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(54) **INTEGRATED DESALINATION AND AIR
CONDITIONING SYSTEM**

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(57) **ABSTRACT**

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2103/08; C02F 1/14; B01D 5/006
See application file for complete search history.

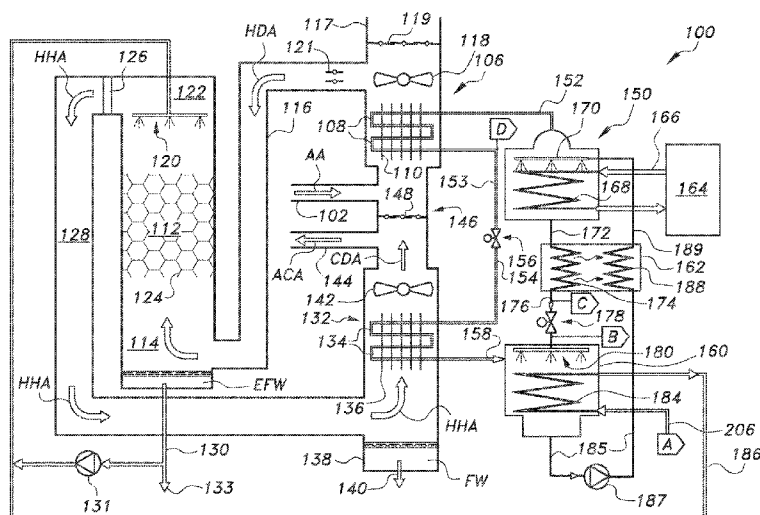
The integrated desalination and air conditioning system can provide desalinated (fresh) water, cold air or both in a single efficient system. The system incorporates a humidification-dehumidification (HdH) desalination system with a water-lithium bromide (H₂O—LiBr) vapor absorption cycle (AbC) system. The AbC system includes an AbC generator that provides a heating source for an AbC condenser that heats the air input of the HdH; two AbC absorbers that provide heating sources for the feed seawater; a first AbC evaporator that provides a cooling source for the humidified air produced in the HdH; and a second AbC evaporator that provides a cooling source for use outside the system. The heat input for the AbC generator can be provided by low-grade heat sources, such as waste heat or solar thermal energy. The system is capable of producing fresh water and/or cold air at different capacities, depending on water demands and cooling load requirements.

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18 Claims, 6 Drawing Sheets



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F25B 15/06 (2006.01)
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C02F 1/14 (2006.01)
C02F 103/08 (2006.01)
C02F 1/16 (2006.01)

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- (52) **U.S. Cl.**
 CPC **F25B 27/007** (2013.01); **F25B 27/02** (2013.01); **F25B 39/00** (2013.01); **C02F 1/14** (2013.01); **C02F 1/16** (2013.01); **C02F 2103/08** (2013.01); **F24F 2005/0064** (2013.01)

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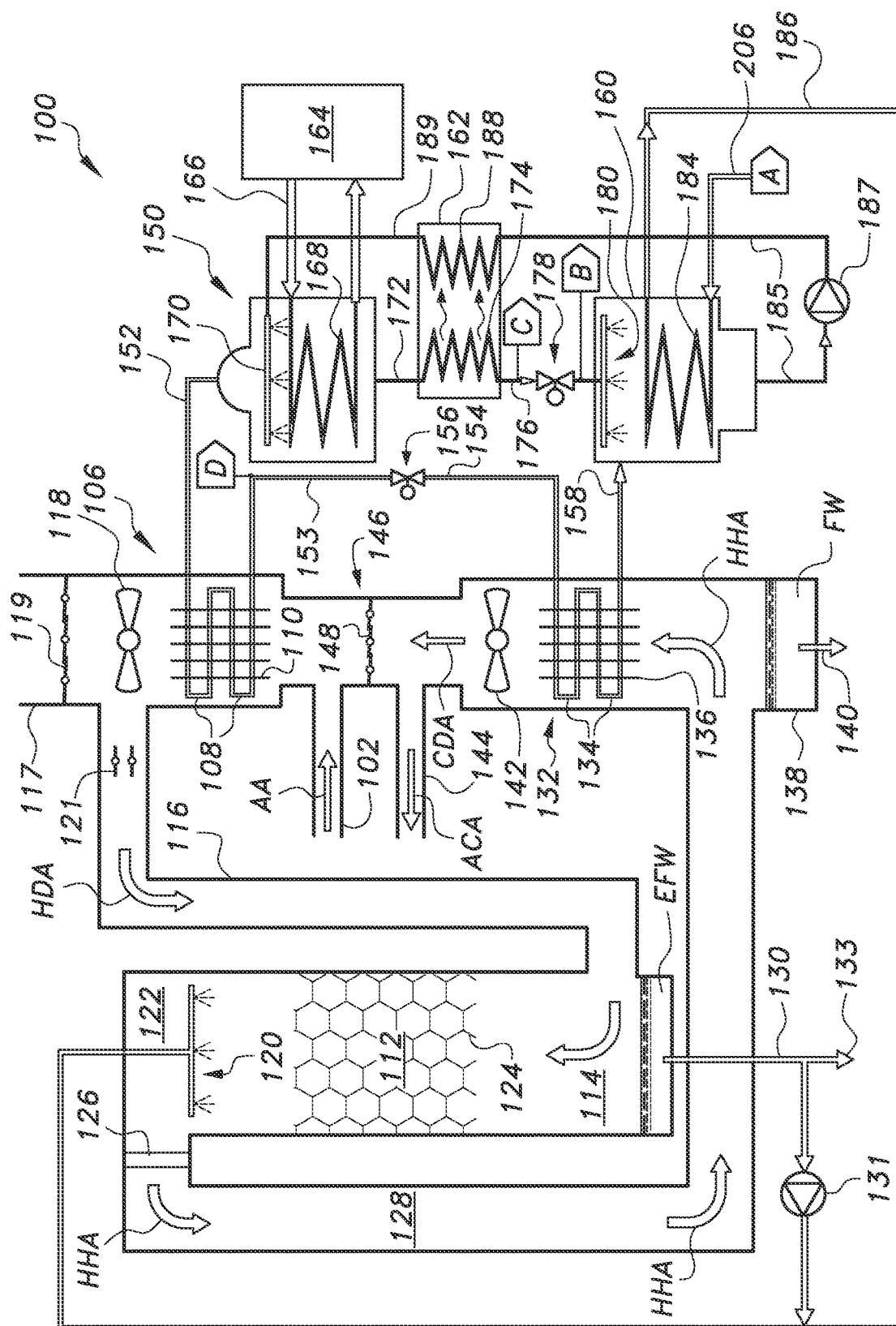


FIG. 1

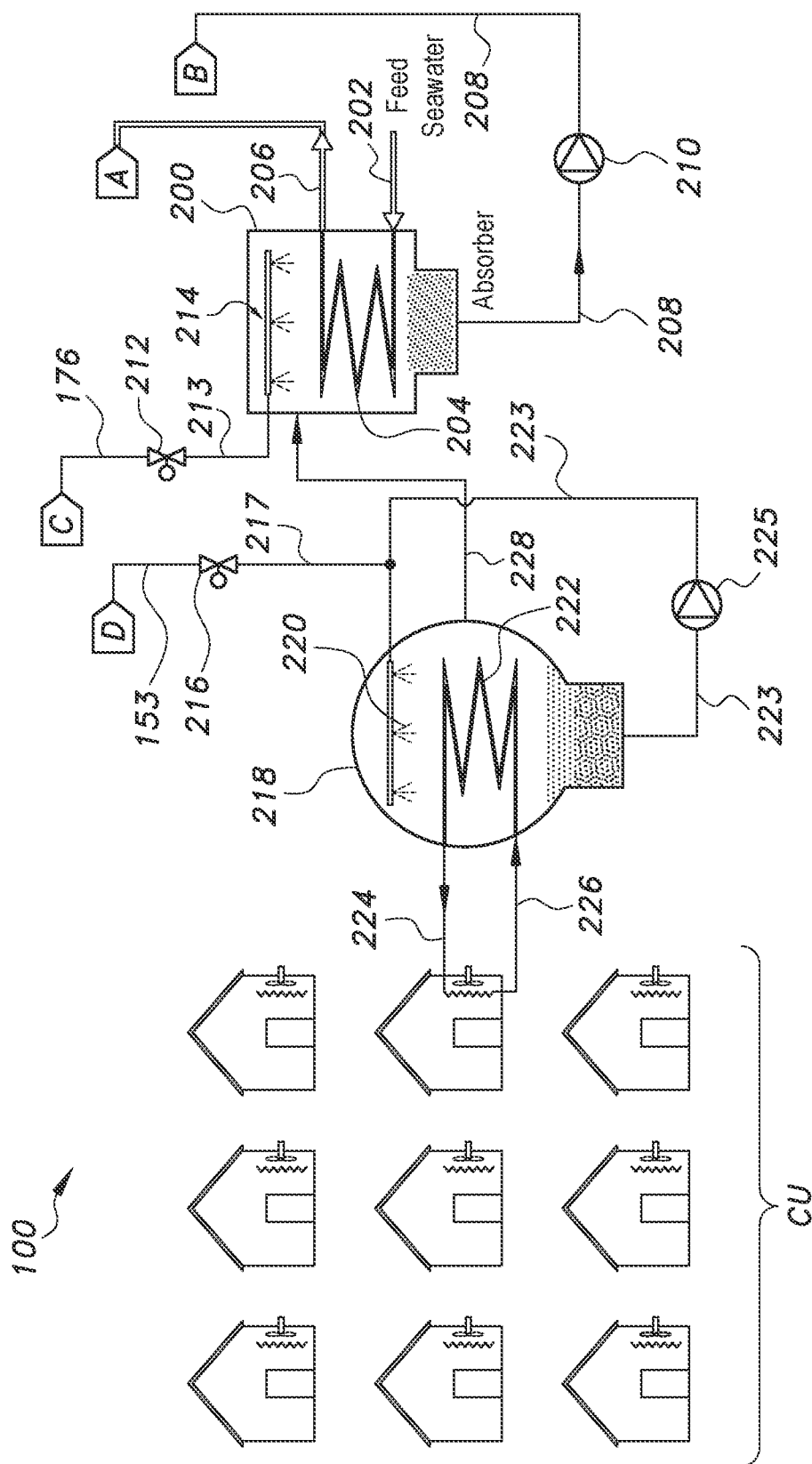


FIG. 2

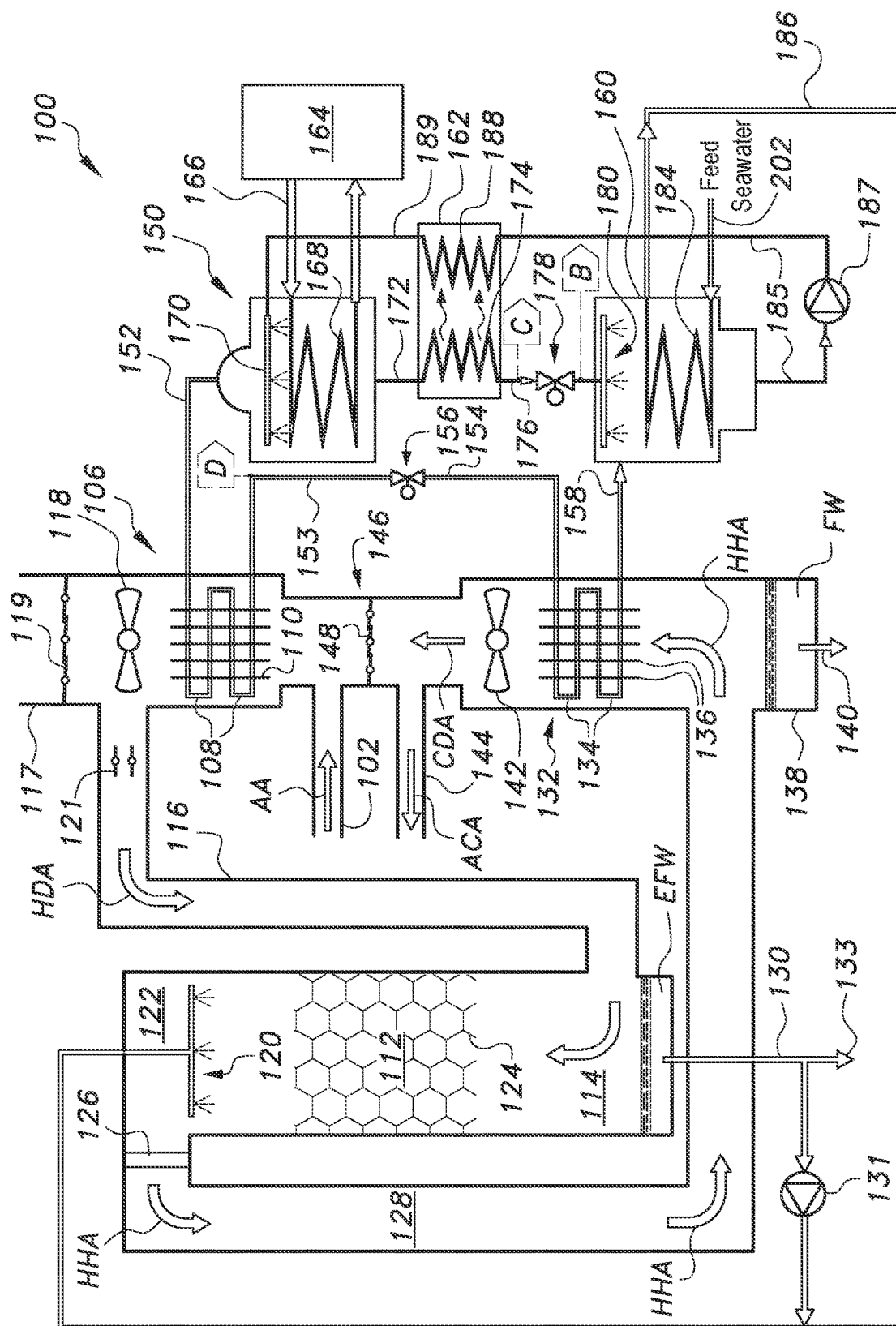


FIG. 3

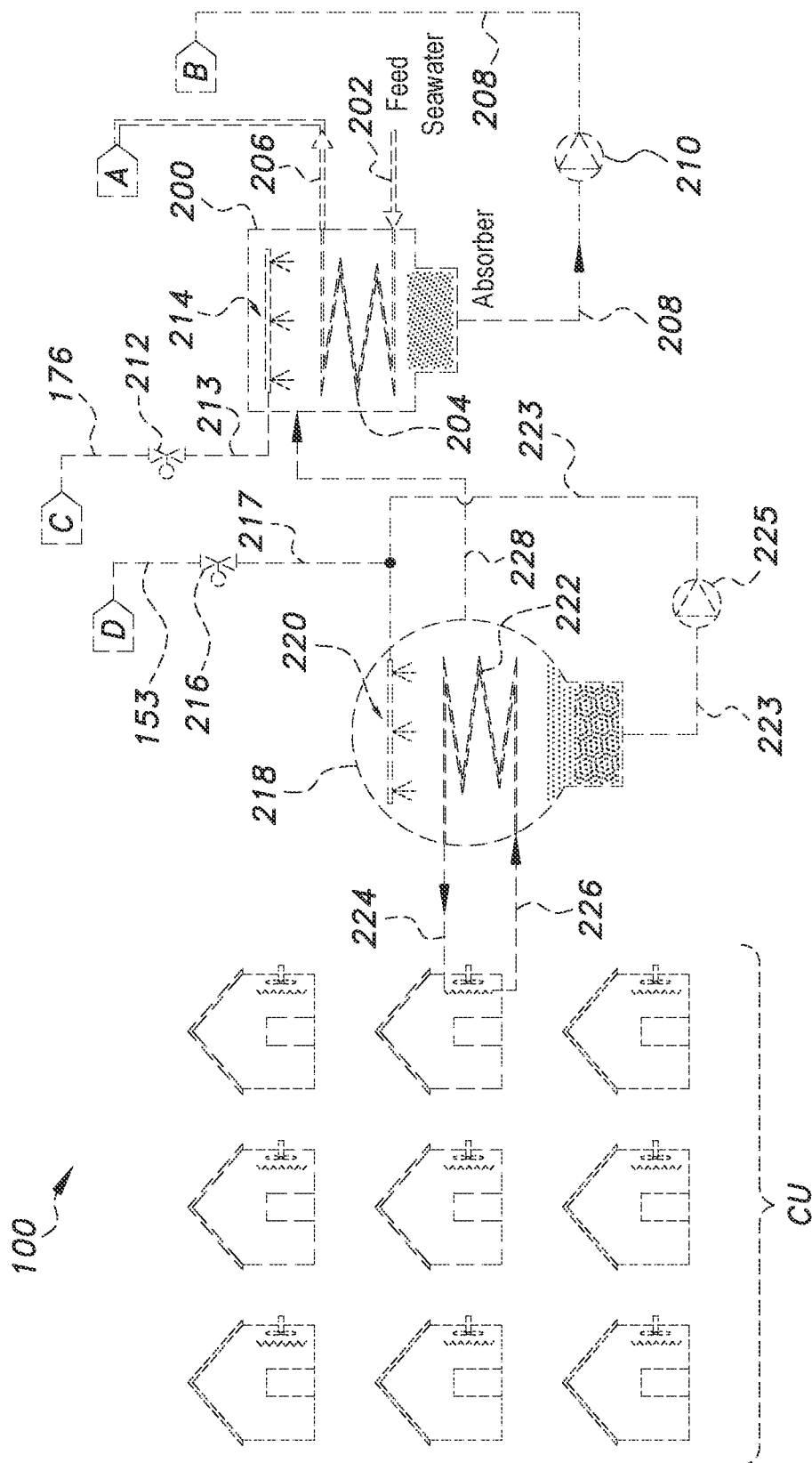


FIG. 4

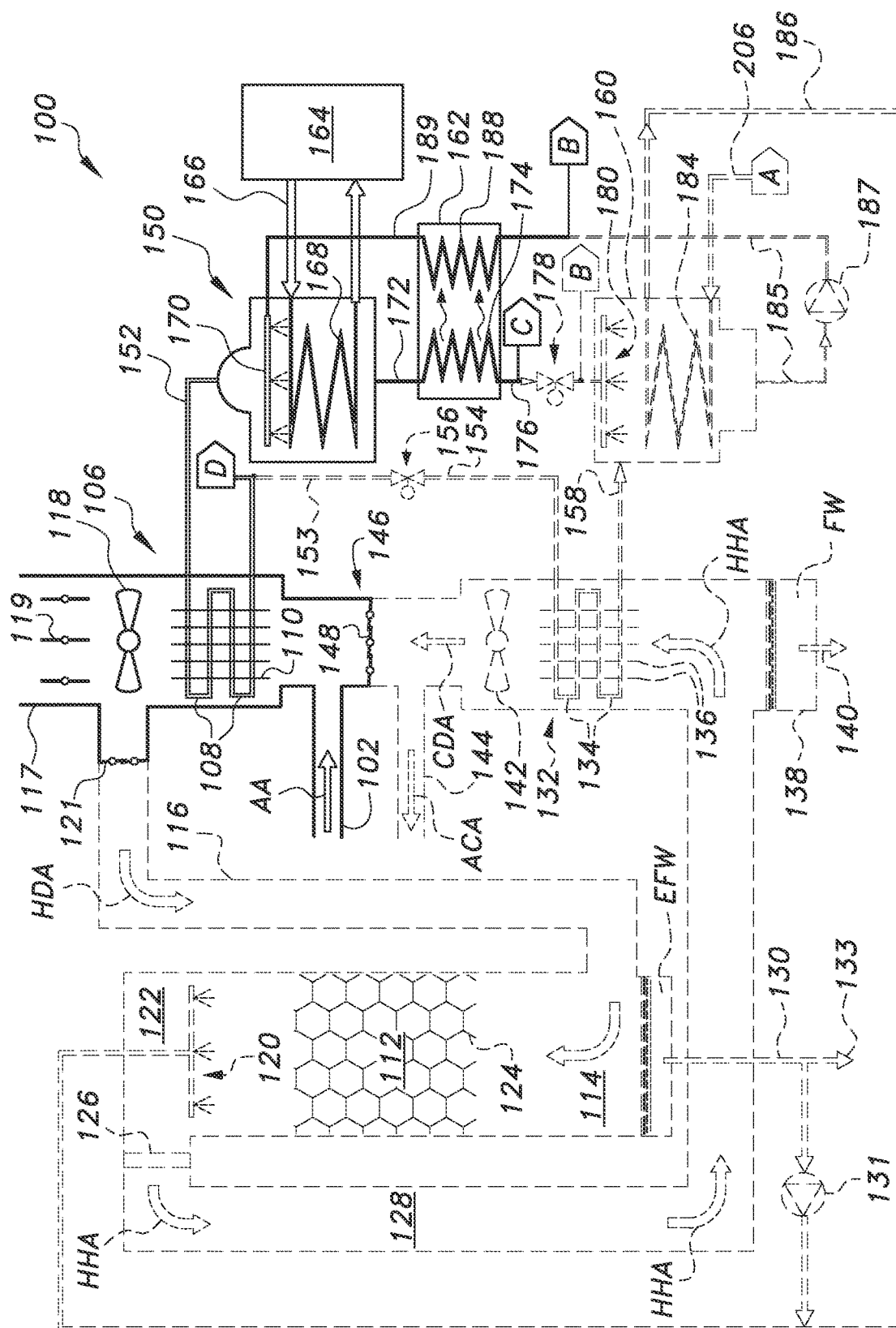


FIG. 5

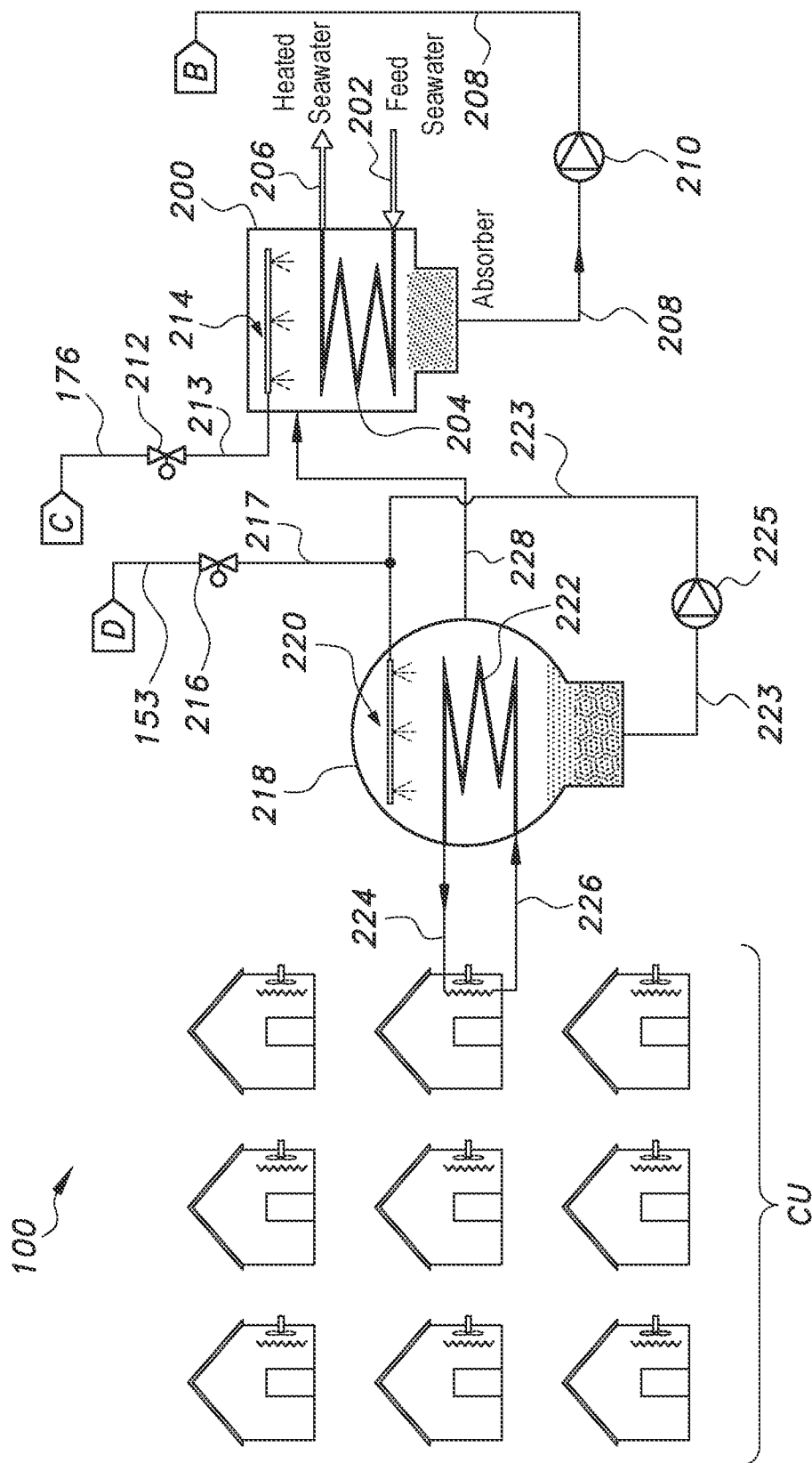


FIG. 6

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INTEGRATED DESALINATION AND AIR CONDITIONING SYSTEM

BACKGROUND

1. Field

The disclosure of the present patent application relates generally to desalination systems and air conditioning systems, and particularly to an integrated desalination and air conditioning system.

2. Description of the Related Art

Water scarcity, as well as uncomfortable and even deadly heat, are particular issues in hot climates, such as in arid and semi-arid regions. Existing desalination systems and air conditioning systems both require large energy sources to perform their intended functions and a larger footprint area to house their separate systems. In addition, if the energy sources for these systems are provided by fossil fuels, there are environmental, health and safety impacts that must be considered. Conventional thermal desalination technologies operating at high temperatures, require expensive materials of construction, and also face scaling, fouling, and corrosion challenges. Conventional, standalone humidification-dehumidification (HdH) desalination systems have a limited water recovery ratio due to energy requirements to heat the feed water and heat and cool the air. Conventional air conditioning systems normally reject thermal heat energy to the environment from the condenser, while conventional HdH systems require thermal energy for heating the air and feed water.

Thus, an integrated desalination and air conditioning system solving the aforementioned problems is desired.

SUMMARY

The integrated desalination and air conditioning system can provide desalinated (fresh) water only, or cooling effect only for air conditioning in the form of cold air and chilled water, or both fresh water and air conditioning in a single efficient system. The system incorporates a humidification-dehumidification (HdH) desalination system with a water-lithium bromide (LiBr) vapor absorption cycle (AbC) system. Combining and integrating both systems allows the HdH system to utilize the rejected thermal energy from the AbC system, which reduces the energy consumption of the integrated system. The AbC system includes: an AbC generator to separate water vapor from an LiBr solution and provides a heating source for an AbC condenser that heats the atmospheric air input of the HdH; two AbC absorbers that absorb the refrigerant vapor from the evaporators and provide heating sources for the feed seawater; a first AbC evaporator that provides a cooling source for the humidified air produced in the HdH and produces fresh water; and a second AbC evaporator that provides a cooling source for chilled water to be used outside the system. The heat input for the AbC generator can be a direct heat source or a motive steam input and can be provided by low-grade heat sources, such as waste heat or solar thermal energy. The integrated desalination and air conditioning system is capable of producing fresh water and providing a cooling effect (desalination/air conditioning mode) at varying capacities, depending on the drinking water demands and corresponding cooling load requirements. By combining desalination and air conditioning in a single system, capital and operating

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expenses are reduced when compared to standalone HdH desalination and air conditioning systems. In addition, the compact design of the system can be easily containerized and used as a portable desalination and air conditioning system.

These and other features of the present subject matter will become readily apparent upon further review of the following specification and drawings.

BRIEF DESCRIPTION OF THE DRAWING

FIGS. 1 and 2 are a schematic diagram of an integrated desalination and air conditioning system, shown operating in a combined desalination and cooling mode or configuration.

FIGS. 3 and 4 are a schematic diagram of the integrated desalination and air conditioning system of FIGS. 1 and 2, showing the system operating in a desalination only mode or configuration.

FIGS. 5 and 6 are a schematic diagram of the integrated desalination and air conditioning system of FIGS. 1 and 2, showing the system in a cooling only mode or configuration.

Similar reference characters denote corresponding features consistently throughout the attached drawings.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

The integrated desalination and air conditioning system **100** is shown in FIGS. 1 and 2 in a combined desalination and cooling mode or configuration. The air handling portion (the humidification-dehumidification (HdH) desalination system) of the integrated system **100** will be described first with respect to FIG. 1, followed by a description of the liquid handling portion (the water-lithium bromide (LiBr) vapor absorption cycle (AbC) system) of the integrated system **100**. Atmospheric air AA or other outside air source is introduced to the system **100** via a first duct **102** using a first blower **118** such that AA flows over the AbC condenser **106**. The air is heated sensibly by coils **108** of the AbC condenser **106**, which include fins **110** to increase heat transfer to the air. The air exits the AbC condenser **106** as hot dry air HDA. The temperature of the air exiting the AbC condenser **106** is dependent on the amount of desalination and cooling required.

The hot and dry air HDA with an atmospheric amount of water vapor (as humidity) is directed by a first fan **118** to the bottom **114** of a humidification column **112** via a second duct **116** in the combined desalination and cooling mode, as the first damper **119** is closed and the second damper **121** is open. Seawater spray nozzles **120** at the top **122** of the humidification column **112** spray heated feed seawater downward into the humidification column **112**, thereby increasing the air humidity and producing hot and humid air HHA. The interior of the humidification column **112** may include packing material **124** to increase the residence time of the water in contact with the air, so the hot, dry air HDA will be humidified with the maximum possible amount of water vapor. A demister **126** at the top **122** of the humidification column **112** prevents the passage of any water droplets into the duct **128**. The excess feed water EFW is collected at the bottom of the humidification column **112** and exits via a brine pipe **130** and is either recycled in the system **100** or is rejected as brine, as described further below.

The hot and humid air HHA is routed to an AbC evaporator **132** by the duct **128** and is cooled by coils **134** of the AbC evaporator **132**, which include fins **136** to increase heat transfer from the air. The water vapor condensed by the AbC

evaporator **132** produces fresh water FW, which is collected in a product water tank **138** underneath the AbC evaporator **132**. A fresh water pipe **140** can supply the fresh water FW from the water tank **138** to municipal water or other fresh water systems.

The resulting cold and dry air CDA from the AbC evaporator **132** is directed by a second fan **142** for use as air conditioning or cooling air in one of two ways. All or a portion of the cold and dry air CDA can be directed as air conditioning air ACA to the desired air conditioned space via a duct **144**. Alternatively, the cold and dry air CDA can be used in an air-to-air heat exchanger (not shown) for sensibly cooling the atmospheric air AA to the desired temperature prior to entering the air-conditioned space. A third damper **146** between the AbC evaporator **132** and the AbC condenser **106** includes a plurality of vanes **148**. Normally, in the combined desalination and cooling mode, the third damper **146** is closed. However, during extremely hot weather the third damper **146** can be opened and closed to control the amount of cold and dry air CDA mixed with the atmospheric air AA, for cooling the atmospheric air AA prior to entering the AbC condenser **106** to improve the heat transfer of the AbC condenser **106**.

The liquid handling portion (the water-lithium bromide (LiBr) vapor absorption cycle (AbC) system) of the integrated system **100** will now be described with respect to FIGS. **1** and **2**. An AbC generator **150** separates the water from the diluted LiBr solution and provides superheated steam to the coils **108** of the AbC condenser **106** via a water vapor pipe **152** for heating the atmospheric air AA (and possibly some of the cold dry air CDA during extremely hot weather), as described above. The cool air condenses the superheated steam to a saturated liquid that is divided into two streams. One stream is supplied to the first refrigerant expansion valve (REV) **156** via saturated liquid pipe **153**. The REV **156** throttles the liquid to a low pressure and temperature liquid-vapor mixture that flows to the coils **134** of the AbC evaporator **132** via a first saturated liquid-vapor mixture pipe **154**. The other stream of the saturated liquid is supplied to a second evaporator **218**, shown in FIG. **2**, via the saturated liquid pipe **153**, a second REV **216** and a second saturated liquid-vapor mixture pipe **217**. The condensed refrigerant is throttled in the refrigerant expansion valves **156**, **216** to a very low pressure (<1 kPa) corresponding to each evaporator according to the required temperature in the evaporator, producing a cold water-vapor mixture at a temperature less than 3° C. The refrigerant (cold liquid-vapor mixture) from the first refrigerant expansion valve **156** flows through the coils **134** of the AbC evaporator **132**, thereby cooling the hot and humid air HHA to condense the water vapor from the air producing fresh water, and the cold and dry air CDA, as described above. The refrigerant leaves the coils **134** of the AbC evaporator **132** as a saturated vapor and is supplied to a first AbC absorber **160** via a first vapor pipe **158**.

As shown in FIG. **2**, the refrigerant from the second refrigerant expansion valve **216** is supplied to a sprayer **220** (via the second saturated liquid-vapor mixture pipe **217**) in the second evaporator **218** and is sprayed on coils **222** of the second evaporator **218**, thereby cooling the water flowing in the coils **222** to produce chilled water for the air conditioning application outside system **100**. The chilled water is supplied to one or more consumer cooling units (CUs) via a chilled water supply pipe **224**, and after use, the chilled water (now heated) from the one or more CUs is returned to the coils **222** via a refrigerant return pipe **226** and a system of pumps and valves (not shown). The chilled water is used

in the one or more CUs to produce cold air for air conditioning the CUs. The CUs include pumps, fans and controlling valves for producing air conditioning using the chilled water. A recirculation pump **225** may be used in the evaporator **218** to recirculate the refrigerant flow to the sprayer **220** via pipe **223**, to be sprayed on the coils **222**. The refrigerant leaves the second evaporator **218** as a saturated vapor and is supplied to a second AbC absorber **200** via a second vapor pipe **228**.

The absorption cycle of the integrated desalination and air conditioning system **100** is a modified single-effect-type, using the AbC generator **150**, the AbC condenser **106**, the AbC evaporators **132**, **218**, the AbC absorbers **160**, **200**, and a solution heat exchanger **162**. Motive steam or heat is provided to the AbC generator **150** from a heat source **164** via pipe **166**. The heat source **164** may be a low-grade heat source, such as industrial waste heat or solar heat sources. The motive steam is fed through a coil **168** in the AbC generator **150** to heat a diluted LiBr solution provided by a LiBr solution sprayer **170**. The heat from the motive steam separates the refrigerant (water vapor) from the diluted LiBr solution. The produced superheated steam is directed to the coils **108** of the AbC condenser **106**, as described above. The remaining concentrated LiBr solution flows to heat-producing coils **174** of the heat exchanger **162** via a concentrated LiBr solution pipe **172**. The cooled concentrated LiBr solution is divided into two streams. One stream is fed to the first AbC absorber **160** via a cooled concentrated LiBr solution pipe **176** and a first solution expansion valve (SEV) **178**. The cooled concentrated LiBr solution is sprayed into the top of the first AbC absorber **160** via solution spray nozzles **180**. In the first AbC absorber **160**, the water vapor supplied to the first AbC absorber **160** from the coils **134** of the AbC evaporator **132** is absorbed by the sprayed concentrated LiBr solution. The concentrated LiBr solution then becomes a diluted LiBr solution.

As the absorption process in the AbC absorber **160** is an exothermic process, cooling is required. A source of cold seawater from the sea is supplied to heated seawater coils **204** of the second AbC absorber **200** by a cold seawater pipe **202**. It should be noted that while the cooling water is noted as being seawater, other sources of salt water, fresh water and even industrial wastewater may be used as the cooling water supplied to pipe **202**. The seawater from the heated seawater coils **204** of the second AbC absorber **200** is supplied to the seawater coils **184** of the first AbC absorber **160** by a second heated seawater pipe **206**, and is further heated by the exothermic process. The cooled diluted LiBr solution from the bottom of the first AbC absorber **160** is supplied to heat absorbing coils **188** of the heat exchanger **162** via a first diluted LiBr solution pipe **185** and a first diluted LiBr solution pump **187**. The solution pump **187** provides a pressure suitable for the AbC generator **150**.

The cooled, concentrated LiBr solution is also fed to the second AbC absorber **200** via the cooled concentrated LiBr solution pipe **176**, a second SEV (solution expansion valve) **212** and pipe **213**. The cooled concentrated LiBr solution is sprayed into the top of the second AbC absorber **200** via solution spray nozzles **214**. In the second AbC absorber **200**, the water vapor supplied to the second AbC absorber **200** from the second evaporator **218** is absorbed by the sprayed concentrated LiBr solution. As in the first AbC absorber **160**, the absorption process in the second AbC absorber **200** is an exothermic process, and the seawater in the seawater coils is heated before being directed to the seawater coils **184** of the first AbC absorber **160**. The cooled diluted LiBr solution from the bottom of the second AbC absorber **200** is supplied

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to the solution spray nozzles of the first AbC absorber **160** via a second diluted LiBr solution pipe **208** and a second diluted LiBr solution pump **210**. The diluted LiBr solution from the AbC absorber **160** absorbs heat from the concentrated LiBr solution flowing in the heat producing coils **174** of the heat exchanger **162** before being routed to the LiBr sprayer **170** via a heated diluted LiBr solution pipe **189** to be sprayed on the coil **168** of the AbC generator **150** tubes to separate the water vapor from the solution, as described above.

The process heated seawater from the seawater coils **184** is supplied to the seawater spray nozzles **120** at the top **122** of the humidification column **112** via a heated seawater pipe **186**. Additional seawater can be provided to the seawater spray nozzles **120** from the excess feed water EFW collected at the bottom of the humidification column **112** via the brine pipe **130** and a brine pump **131**. Excess brine can be removed from the integrated desalination and air conditioning system **100** from the brine pipe **130** via a brine drain **133** for further processing into a salt product, or for other uses.

As previously noted, the integrated desalination and air conditioning system **100** is capable of producing fresh water, (desalination only mode), cooling effect (chilled water), (air conditioning only mode) or both fresh water and cooling effect (chilled water and CDA) (desalination/air conditioning mode). In the desalination/air conditioning mode, all of the above components are included and activated and operate in the manner described above.

As shown in FIGS. 3-4, in the desalination only mode (or configuration), the first damper **119** is closed, the second damper **121** is open and the third damper **146** operates normally, as described above. The second AbC absorber **200**, the second SEV **212**, the second REV **216**, the second evaporator **218** (and attached CUs), the recirculation pump **225** and the second diluted LiBr solution pump **210** (and associated pipes) can be eliminated for a desalination only configuration and the seawater is fed directly to the seawater coils **184** of the first AbC absorber **160** via pipe **202**. Alternatively, valves (not shown) may be provided and closed just before the second SEV **212**, and the second REV **216** and the second diluted LiBr solution pump **210** can be deactivated for operating in the desalination only mode. The seawater is routed directly to the seawater coils **184** of the first AbC absorber **160**, using valves (not shown) to bypass the seawater coils **204** of the second AbC absorber **200**.

As shown in FIGS. 5-6, in the cooling only mode or configuration, the first damper **119** is open, the second damper **121** is closed, and the third damper **146** is closed. The first AbC absorber **160**, the first SEV **178**, the first REV **156**, the first diluted LiBr solution pump **187**, the humidification column **112**, the demister **126**, the first evaporator **132**, the third fan **142** and the associated ductwork can be eliminated for a cooling only configuration, and the heated seawater from the seawater coils **204** of the second AbC absorber **200** can be vented out of the integrated desalination and air conditioning system **100** for use in other systems or dumped to the drainage sump, as desired. The cooled diluted LiBr solution from the bottom of the second AbC absorber **200** is supplied directly to the heat absorbing coils **188** of the heat exchanger **162** via solution pump **210** and conduit **208**, as shown in FIGS. 5-6. Alternatively, valves (not shown) may be provided and closed just before the first SEV **178**, and the first REV **156** and the first diluted LiBr solution pump **187** can be deactivated for operating in the cooling only mode. The seawater may still be supplied to the seawater coils **204** of the second AbC absorber **200**, and a

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valve (not shown) can direct the seawater from the seawater coils **204** to be vented out of the system **100**.

It is to be understood that the integrated desalination and air conditioning system is not limited to the specific embodiments described above, but encompasses any and all embodiments within the scope of the generic language of the following claims enabled by the embodiments described herein, or otherwise shown in the drawings or described above in terms sufficient to enable one of ordinary skill in the art to make and use the claimed subject matter.

We claim:

1. An integrated desalination and air conditioning system, comprising:

a humidification-dehumidification desalination system, including:

a first air input duct for supplying outside air to the desalination system;

a vapor absorption cycle (AbC) condenser for heating the outside air supplied by the first air duct, the AbC condenser having a plurality of condenser coils;

a humidification column having an interior, a top, a bottom and seawater spray nozzles at the top of the humidification column;

a second air duct providing a conduit directing heated air from the AbC condenser to the bottom of the humidification column;

a first AbC evaporator for cooling heated humid air from the top of the humidification column, the first AbC evaporator having a first plurality of evaporator coils;

a third air duct directing heated humid air from the top of the humidification column to the first AbC evaporator;

a fourth air duct directing cold and dry air from the first AbC evaporator to a predetermined location, the predetermined location defining an air conditioned space;

a product water tank underneath the first AbC evaporator for collecting fresh water condensed by the first plurality of evaporator coils; and

a water-lithium bromide vapor absorption cycle system, including:

an AbC generator having:

a solution sprayer for spraying a diluted LiBr solution; and

means for receiving heat from a heat source to separate water vapor from the diluted LiBr solution, thereby forming a concentrated LiBr solution;

a water vapor pipe extending between the AbC generator and the AbC condenser coils, providing the water vapor to the condenser coils;

a saturated liquid pipe extending between the AbC condenser coils and the first plurality of evaporator coils;

a first refrigerant expansion valve in the saturated liquid pipe for providing very low pressure cold water to the first plurality of evaporator coils;

a first AbC absorber having:

first solution spray nozzles for spraying the concentrated LiBr solution; and

first seawater heating coils;

a first vapor pipe extending between the first plurality of evaporator coils and the first AbC absorber for providing water vapor from the first plurality of evaporator coils to the first AbC absorber;

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- a solution heat exchanger having:
 - heat producing coils; and
 - heat absorbing coils;
 - a concentrated LiBr solution pipe extending between the AbC generator and the heat producing coils, providing the concentrated LiBr solution to the heat producing coils to produce a cooled, concentrated LiBr solution;
 - a cooled, concentrated LiBr solution pipe extending between the heat producing coils and the first solution spray nozzles of the first AbC absorber, providing the cooled, concentrated LiBr solution to the first solution spray nozzles, the water vapor from the first plurality of evaporator coils being absorbed by the cooled concentrated LiBr solution, producing heat and the diluted LiBr solution;
 - a first solution expansion valve in the cooled, concentrated LiBr solution pipe;
 - a first diluted LiBr solution pipe extending between the first AbC absorber and the heat absorbing coils;
 - a first diluted LiBr solution pump in the first diluted LiBr solution pipe for pumping the diluted LiBr solution to the heat absorbing coils, the diluted LiBr solution being heated in the heat absorbing coils by the concentrated LiBr solution in the heat producing coils;
 - a heated, diluted LiBr solution pipe extending between the heat absorbing coils and the solution sprayer of the AbC generator for providing the heated diluted LiBr solution to the AbC generator solution sprayer;
 - a cold seawater pipe extending between a source of cooling water and the first seawater heating coils to provide seawater to the first seawater heating coils to produce heated seawater;
 - a first heated seawater pipe extending between the first seawater heating coils and the seawater spray nozzles at the top of the humidification column, providing the heated seawater to the seawater spray nozzles; and a second heated seawater pipe defining a conduit for heated seawater from seawater heating coils of a second AbC absorber to the first heating seawater coils of the first AbC absorber.
2. The integrated desalination and air conditioning system as recited in claim 1, further comprising a demister at the top of the humidification column to prevent passage of any water droplets into the third air duct.
 3. The integrated desalination and air conditioning system as recited in claim 1, further comprising packing material in the interior of the humidification column, the packing material increasing the residence time of the heated seawater from the seawater spray nozzles with the heated air from the AbC condenser.
 4. The integrated desalination and air conditioning system as recited in claim 1, further comprising a brine pipe extending from the bottom of the humidification column, for draining excess feed water from the humidification column.
 5. The integrated desalination and air conditioning system as recited in claim 4, further comprising a brine pump directing excess feed water from the brine pipe into the first heated seawater pipe, the excess feed water being mixed with the heated seawater for dispensing by the seawater spray nozzles at the top of the humidification column.
 6. The integrated desalination and air conditioning system as recited in claim 5, further comprising a brine drain connected to the brine pipe, excess brine being drained from the integrated desalination and air conditioning system, via the brine drain.

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7. The integrated desalination and air conditioning system as recited in claim 1, further comprising a fresh water pipe extending from the product water tank to an external water system.
8. The integrated desalination and air conditioning system as recited in claim 1, further comprising:
 - an exhaust duct in the second air duct;
 - a first damper in the exhaust duct;
 - a second damper in the second air duct between the humidification column and the AbC condenser, the first damper and the second damper each having an open position and a closed position so that:
 - when the first damper is closed and the second damper is open, the heated air from the AbC condenser is fed to the bottom of the humidification column via the second duct; and
 - when the first damper is open and the second damper is closed, the heated air from the AbC condenser is vented out of the integrated desalination and air conditioning system via the exhaust duct.
9. The integrated desalination and air conditioning system as recited in claim 8, further comprising a third damper between the first AbC evaporator and the AbC condenser, the third damper having a plurality of vanes for controlling an amount of cold and dry air from the first AbC evaporator to be mixed with the outside air entering the AbC condenser.
10. The integrated desalination and air conditioning system as recited in claim 9, further comprising a first fan for blowing the outside air from the first air input duct to the AbC condenser.
11. The integrated desalination and air conditioning system as recited in claim 10, further comprising a second fan for directing the hot and dry air from the AbC condenser to the bottom of the humidification column when the first damper is closed and the second damper is open or out of the integrated desalination and air conditioning system via the exhaust duct when the first damper is open and the second damper is closed.
12. The integrated desalination and air conditioning system as recited in claim 11, further comprising a third fan for blowing the cold and dry air from the AbC evaporator to the fourth air duct and to the AbC condenser when the third damper is at least partially open.
13. The integrated desalination and air conditioning system as recited in claim 9, further comprising:
 - a second evaporator having:
 - a second evaporator sprayer; and
 - second evaporator coils containing a refrigerant; and
 - a second refrigerant expansion valve in the saturated liquid pipe for providing very low pressure cold water refrigerant to the second evaporator sprayer, so that the low pressure cold water is sprayed on the second evaporator coils by the second evaporator sprayer, thereby chilling the water in the second evaporator coils and converting the low pressure cold refrigerant to a saturated vapor.
14. The integrated desalination and air conditioning system as recited in claim 13, further comprising:
 - a chilled water supply pipe for supplying chilled water from the second evaporator coils to at least one consumer cooling unit; and
 - a chilled water return pipe for supplying heated chilled water from the at least one consumer cooling unit to the second evaporator coils.
15. The integrated desalination and air conditioning system as recited in claim 13, further comprising:

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the second AbC absorber having: second solution spray nozzles; and the second seawater coils;

a second vapor pipe for supplying the saturated vapor refrigerant from the second evaporator to the second AbC absorber;

a second solution expansion valve for supplying the cooled concentrated LiBr solution from the cooled, concentrated LiBr solution pipe to the second solution spray nozzles, the water vapor from the first plurality of evaporator coils being absorbed by the cooled concentrated LiBr solution, producing heat and the diluted LiBr solution;

a second diluted LiBr solution pipe extending between the second AbC absorber and the first solution spray nozzles of the first AbC absorber; and

a second diluted LiBr solution pump in the second diluted LiBr solution pipe for supplying the diluted LiBr solution from the second AbC absorber to the first solution spray nozzles of the first AbC absorber.

16. The integrated desalination and air conditioning system as recited in claim 1, wherein the cold seawater pipe extends directly between the source of cooling water and the seawater coils of the first AbC absorber.

17. The integrated desalination and air conditioning system as recited in claim 1, wherein the heat source is a low-grade heat source, chosen from the group consisting of waste heat and solar thermal energy.

18. An integrated desalination and air conditioning system, comprising:

a first air input duct supplying outside air to the desalination system;

a vapor absorption cycle condenser for heating the outside air, the vapor absorption cycle condenser having a plurality of condenser coils;

a humidification column having an interior, a top, a bottom and seawater spray nozzles at the top of the humidification column;

a second air duct directing heated air from the AbC condenser to the bottom of the humidification column;

a first AbC evaporator for cooling heated humid air from the top of the humidification column, the first AbC evaporator having a first plurality of evaporator coils;

a third air duct directing heated humid air from the top of the humidification column to the first AbC evaporator;

a fourth air duct for directing cold and dry air from the first AbC evaporator to a predetermined location, the predetermined location defines an air conditioned space;

an exhaust duct in the second air duct;

an AbC generator having:

a solution sprayer for spraying a diluted LiBr solution; and means for receiving heat from a heat source to separate heated water vapor from the diluted LiBr solution, thereby forming a concentrated LiBr solution;

a water vapor pipe extending between the AbC generator and the AbC condenser coils, to provide the water vapor to the AbC condenser coils;

a saturated liquid pipe extending between the AbC condenser coils and the first AbC evaporator coils;

a first refrigerant expansion valve in the saturated liquid pipe for providing very low pressure, cold water to the first AbC evaporator coils;

a first AbC absorber having:

first solution spray nozzles for spraying the concentrated LiBr solution; and

first seawater heating coils;

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a first vapor pipe extending between the first AbC evaporator coils and the first AbC absorber for providing water vapor from the first AbC evaporator coils to the first AbC absorber;

a solution heat exchanger having:

heat producing coils; and

heat absorbing coils;

a concentrated LiBr solution pipe extending between the AbC generator and the heat producing coils for providing the concentrated LiBr solution to the heat producing coils to produce a cooled concentrated LiBr solution;

a cooled, concentrated LiBr solution pipe extending between the heat producing coils and the first AbC absorber solution spray nozzles for providing the cooled concentrated LiBr solution to the first AbC absorber solution spray nozzles, the water vapor from the first AbC evaporator coils being absorbed by the cooled, concentrated LiBr solution, producing heat and the diluted LiBr solution;

a first solution expansion valve in the cooled, concentrated LiBr solution pipe;

a first diluted LiBr solution pipe extending between the AbC absorber and the heat absorbing coils;

a first diluted LiBr solution pump in the first diluted LiBr solution pipe for pumping the diluted LiBr solution to the heat absorbing coils, the diluted LiBr solution being heated in the heat absorbing coils by the concentrated LiBr solution in the heat producing coils;

a heated, diluted LiBr solution pipe extending between the heat absorbing coils and the solution sprayer of the AbC generator for providing the heated, diluted LiBr solution to the AbC generator solution sprayer;

a second evaporator having:

a second evaporator sprayer; and

second evaporator coils containing a refrigerant;

a second refrigerant expansion valve in the saturated liquid pipe for providing very low pressure cold water refrigerant to the second evaporator sprayer, wherein the low pressure cold water refrigerant is sprayed on the second evaporator coils by the second evaporator sprayer, thereby cooling the heated chilled water in the second evaporator coils and converting the low pressure cold refrigerant to a saturated vapor;

a second AbC absorber having:

second solution spray nozzles; and

second seawater heating coils;

a second vapor pipe for supplying the saturated vapor from the second evaporator to the second AbC absorber;

a second solution expansion valve for supplying the cooled concentrated LiBr solution from the cooled, concentrated LiBr solution pipe to the second solution spray nozzles, the water vapor from the first plurality of evaporator coils being absorbed by the cooled concentrated LiBr solution, producing heat and the diluted LiBr solution;

a second diluted LiBr solution pipe extending between the second AbC absorber and the first solution spray nozzles of the first AbC absorber;

a second diluted LiBr solution pump in the second diluted LiBr solution pipe for supplying the cooled diluted LiBr solution from the second AbC absorber to the first solution spray nozzles of the first AbC absorber;

a cold seawater pipe extending between a source of cooling water and the second seawater heating coils to

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provide seawater to the second seawater heating coils
to produce heated seawater;
a first heated seawater pipe extending between the first
seawater heating coils and the seawater spray nozzles at
the top of the humidification column for providing the 5
heated seawater to the seawater spray nozzles; and
a second heated seawater pipe extending between the first
seawater coils of the first AbC absorber and the second
seawater coils of the second AbC absorber.

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