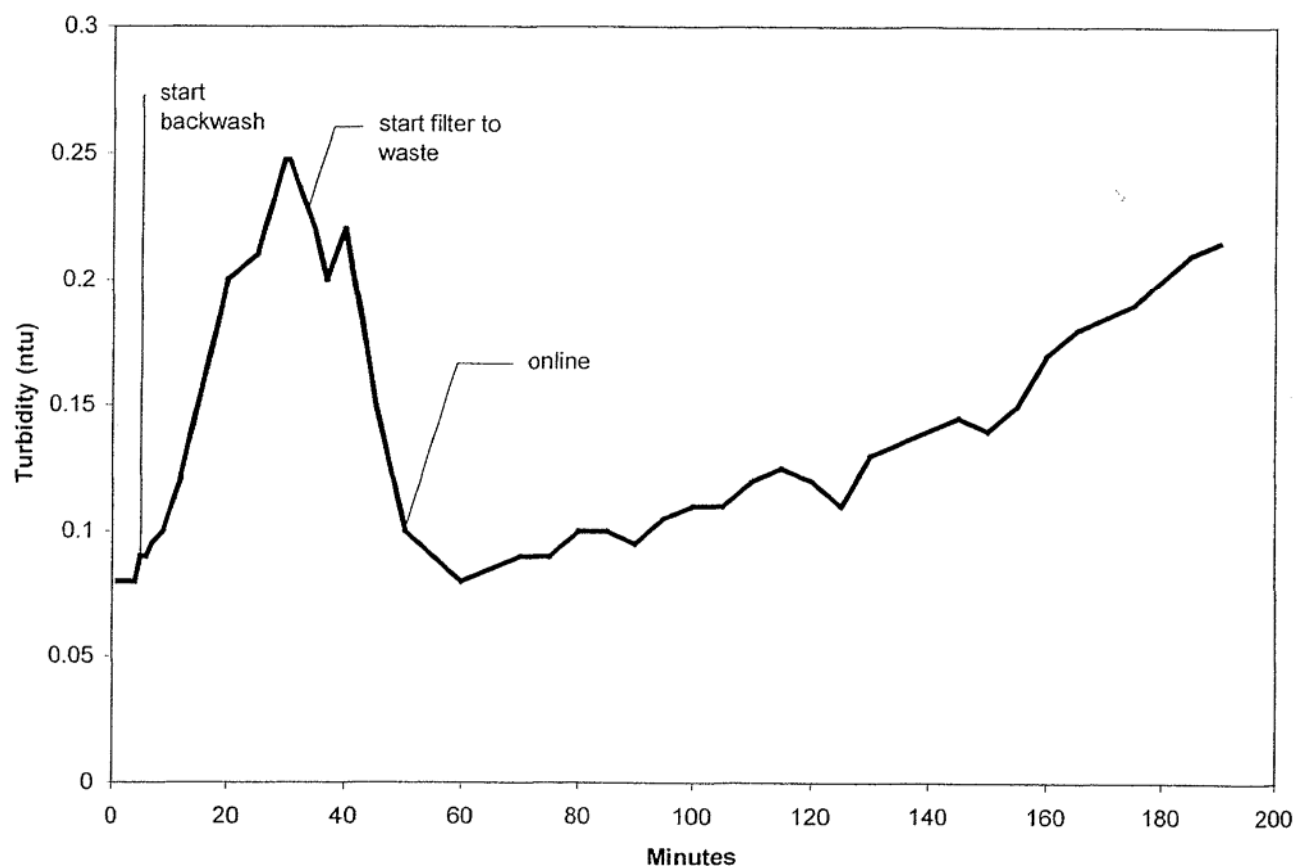


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Filter Issues – Effluent Turbidity “Creep”



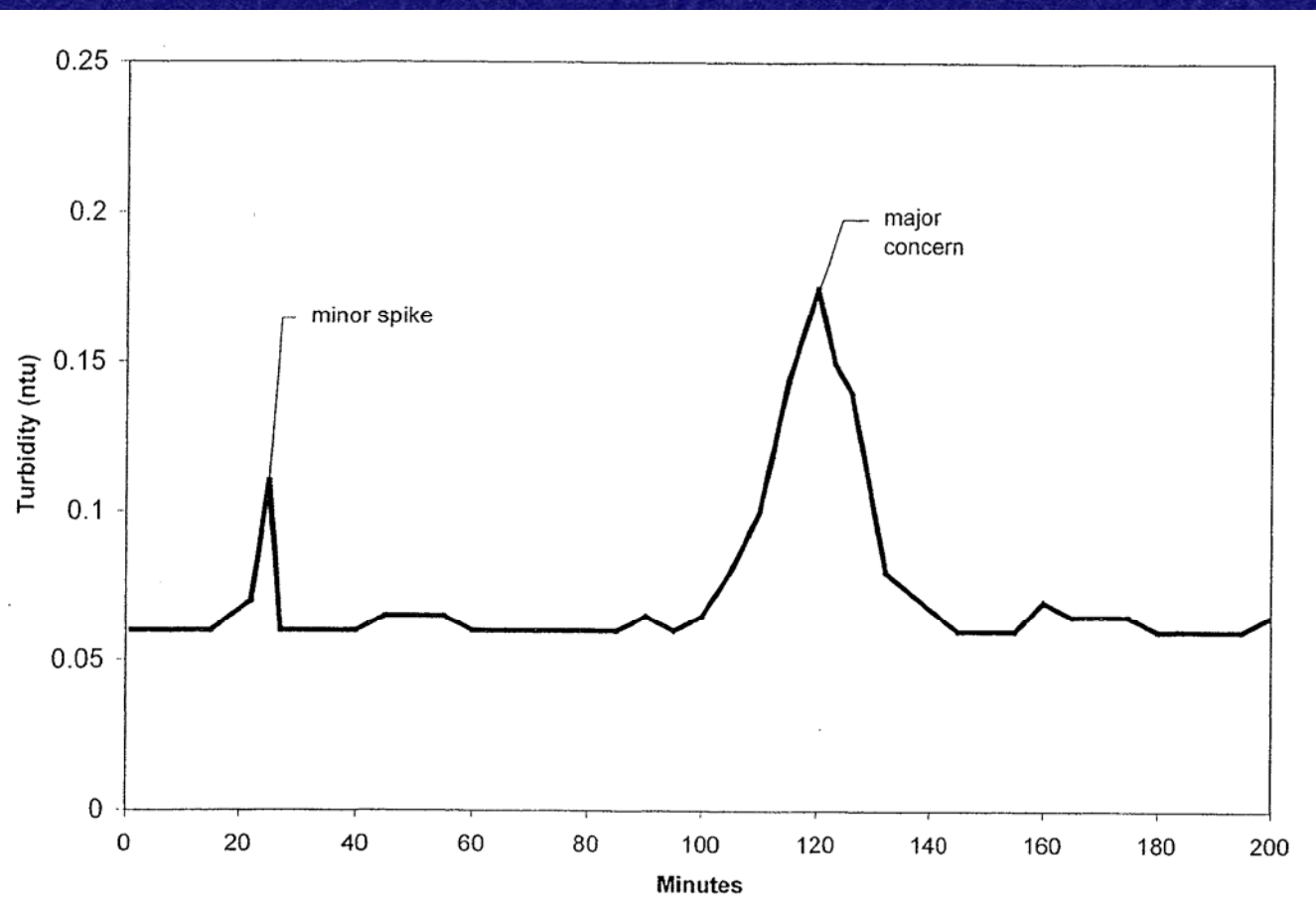


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

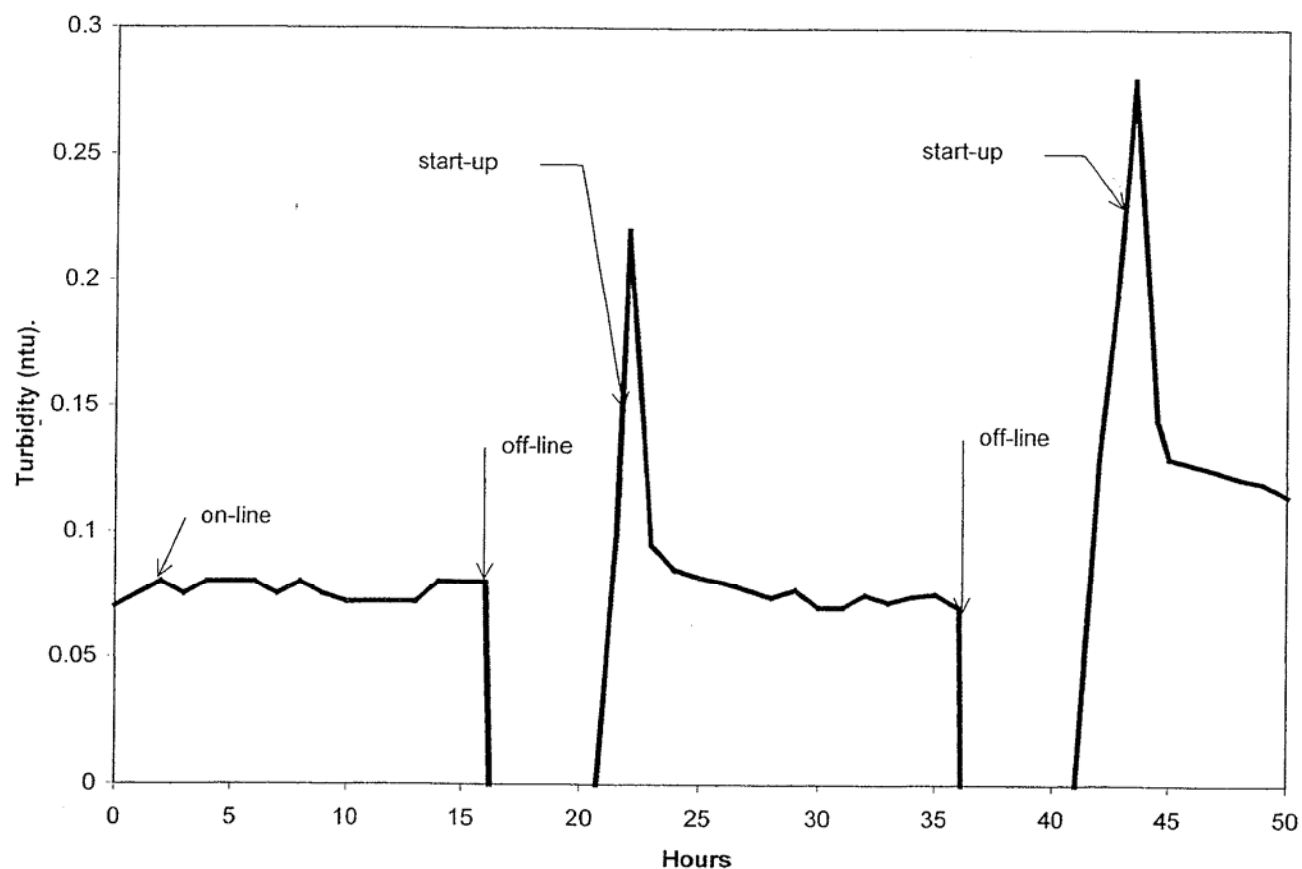


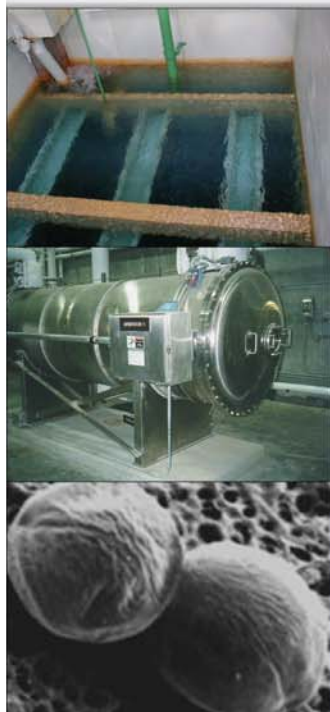
Filter Issues – Spiking during Run





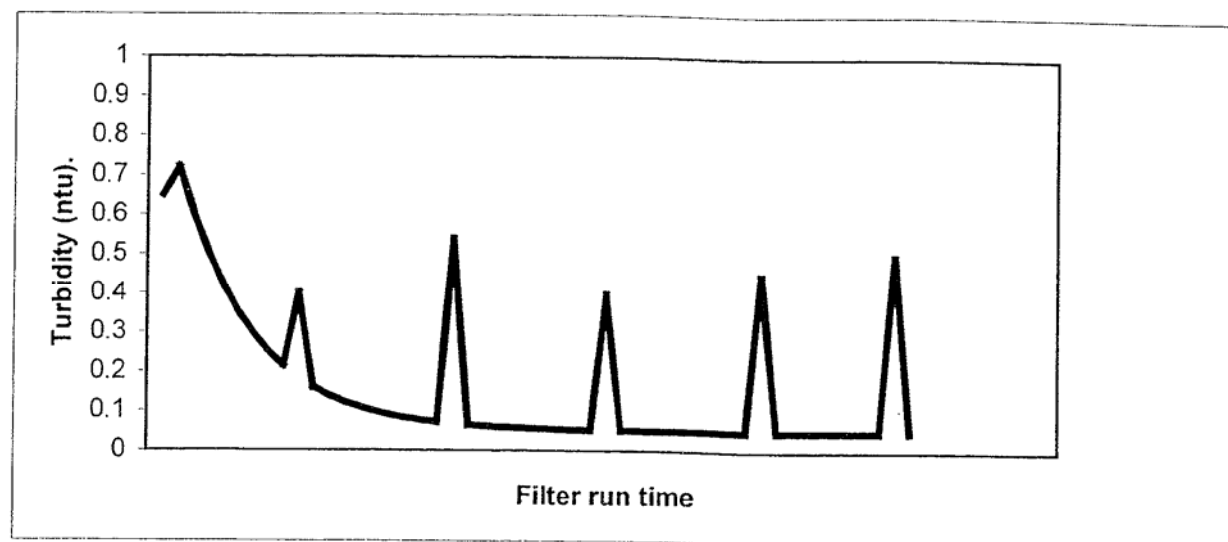
Filter Issues – Hydraulic “Shock”





Filter Issues – Spiking during Backwash

- Backwashing of other filters increases flow to remaining filters
- Short term hydraulic shock dislodges particles



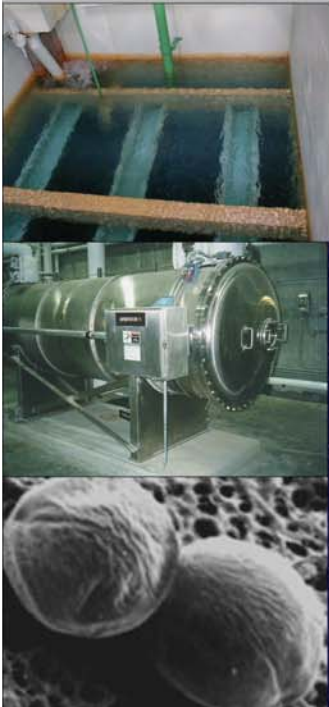


AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006

Premature Particle Breakthrough

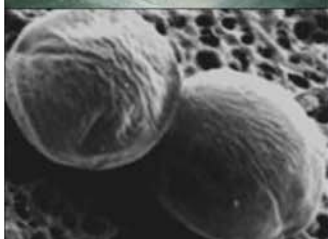
- Increases in filtered water particle concentrations are common near the end of a filter run – Well before turbidity breakthrough
- Passage of pathogens may occur before a turbidimeter “notices”
- Particle counting may be a more appropriate trigger for backwashing than turbidity measurements



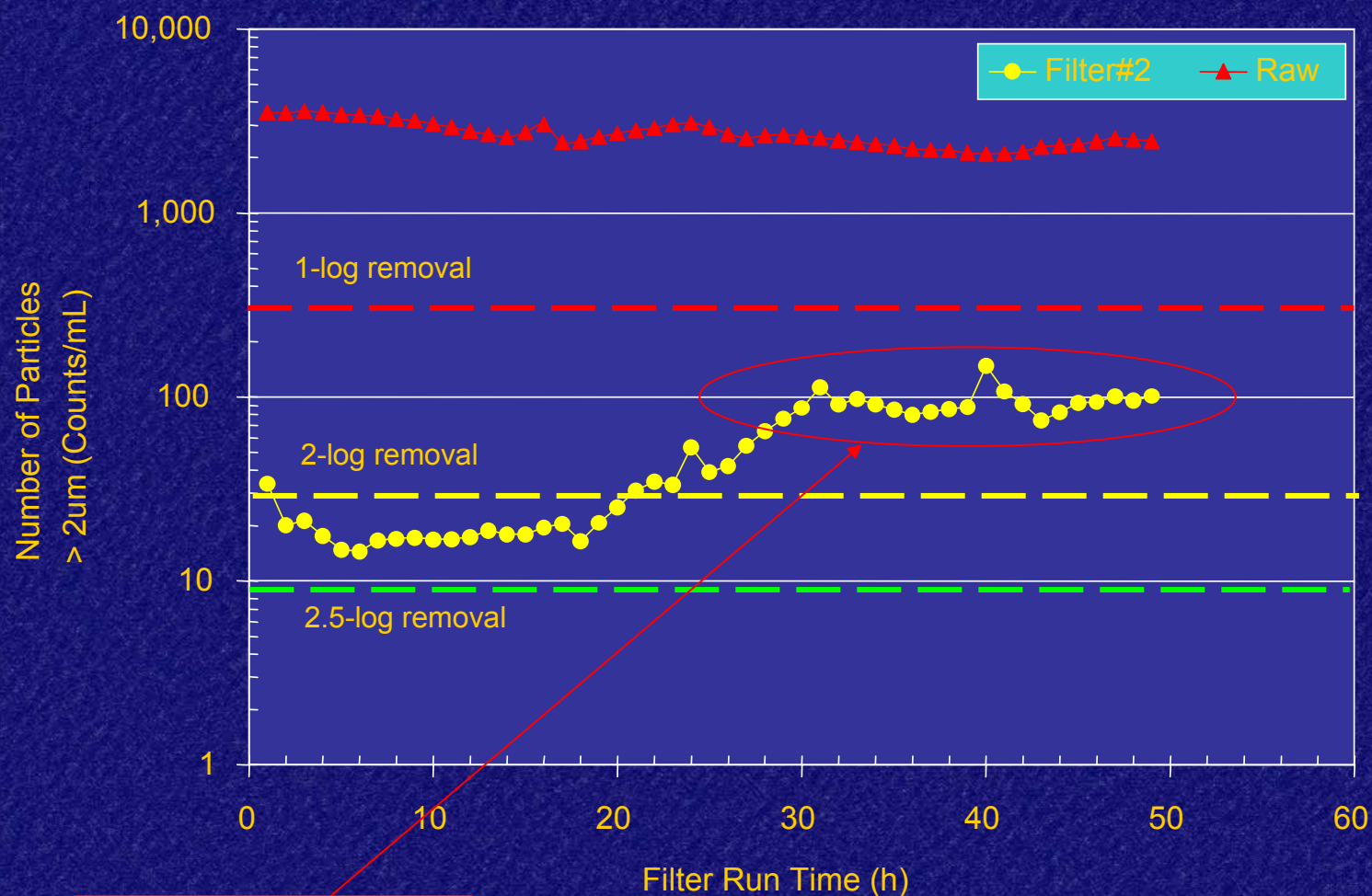


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Particle Count Data is particularly sensitive for filter monitoring



Filters are at 1.5 log removal
for latter part of filter run



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Common Causes for Poor Filter Performance

- Poor clarifier performance – Excessive solids loading
- Excessive operational loading rates
- Lack of FTW capability
- Sudden changes in flow to filter – Hydraulic “shock”
- Filter media loss or upset
- Filter underdrain damage or failure
- Poor cleaning effectiveness
 - Mudballing
 - Short circuiting



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Granular Media Filtration *Evaluation & Optimization*



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Granular Media Filters Evaluation Techniques

- Visual Inspection
- Filter Surveying
 - Filter Indices
 - Unit Filter Run Volume
 - Filter “Efficiency”
- Filter Core Sampling
- Backwash Waste Characterization
- Floc Retention Profiling
- Backwash Trough Level Check
- Remember – **SAFETY FIRST**





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Filter Evaluation Safety Issues

- Never walk directly on filter media
- Ensure filter is FULLY drained before entering filter box
- Beware of filter appurtenances – Wear a hard hat
- Use a safety harness where applicable, particularly during bed fluidization testing

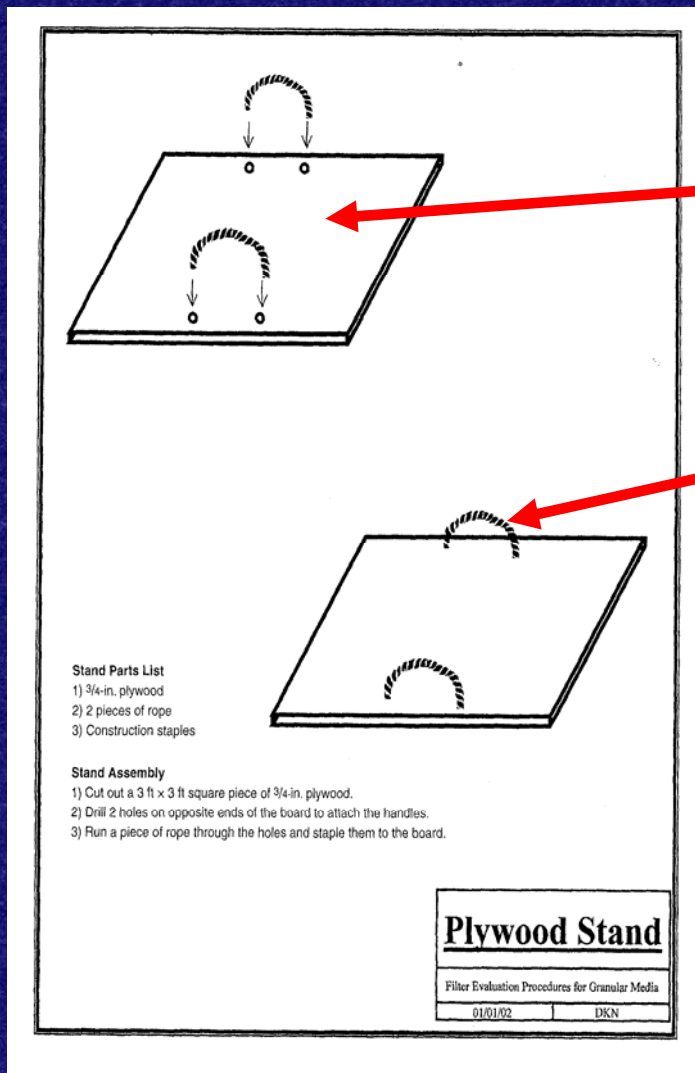


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Homemade Device for Walking on Filter Media



$\frac{3}{4}$ " Plywood Sheeting

Rope Handles

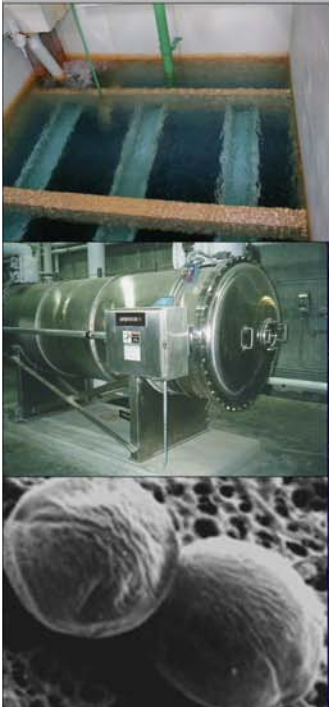


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

Filter Indices

- Unit Filter Run Volume (UFRV)
 - A measure of **NET** filter production per unit filter area per filter run
 - $\text{UFRV} = \text{Filtration Rate (m/hr)} \times \text{Filter Run (hr)}$
 - UFRV of 300 – 500 m^3/m^2 is desirable
- L/d Ratio
 - Ratio of Filter Bed Depth to Media Nominal Diameter
 - In theory filters with the same L/d should perform equally under similar conditions
 - L/d ratio > 1,000 for conventional filters, > 1,200 if using filter aid
- Filter Efficiency – Similar to UFRV, but accounts for losses as waste. Filters should typically produce 2 – 4 % as waste





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Visual Observation of Filters

- The first line of defence in filter monitoring and evaluation
- Look for easy to recognize issues:
 - Media boiling during wash
 - Uneven wash distribution
 - Uneven overflow into BW troughs
 - Cratering in media surface
 - Visible mudballs
- Create a map of the filter and track observations for future mitigation



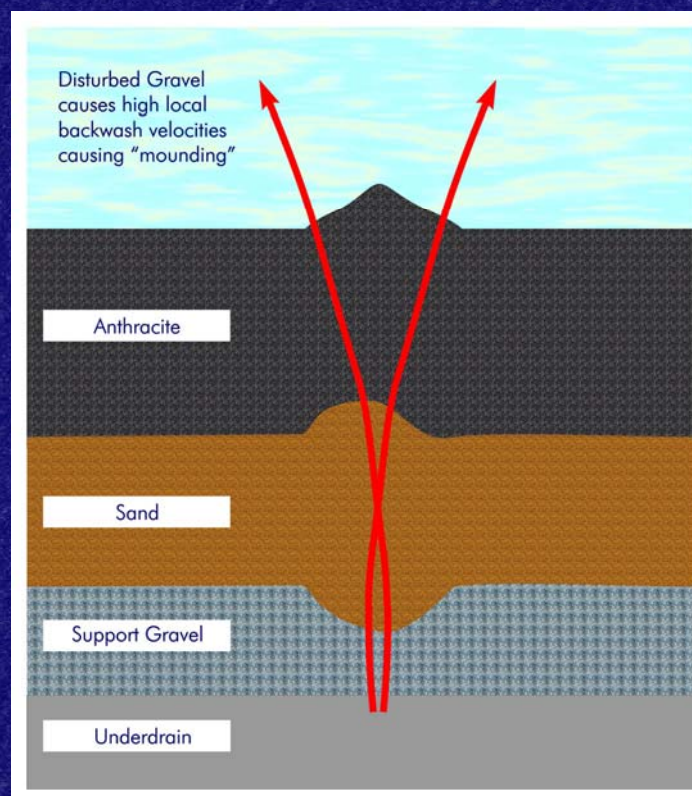
AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Visual Inspection - Mounding

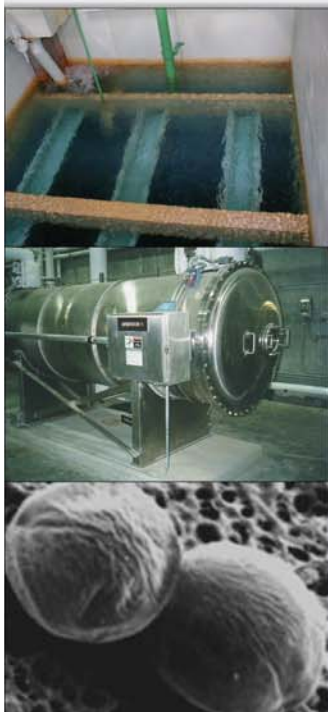
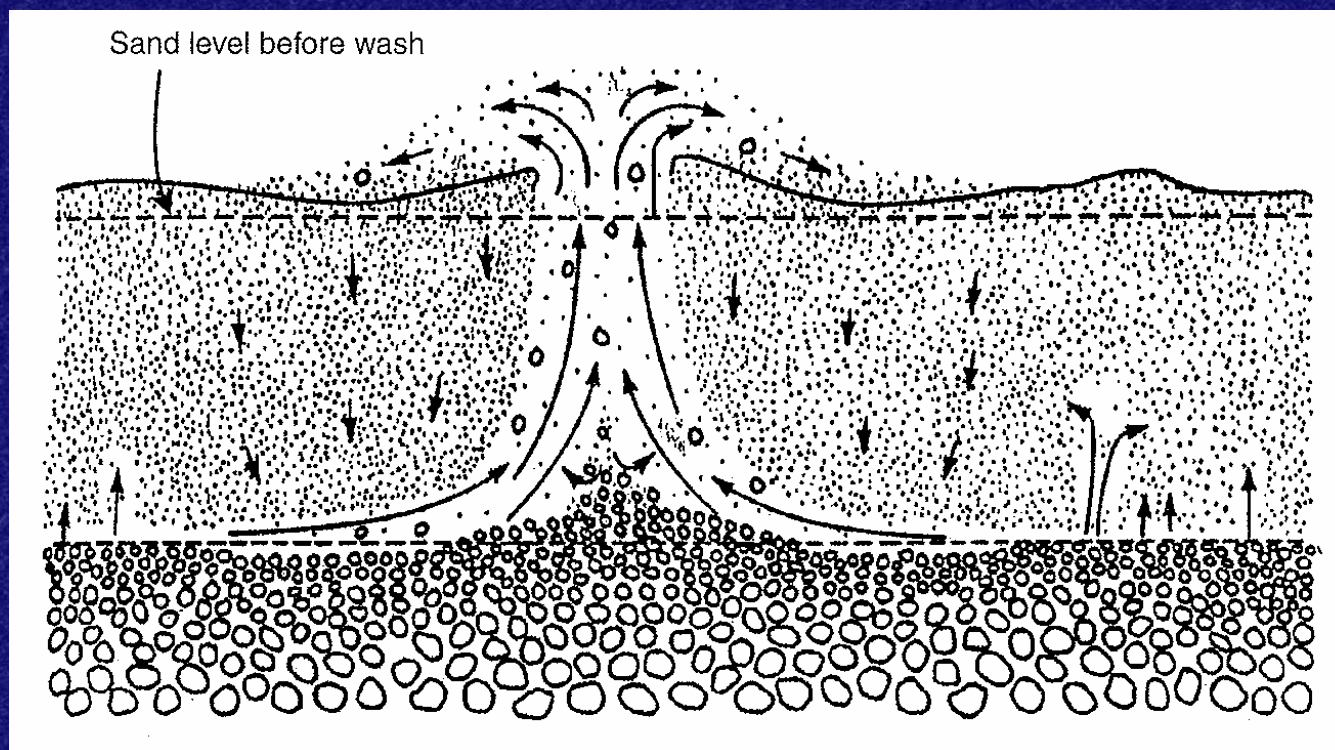
- “Mounding” of filter media surface –
Suggests possible disturbance in gravel
layer – High localized flow





Filter "Boiling"

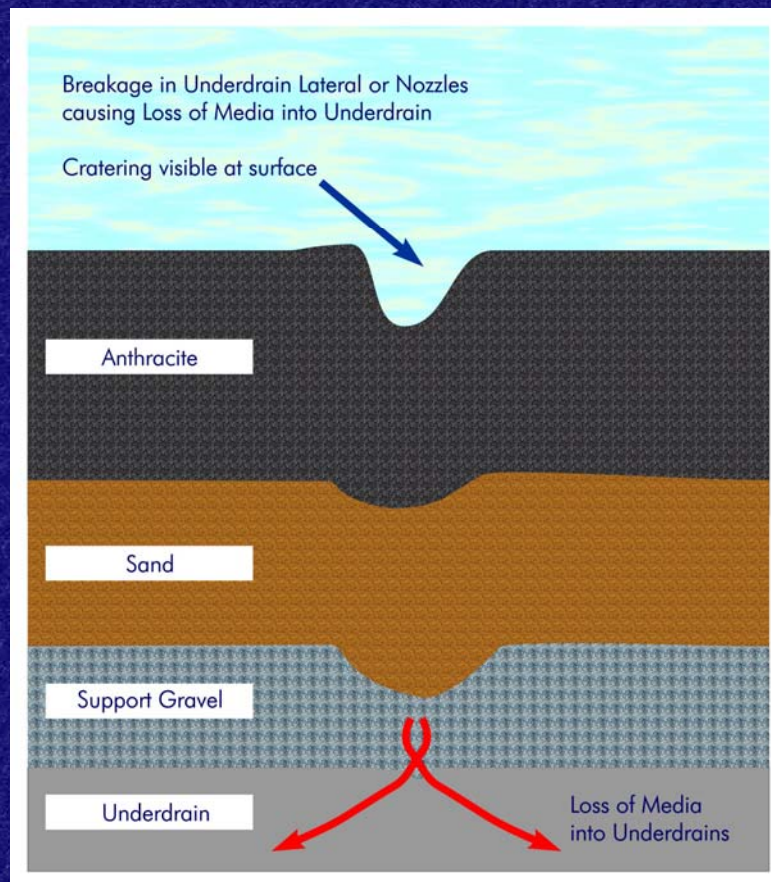
- Boiling is usually clearly visible during the early stages of backwash

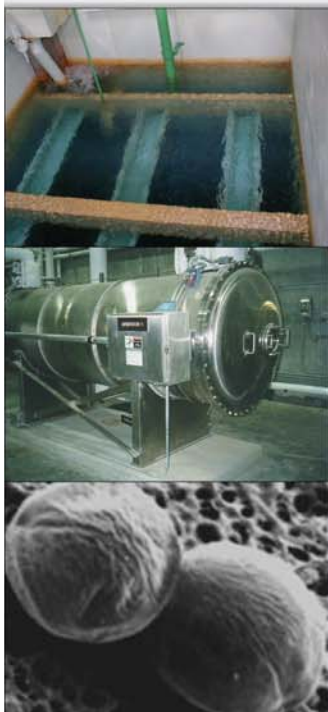




Visual Inspection - Cratering

- Cratering of filter media surface –
Suggests possible damage to underdrain





Visual Inspection - Mudballs

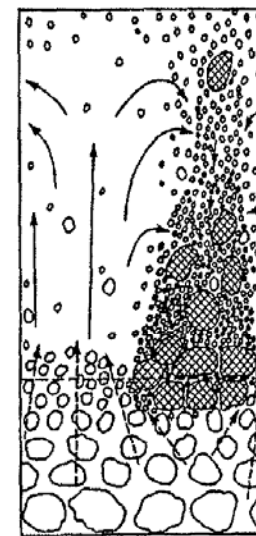
- Insufficient Wash Velocities to remove heavier mud and silts
- Effectively blocks off filter area and increases local loading rates



(a)
Newly constructed bed



(b)
After several washes



(c)
Mudballs forming
clogged area



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Visual Inspection – Other Issues

- “Cracking” at media surface
- Sand separation at filter walls
- Visible algae growth
- Filter media in troughs
- Has scaling or fouling changed the backwash characteristics of the media ?
- Depth of Media – Is it uniform ?
- Are the washwater troughs level ?
- Freeboard – Top of media to underside of trough
- Does surface wash effectively reach the corners ?



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Detailed Filter Evaluation

- A number of techniques can be used to diagnose filter performance issues
 - Filtration Rate Checking
 - Backwash Rise Rate Checking
 - Floc Retention Profiling
 - Backwash Waste Characterization
 - Gravel profiling
 - Sieve testing of media size
 - Media bed depth checking
 - Bed Fluidization Checking
- Tests are relatively easy, and can use home-made testing equipment



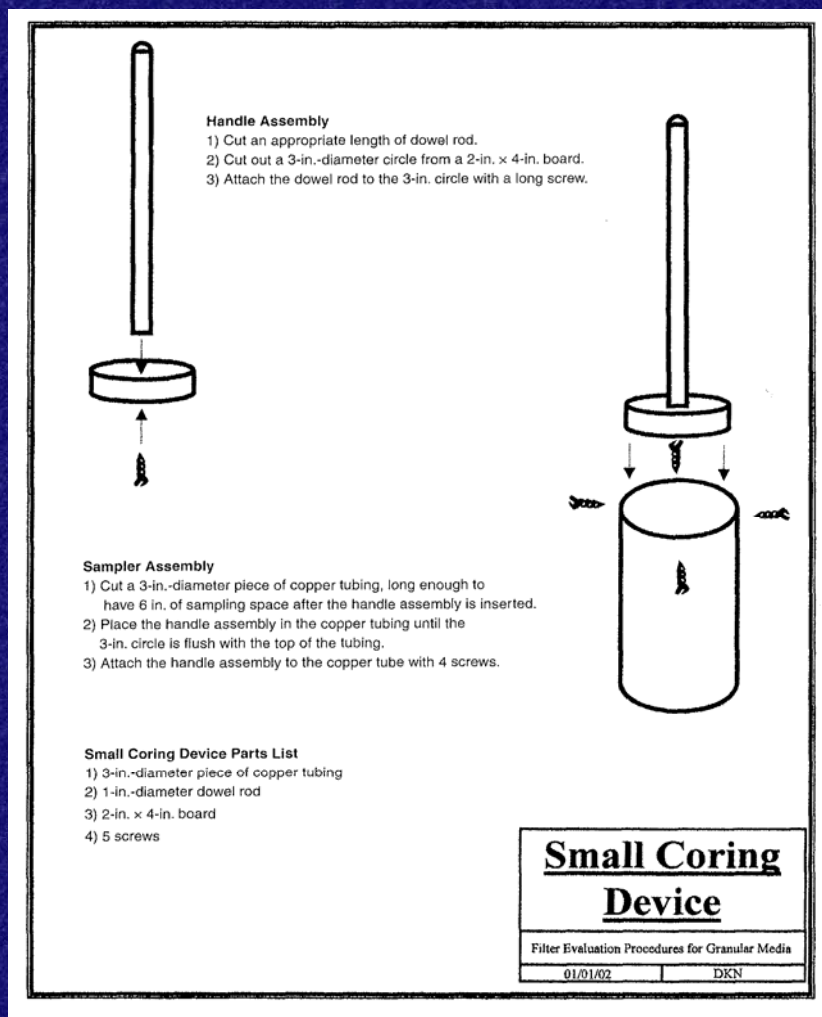
AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



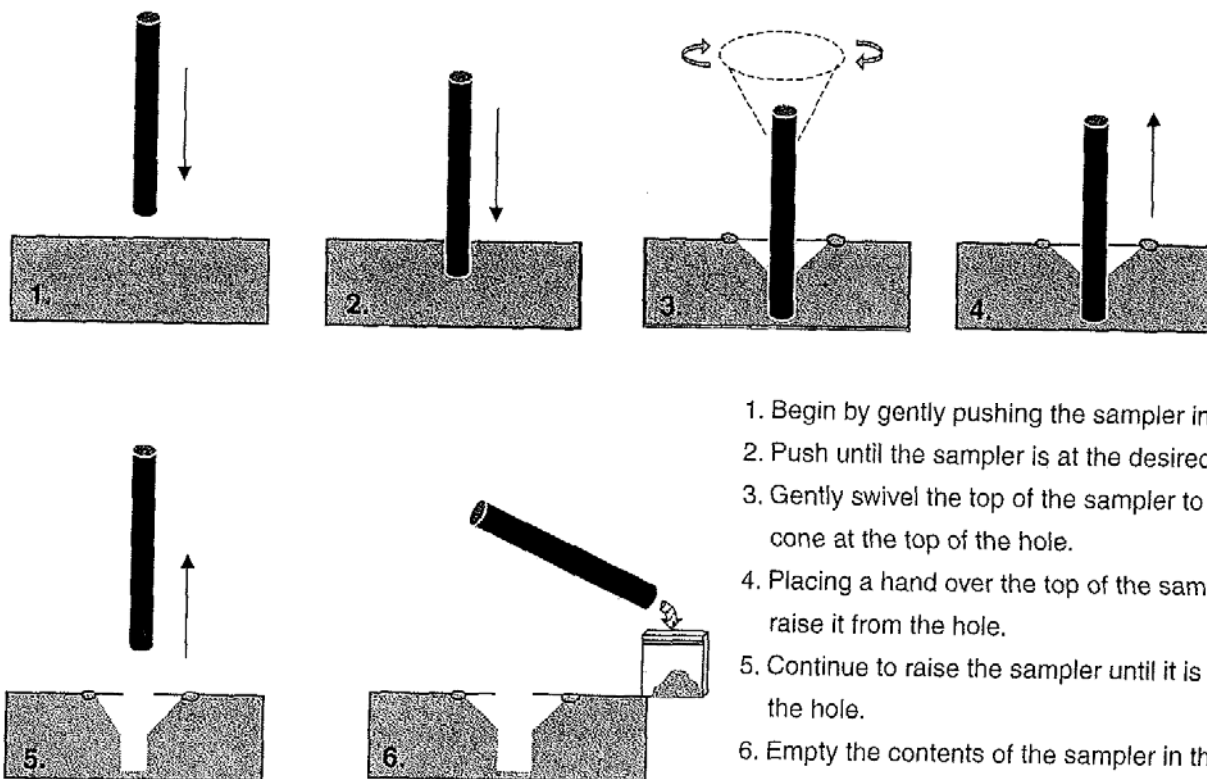
Filter Core Sampling Coring Device

- Source:** Filter Maintenance & Operations Guidance Manual, AWWARF, 2002





Filter Core Sampling Procedure





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Backwash Waste Characterization

- There is such a thing as over-washing a filter !!!
- Backwash waste characterization can help assess the “right” duration
- Perform timed sampling of backwash waste to determine solids content
- Use data to assess when to terminate washing
- May allow reduction in water wastage, and residuals volumes

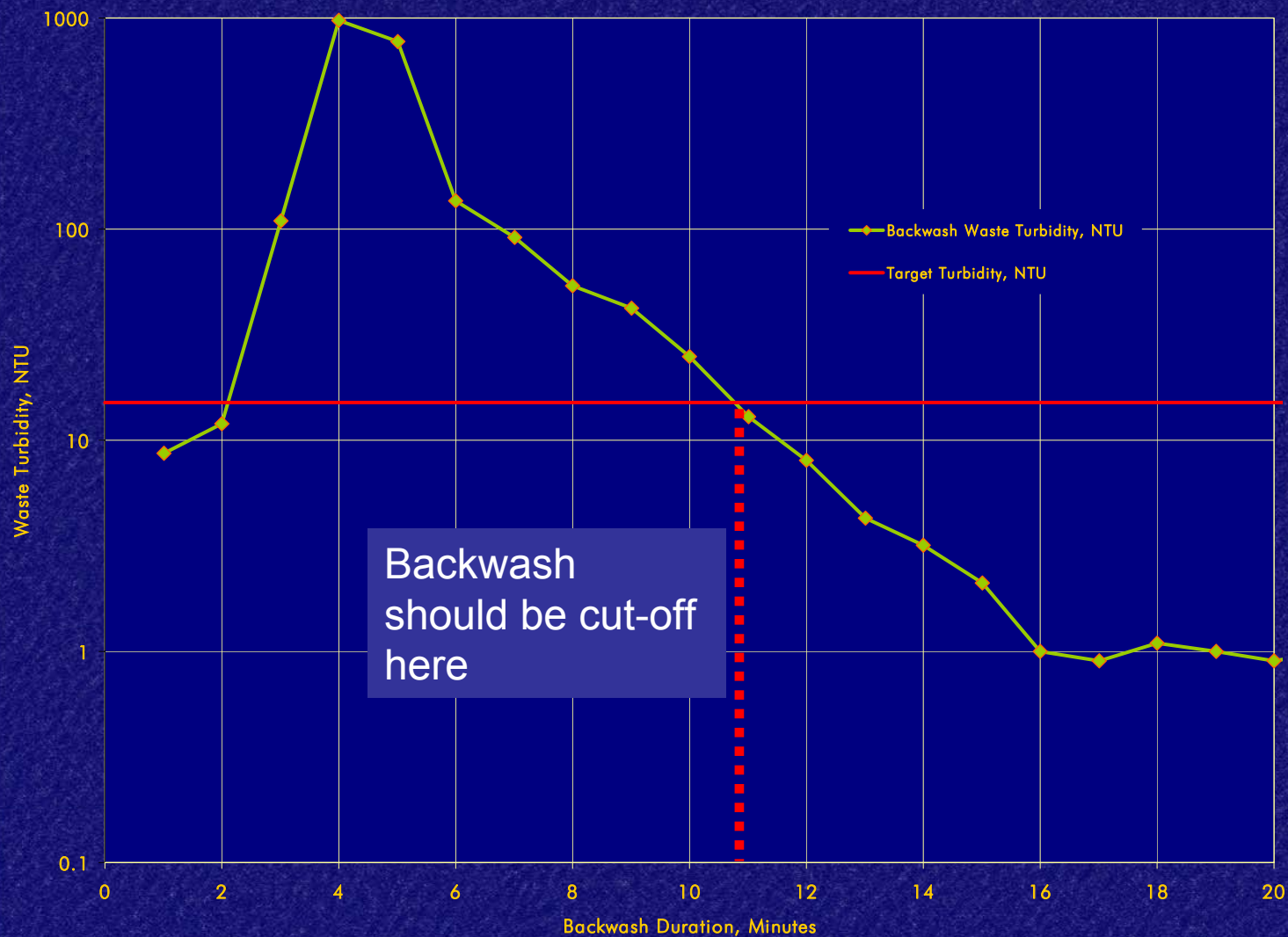


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Typical Waste Evaluation





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Floc Retention Profiling

- Take a core sample
- Sub-divide the core into depth fractions
- Rinse each fraction using a known volume of water, to clean solids off the media
- Measure turbidity in each fraction, before and after washing of filter
- Measures how well solids are being removed from the bed



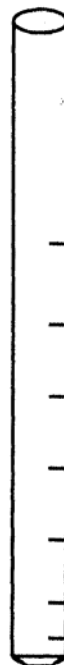
AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Floc Retention Profile Sampler

- **Source:** Filter Maintenance & Operations Guidance Manual, AWWARF, 2002



Sludge Retention Core Sampler Parts List

- 1) 1.5-in. PVC pipe

Sludge Retention Core Sampler Assembly

- 1) Cut an appropriate length of 1.5-in. PVC pipe.
- 2) Using a grinder, slightly bevel the sampling end of the pipe.
- 3) Mark the outside of the PVC pipe at 2-, 6-, 12-, 18-, 24-, 30-, and 36-in. increments with a permanent marker.

Sludge Retention Core Sampler

Filter Evaluation Procedures for Granular Media

01/01/02

DKN



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Floc Retention Profile Graph





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



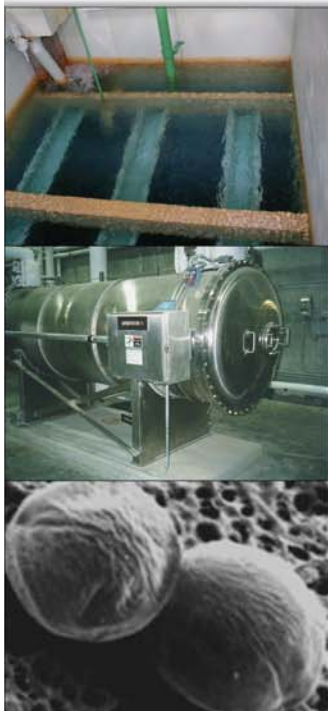
Floc Retention Profile Results

Turbidity, NTU	Filter Media Condition
0 - 30 NTU	Clean - Unripened filter – Long ripening time
30 - 60 NTU	Clean - Ripened Filter
60 - 120 NTU	Slightly dirty, Still OK
120 - 300 NTU	Dirty - Re-Evaluate Backwashing
> 300 NTU	Mudball Problems

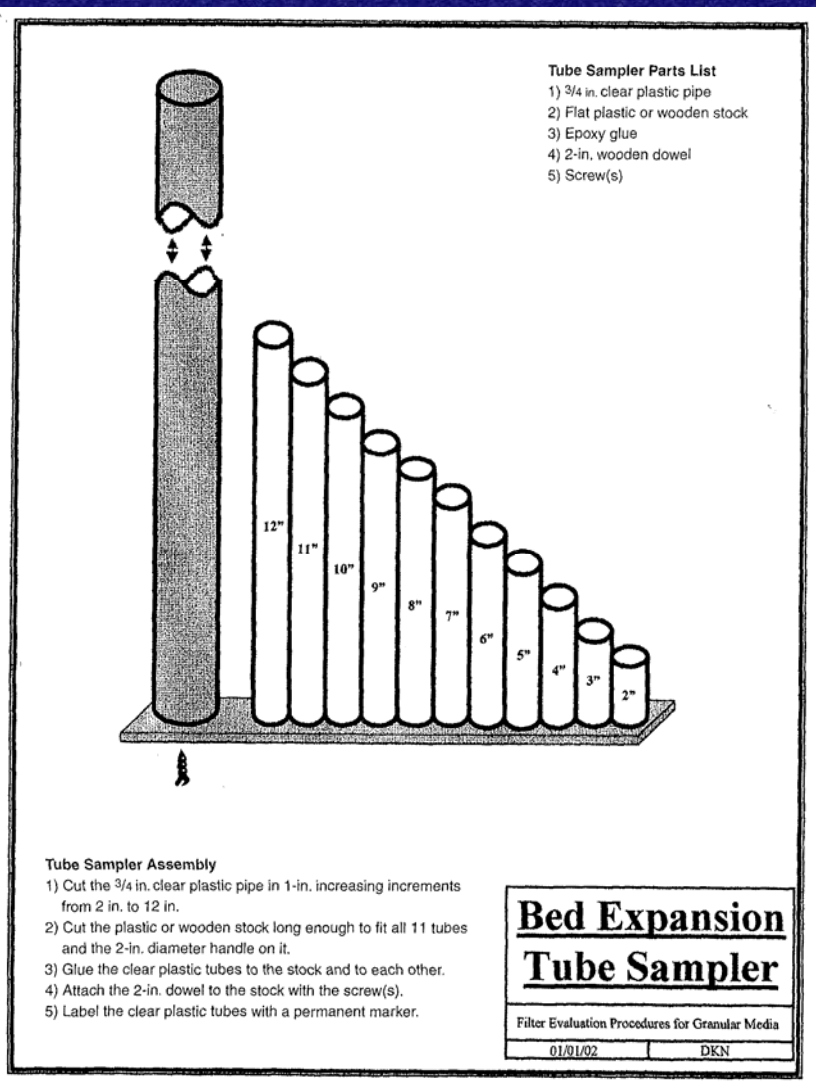


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



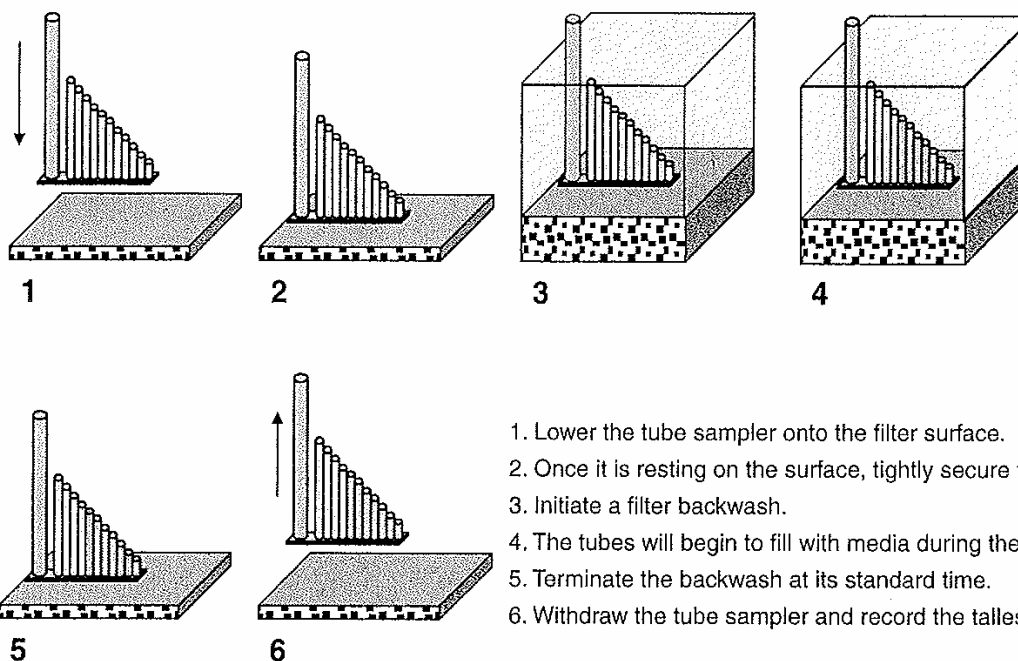
Filter Bed Fluidization Testing Equipment



- **Source:** Filter Maintenance & Operations Guidance Manual, AWWARF, 2002



Bed Fluidization Protocol





AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Compare backwash rate and fluidization

Backwash Flow Rate	Bed Expansion	Notes
Below required	< 20%	Increase backwash rate and repeat test
Below required	20 - 30%	Increase backwash rate and repeat test
Below required	> 30%	Check water temperature
Correct Flow	< 20%	Check for Polymer Buildup on Filter
Correct Flow	20 - 30%	No Action Required
Correct Flow	> 30%	Check Media Specs.
Above Required	< 20%	Check for Polymer Buildup on Filter
Above Required	20 - 30%	Check for Polymer Buildup on Filter
Above Required	> 30%	Reduce Backwash Rate and Repeat Test



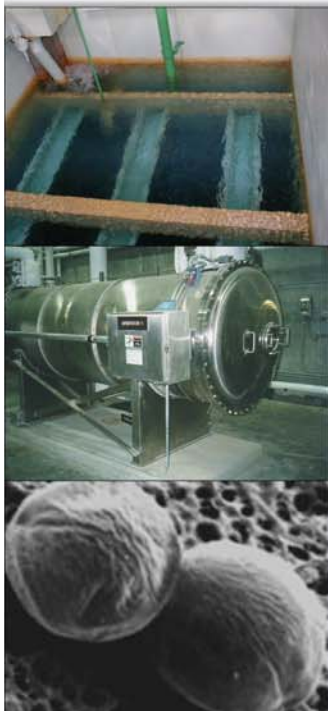
AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

Mudball Analysis

- Used to physically determine the extent of filter mudballing due to chronic underwashing
- Collect 6" Core Samples
- **Gently** sieve the samples to separate mudballs from media
- Place mudballs into a 250 mL graduated cylinder

Percent Mudballs	Filter Condition
0 - 0.1%	Excellent
0.1 - 0.2%	Very good
0.2 - 0.5%	Good
0.5 - 1.0%	Fair
1.0 - 2.5%	Fairly Bad
2.5 - 5%	Bad
Over 5%	Very Bad



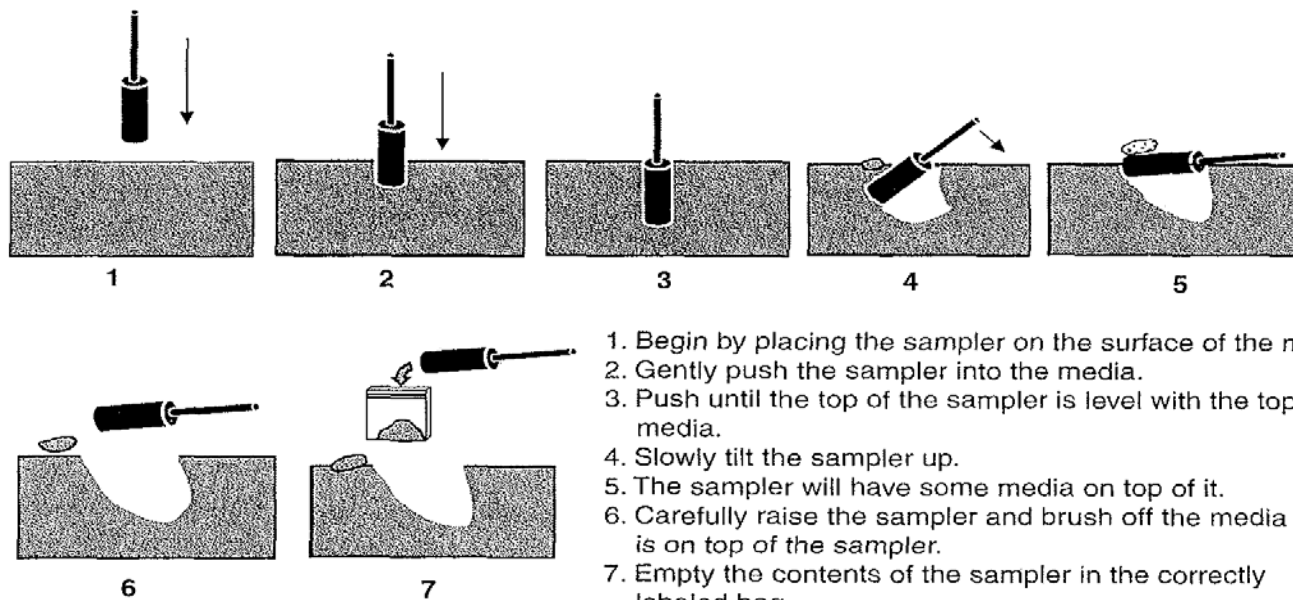


AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

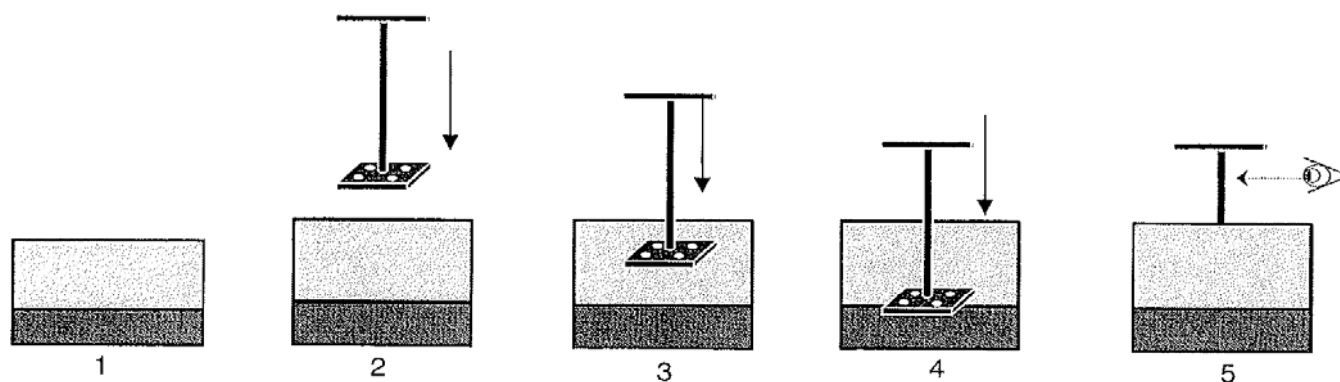


Mudball Sampling Protocol



Gravel Profiling

- Manual measurement of gravel depth at various locations in the filter
- Variation should be no more than ± 25 mm



1. Determine the sampling area.
2. Begin the backwash and start to lower the punch plate into the fluidized media.
3. Continue to press the punch plate down through the media, until ...
4. ... it comes to rest on the gravel layer.
5. Take a reading off of the punch plate and move to the next location.



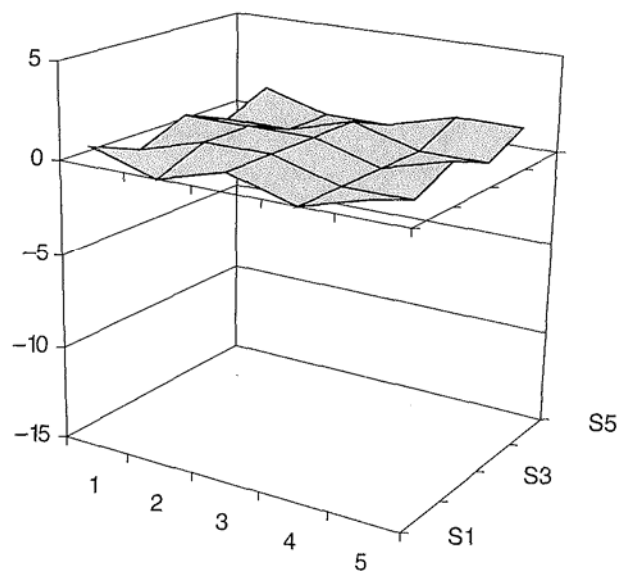
AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



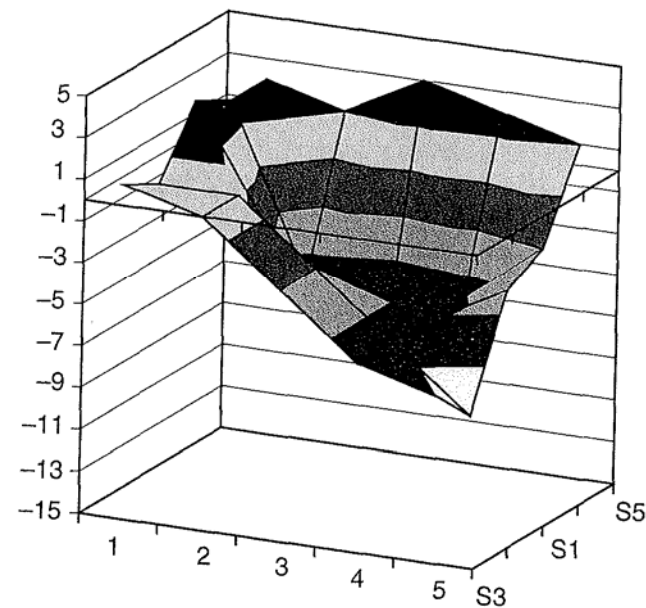
Gravel Profile Examples

Top of Gravel Footprint Filter No. 14



Good

Top of Gravel Footprint Filter No. 1



Severe



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Possible Solutions for Poor Filter Performance

- Optimization of Filter Backwashing
 - Even distribution of flow
 - Selection of Appropriate Wash Rates
 - Levelling of Wash Trough Crests
 - Air Scour
 - Surface Wash
- Addition to Filter-to-Waste
- Use of filter aid polymers
- Addition of coagulant or other chemicals to backwash water



AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



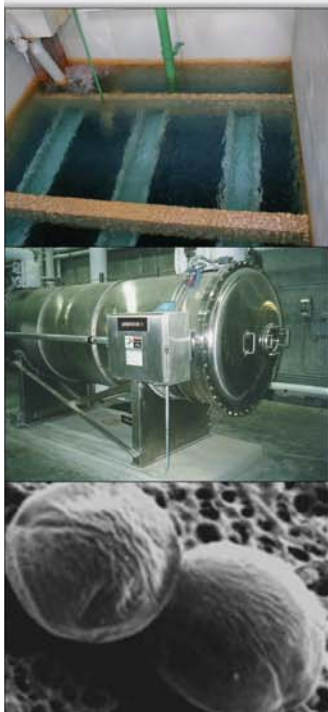
Dealing with badly fouled media

- Filters which exhibit significant fouling problems, mudballing, cracking, etc. are very difficult to rectify
- Lancing is a possible solution, but be very careful if support gravel is in place
- Replacement of the media may be the only solution



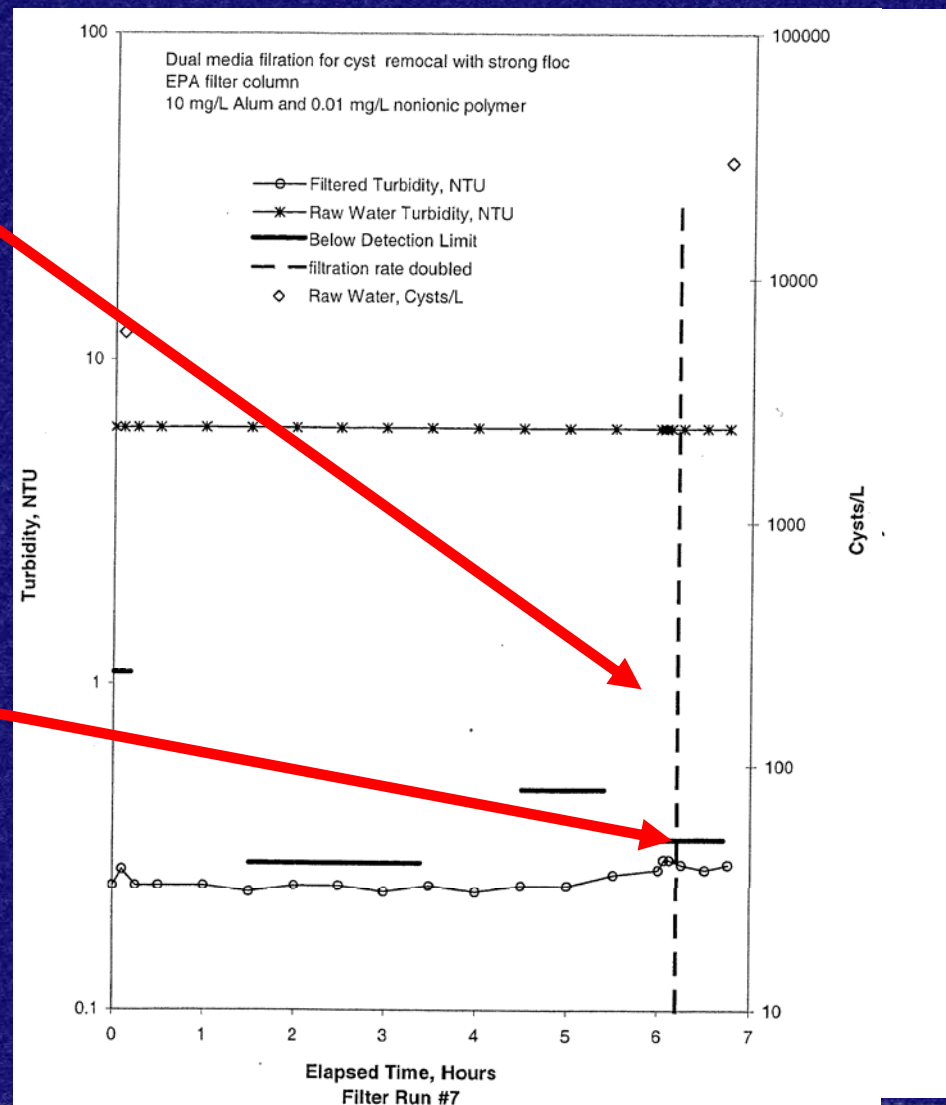
AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006



Filter Aid Polymer can reduce turbidity spiking

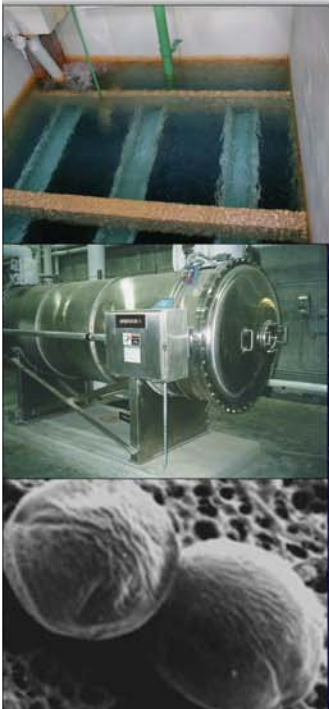
- Note turbidity spike due to flow change
- Use of filter aid strengthens floc, and eliminates spiking





AWWQA Annual
Seminar

Banff, Alberta
March 15, 2006



Excellent Resources

- AWWA Std. M37 – “Operational Control of Coagulation and Filtration Processes”, 2000
- AWWARF, “Filter Maintenance and Operations Guidance Manual”, 2002
- AWWARF, “Self Assessment Guide for Surface WTP Optimization”, 1997
- AWWA, “Filter Evaluation Procedures for Granular Media”, 2002
- AWWARF, “Design & Operation Guidelines for Optimization of the High-Rate Filtration Process – Plant Survey Results”, 1989
- AWWA, “Filter Troubleshooting & Design Handbook”, 2005



AWWOA Annual
Seminar

Banff, Alberta
March 15, 2006

Questions ??

Contact: Simon Breese, M.A.Sc., P.Eng.
Technical Practice Leader, Drinking Water, Earth Tech
simon.breese@earthtech.ca
(519) 570-2102

